FHI, Berlin, January 27th, 2017



In-Situ Differential Scanning Calorimetry in the Studies of Oxide Catalysts and Mechanisms in Oxidative Heterogeneous Catalysis

Mikhail Sinev



Semenov Institute of Chemical Physics, Russian Academy of Sciences Moscow, RUSSIA

Outline

- 1. Introduction:
 - energy factor in chemical processes
 - Chemical Thermodynamics vs. Thermochemistry
 - particularity of 'reaction independence' principle in heterogeneous catalysis
- 2. Calorimetric measurements: methods and instruments
- 3. Signal treatment
- 4. Case studies
- 5. Summary & Concluding Remark





FHI, Berlin, 27.01.2017

Energy Factor:

- intrinsic reactivity
- interaction with environment



Energy Factor:

- intrinsic reactivity
- interaction with environment

Reactivity:

- thermodynamic aspect (Free Energy 'driving force', feasibility)
- kinetic aspect (Activation Energy 'barrier on reaction coordinate')

Energy Factor:

- intrinsic reactivity
- interaction with environment

Reactivity:

- thermodynamic aspect (Free Energy 'driving force', feasibility)
- kinetic aspect (Activation Energy 'barrier on reaction coordinate')

Interaction with environment:

- external parameters ('conditions')
- subject to change



Energy Factor:

- intrinsic reactivity
- interaction with environment

Reactivity:

ICP RAS

- thermodynamic aspect (Free Energy 'driving force', feasibility)
- kinetic aspect (Activation Energy 'barrier on reaction coordinate')

Interaction with environment:

- external parameters ('conditions')
- subject to change



Introduction: Chemical Thermodynamics vs. Thermochemistry

Chemical Thermodynamics –

the study (branch of Physical Chemistry) of interrelations between heat and work in relation to chemical systems, i.e. to substances and their chemical transformations and changes of physical state (e.g., phase transitions)



Introduction: Chemical Thermodynamics vs. Thermochemistry

Chemical Thermodynamics –

the study (branch of Physical Chemistry) of interrelations between heat and work in relation to chemical systems, i.e. to substances and their chemical transformations and changes of physical state (e.g., phase transitions)

Thermochemistry –

the branch of Chemical Thermodynamics) which focuses on the study of heat associated with chemical reactions and/or physical transformations



Introduction: Chemical Thermodynamics vs. Thermochemistry

Chemical Thermodynamics –

the study (branch of Physical Chemistry) of interrelations between heat and work in relation to chemical systems, i.e. to substances and their chemical transformations and changes of physical state (e.g., phase transitions)

Thermochemistry –

the branch of Chemical Thermodynamics) which focuses on the study of heat associated with chemical reactions and/or physical transformations

<u>Key parameters</u>: enthalpy of formation/transformation (reaction, phase transition), heat capacity



Introduction: Chemical Thermodynamics and Catalysis



Catalyst does not affect the chemical equilibrium, but only changes (e.g. accelerates) the rate(s) of thermodynamically feasible reaction(s)

Friedrich Wilhelm Ostwald (1853-1932)







Friedrich Wilhelm Ostwald (1853-1932)

Independence of Reactions Principle –

the applicability of the main postulate of chemical kinetics (Mass Action Law) to a particular reaction does not depend on the occurrence of other reactions in the system







Friedrich Wilhelm Ostwald (1853-1932)

Independence of Reactions Principle –

the applicability of the main postulate of chemical kinetics (Mass Action Law) to a particular reaction does not depend on the occurrence of other reactions in the system

If the 'chemical nature' of the process does not change, its kinetic behaviour also does not change – ???







Independence of Reactions Principle –

the applicability of the main postulate of chemical kinetics (Mass Action Law) to a particular reaction does not depend on the occurrence of other reactions in the system

Friedrich Wilhelm Ostwald (1853-1932)

If the 'chemical nature' of the process does not change, its kinetic behaviour also does not change – ???

Homogeneous reactions in gas – YES!







Independence of Reactions Principle –

the applicability of the main postulate of chemical kinetics (Mass Action Law) to a particular reaction does not depend on the occurrence of other reactions in the system

Friedrich Wilhelm Ostwald (1853-1932)

If the 'chemical nature' of the process does not change, its kinetic behaviour also does not change – ???

Homogeneous reactions in gas – YES!

Heterogeneous catalysis – NO:

- non-uniformity (irregularity) of surfaces and ad-layers
- non-stoichiometry of solids and their dynamic character







Independence of Reactions Principle –

the applicability of the main postulate of chemical kinetics (Mass Action Law) to a particular reaction does not depend on the occurrence of other reactions in the system

Friedrich Wilhelm Ostwald (1853-1932)

If the 'chemical nature' of the process does not change, its kinetic behaviour also does not change – ???

FHI, Berlin, 27.01.2017

Homogeneous reactions in gas – YES!

Heterogeneous catalysis – NO:

- non-uniformity (irregularity) of surfaces and ad-layers
- non-stoichiometry of solids and their dynamic character

In heterogeneous catalysis we cannot rely on 'tabular' values of thermodynamic characteristics



Chemical Thermodynamics –

the study (branch of Physical Chemistry) of interrelations between heat and work in relation to chemical systems, i.e. to substances and their chemical transformations and changes of physical state (e.g., phase transitions)

Thermochemistry –

the branch of Chemical Thermodynamics) which focuses on the study of heat associated with chemical reactions and/or physical transformations

Key parameters: enthalpy of formation/transformation (reaction, phase transition), heat capacity





Chemical Thermodynamics –

the study (branch of Physical Chemistry) of interrelations between heat and work in relation to chemical systems, i.e. to substances and their chemical transformations and changes of physical state (e.g., phase transitions)

Thermochemistry –

the branch of Chemical Thermodynamics) which focuses on the study of heat associated with chemical reactions and/or physical transformations

<u>Key parameters</u>: enthalpy of formation/transformation (reaction, phase transition), heat capacity determined in realistic conditions





Chemical Thermodynamics –

the study (branch of Physical Chemistry) of interrelations between heat and work in relation to chemical systems, i.e. to substances and their chemical transformations and changes of physical state (e.g., phase transitions)

Thermochemistry –

ICP RAS

the branch of Chemical Thermodynamics) which focuses on the study of heat associated with chemical reactions and/or physical transformations

<u>Key parameters</u>: enthalpy of formation/transformation (reaction, phase transition), heat capacity determined in realistic conditions



Calorimetry –

experimental methods for measuring thermal effects (heat evolution and consumption) accompanying the processes of various types (chemical, physical, biological) and based on different physical principles





Adiabatic Calorimetry





Adiabatic Calorimetry –

in a system that is thermally isolated from the environment (no external heat exchange) called *adiabatic*

 $\Delta T = Q/C$,

where ΔT – temperature change; Q – heat evolved (consumed);

C – heat capacity





Adiabatic Calorimetry –

in a system that is thermally isolated from the environment (no external heat exchange) called *adiabatic*

 $\Delta \mathsf{T} = \mathsf{Q}/\mathsf{C},$

where ΔT – temperature change;

Q – heat evolved (consumed);

C – heat capacity





 $Q = C \Delta T_{\infty}$

FHI, Berlin, 27.01.2017



Adiabatic Calorimetry -

- high precision (ΔH_f , C_P , etc.);
- limited T range;
- long-lasting measurements / low productivity;
- low temporal resolution





Differential Scanning Calorimetry (DSC)





Differential Scanning Calorimetry (DSC) – experimental methods for measuring thermal effects (heat evolution and consumption)

- in extended range of temperatures;
- with improved productivity;
- with higher temporal resolution





Differential Scanning Calorimetry (DSC) – experimental methods for measuring thermal effects (heat evolution and consumption)

- in extended range of temperatures;
- with improved productivity;
- with higher temporal resolution

Differential Scanning Calorimetry (DSC) – scheme of measurements (permanently compared to reference)





Differential Scanning Calorimetry (DSC) – experimental methods for measuring thermal effects (heat evolution and consumption)

- in extended range of temperatures;
- with improved productivity;
- with higher temporal resolution

Differential Scanning Calorimetry (DSC) – measurements at varied (programmed) temperature (permanently and/or stepwise)



Differential Scanning Calorimetry (DSC) – experimental methods for measuring thermal effects (heat evolution and consumption)

- in extended range of temperatures;
- with improved productivity;
- with higher temporal resolution

Differential Scanning Calorimetry (DSC) – 'near-calorimetric' (although reduced) precision (typically, 1-2% of measured thermal value) – as a rule, satisfactory for a wide range of applications





Differential Scanning Calorimetry (DSC) – experimental methods for measuring thermal effects (heat evolution and consumption)

- in extended range of temperatures;
- with improved productivity;
- with higher temporal resolution

based on different technical principles and schemes but fundamentally – on the same physical background: heat transfer and balance



Differential Scanning Calorimetry (DSC) – experimental methods for measuring thermal effects (heat evolution and consumption)

- in extended range of temperatures;
- with improved productivity;
- with higher temporal resolution

based on different technical principles and schemes but fundamentally – on the same physical background: heat transfer and balance

> *q* = k∆T + C(dT/dt) – Tian equation (heat removal & storage)



Differential Scanning Calorimetry (DSC) -

experimental methods for measuring thermal effects (heat evolution and consumption), based on different technical principles and schemes, but on the same physical principles of heat transfer and balance

 $q = k\Delta T + C(dT/dt) - heat removal and stortage$





FHI, Berlin, 27.01.2017

ICP RAS

DSC: different technical principles and schemes





- DSC: different technical principles and schemes
- 1. 'Quantitative TA'
 - TA thermal analysis, i.e. measurement of
 ∆T between the sample and the reference (usually, in a T-programmed regime)





- DSC: different technical principles and schemes
- 1. 'Quantitative TA'

ICP RAS

TA – thermal analysis, i.e. measurement of ΔT between the sample and the reference (usually, in a T-programmed regime)





- DSC: different technical principles and schemes
- 1. 'Quantitative TA'

ICP RAS

TA – thermal analysis, i.e. measurement of ΔT between the sample and the reference (usually, in a T-programmed regime)





- DSC: different technical principles and schemes
- 1. 'Quantitative TA'
 - multiple sensors
 - tight contact between sensors and holders
 - rapid heat removal from the sample






- DSC: different technical principles and schemes
- 1. 'Quantitative TA'

ICP RAS

- multiple sensors
- tight contact between sensors and holders
- rapid heat removal from the sample

 $C(dT/dt) \approx 0$ and $q \approx k\Delta T$





FHI, Berlin, 27.01.2017

- DSC: different technical principles and schemes
- 1. 'Quantitative TA'
 - multiple sensors
 - tight contact between sensors and holders
 - rapid heat removal from the sample



- relatively simple design;
- wide range of T's;
- compatible with other methods (e.g. TG)
- calibration is critical and can vary from sample to sample;
- gas-solid diffusion





DSC: different technical principles and schemes



FHI, Berlin, 27.01.2017

DSC: different technical principles and schemes

2. 'Zero ΔT ' or 'heat-compensation' DSC





- 2. 'Zero ΔT ' or 'heat-compensation' DSC
 - precise T-sensor + fast feed-back control + thermal compensation (Joule or combined Joule-Peltier elements, i.e. thermoelectric heaters or heater/cooler)
 - measured parameter electric power required to compensate thermal effects in the sample







- 2. 'Zero ΔT ' or 'heat-compensation' DSC
 - precise T-sensor + fast feed-back control + thermal compensation (Joule or combined Joule-Peltier elements, i.e. thermoelectric heaters or heater/cooler)
 - measured parameter electric power required to compensate thermal effects in the sample



- direct measurement of power;
- precise measurements of T
- calibration is critical and can vary from sample to sample (2D T sensing);
- gas-solid diffusion





- 2. 'Zero ΔT ' or 'heat-compensation' DSC
 - precise T-sensor + fast feed-back control + thermal compensation (Joule or combined Joule-Peltier elements, i.e. thermoelectric heaters or heater/cooler)
 - measured parameter electric power required to compensate thermal effects in the sample







- 3. 'Heat-flux', or 'heat-conductive', or Calvet-type DSC
 - heat flux is measured outside of the sample assuming that it is proportional to the ΔT on different distances from it





DSC: different technical principles and schemes

- 3. 'Heat-flux', or 'heat-conductive', or Calvet-type DSC
 - heat flux is measured outside of the sample assuming that it is proportional to the ΔT on different distances from it

Calvet sensor (top view)

thermocouple sample (reaction) tube



outer cyl.surface $(T_{out})\;$ inner cyl.surface $(T_{in})\;$

 $q \sim (T_{in} - T_{out})$

Calvet calorimetry (incl. DSC):

- none of the TC's measures the temperature of the sample (!!!);
- the DSC signal is formed as ∆T between two cylindrical surfaces (inner and outer) on different
 distances from the sample





DSC: different technical principles and schemes

- 3. 'Heat-flux', or 'heat-conductive', or Calvet-type DSC
 - heat flux is measured outside of the sample assuming that it is proportional to the ΔT on different distances from it



ICP RAS

Side view: Calvet (3D) vs. TA (2D) sensing



<u>3D vs. 2D sensing</u>: more efficient (complete) capturing of heat fluxes from/to the sample – lower sensitivity to the sample properties !!!

FHI, Berlin, 27.01.2017

DSC: different technical principles and schemes

- 3. 'Heat-flux', or 'heat-conductive', or Calvet-type DSC
 - heat flux is measured outside of the sample assuming that it is proportional to the ΔT on different distances from it



 $q \sim (T_{in} - T_{out})$

ICP RAS

- fool realization of the potential of Newton-Richmann law and Tian equation;
- the sample does not play the role of 'thermal resistance';
- no tight contact between sample (and reference) holder(s) and the sensor is required;
- 3D heat sensing;
- good gas-solid mass-transfer conditions;

FHI, Berlin, 27.01.2017

- high compatibility (e.g. with TGA)
- relatively low temporal resolution

- 3. 'Heat-flux', or 'heat-conductive', or Calvet-type DSC
 - heat flux is measured outside of the sample assuming that it is proportional to the ΔT on different distances from it







DSC: different technical principles and schemes

3. 'Heat-flux', or 'heat-conductive', or Calvet-type DSC

– heat flux is measured outside of the sample assuming that it is proportional to the ΔT on different distances from it





DSC: different technical principles and schemes

3. 'Heat-flux', or 'heat-conductive', or Calvet-type DSC

– heat flux is measured outside of the sample assuming that it is proportional to the ΔT on different distances from it





Setaram SENSYS evo (DSC-111)















Setaram DSC-111













ICP RAS

Setaram DSC-111

Setaram DSC-111 for heterogeneous catalysis





Setaram DSC-111 for heterogeneous catalysis – *in situ* cell







Setaram DSC-111 for heterogeneous catalysis – in situ DSC



FHI, Berlin, 27.01.2017

Setaram DSC-111 for heterogeneous catalysis – in situ DSC



Temperature range: R.T - 1100 K; heating rates: 0-20 K/min.; 'chemical resolution' - 10^{15} - 10^{16} at. (~0.01 ML @ ~1 m²/g & m = 25 mg)

FHI, Berlin, 27.01.2017











FHI, Berlin, 27.01.2017



 $\mathbf{Q} = \int_{0}^{\infty} q dt \simeq a \int_{0}^{\infty} \Delta T dt$

Treatment of DSC signal:

- baseline







 $\mathbf{Q} = \int_{0}^{\infty} q dt \simeq a \int_{0}^{\infty} \Delta T dt$

Treatment of DSC signal:

- baseline
- signal as such

- ...





 $\mathbf{Q} = \int_{0}^{\infty} q dt \simeq a \int_{0}^{\infty} \Delta T dt$

Treatment of DSC signal:

- baseline
- signal as such

- ...







$$\mathbf{Q} = \int_{0}^{\infty} q \, \mathrm{dt} \simeq a \int_{0}^{\infty} \Delta \mathrm{T} \, \mathrm{dt}$$

 $q = k\Delta T + C(dT/dt) - Tian equation$







$$\mathbf{Q} = \int_{0}^{\infty} q \, \mathrm{dt} \simeq a \int_{0}^{\infty} \Delta \mathrm{T} \, \mathrm{dt}$$

 $q = k\Delta T + C(dT/dt) \approx k\Delta T + C(d\Delta T/dt)$







 $q = k\Delta T + C(dT/dt) \approx k\Delta T + C(d\Delta T/dt)$ $\int_{0}^{\infty} qdt$ $\int_{0}^{\infty} \Delta Tdt \approx a, \text{ however } \frac{q}{\Delta T} \neq \text{const.}$

FHI, Berlin, 27.01.2017





 $q = k\Delta T + C(dT/dt) \approx k\Delta T + C(d\Delta T/dt)$ = $k[\Delta T + \tau^*(d\Delta T/dt)]$ $\tau^* = C/k$ – time constant of fluxmeter

for DSC-111 $\tau^{\star}\approx 25~s$







 $q = k\Delta T + C(dT/dt) \approx k\Delta T + C(d\Delta T/dt)$ $= k[\Delta T + \tau^*(d\Delta T/dt)]$

 $\tau^* = C/k - time \text{ constant of fluxmeter}$ for DSC-111 $\tau^* \approx 25 \text{ s} - ???$

FHI, Berlin, 27.01.2017





 ΔT -curve 'tail': $q = k[\Delta T + \tau^*(d\Delta T/dt)] \approx 0 \Rightarrow$ $\Delta T \sim 1 - \exp(-t/\tau^*)$ and $\tau^* = - d(Log\Delta T)/dt$





 ΔT -curve 'tail': $q = k[\Delta T + \tau^*(d\Delta T/dt)] \approx 0 \Rightarrow$ $\Delta T \sim 1 - \exp(-t/\tau^*)$ and $\tau^* = - d(Log\Delta T)/dt$

$q = k\Delta T + C(dT/dt) \approx k\Delta T + C(d\Delta T/dt)$ $= k[\Delta T + \tau^*(d\Delta T/dt)]$



Treatment of DSC signal (q-curve)

$q = k\Delta T + C(dT/dt) \approx k\Delta T + C(d\Delta T/dt)$ $= k[\Delta T + \tau^*(d\Delta T/dt)]$



Treatment of DSC signal (q-curve)
$q = k\Delta T + C(dT/dt) \approx k\Delta T + C(d\Delta T/dt)$ $= k[\Delta T + \tau^*(d\Delta T/dt)]$



Treatment of DSC signal (q-curve)

$q = k\Delta T + C(dT/dt) \approx k\Delta T + C(d\Delta T/dt)$ $= k[\Delta T + \tau^*(d\Delta T/dt)]$



Treatment of DSC signal (q-curve)

$q = k\Delta T + C(dT/dt) \approx k\Delta T + C(d\Delta T/dt)$ $= k[\Delta T + \tau^*(d\Delta T/dt)]$



Treatment of DSC signal (q-curve)











If $\tau_{chem} \leq \tau^*$, dynamic (e.g., T-prog.) measurements may lead to substantial errors (both kinetic and calorimetric)

FHI, Berlin, 27.01.2017

In Calvet-type DSC $q = k\Delta T + C(dT/dt) \approx k\Delta T + C(d\Delta T/dt)$ $= k[\Delta T + \tau^*(d\Delta T/dt)]$ $k\uparrow \Rightarrow \tau^* (\approx C/k)\downarrow, \quad but \langle q \rangle \sim \Delta T\downarrow \Rightarrow$ $\langle q \rangle \downarrow @ \tau^* \downarrow (\langle q \rangle \times \tau^* \approx const.)$



In Calvet-type DSC $q = k\Delta T + C(dT/dt) \approx k\Delta T + C(d\Delta T/dt)$ $= k[\Delta T + \tau^*(d\Delta T/dt)]$ $k\uparrow \Rightarrow \tau^* (\approx C/k)\downarrow, \qquad but \langle q \rangle \sim \Delta T\downarrow \qquad \Rightarrow$ $\langle q \rangle \downarrow @ \tau^* \downarrow \quad (\langle q \rangle \times \tau^* \approx const.)$

MS80







SETSYS evo (DSC-111)

FHI, Berlin, 27.01.2017





Measurements: calorimetric

dynamic

FHI, Berlin, 27.01.2017





 $\tau^* \approx 5-10$ min.

ICP RAS

~ 25 sec.





Pulse suply if active reactants \Rightarrow

ICP RAS

'differential' heats in each pulse correct dQ/dN values

FHI, Berlin, 27.01.2017

DSC – methods & instrumentation: summary

wide variety of instruments



FHI, Berlin, 27.01.2017

DSC – methods & instrumentation: summary

- wide variety of instruments
- careful selection according to specific needs & requirements Tr



DSC – methods & instrumentation: summary

- wide variety of instruments
- careful selection according to specific needs & requirements
- rough experimental data must be "handled with care"



FHI, Berlin, January 27th, 2017



In-Situ Differential Scanning Calorimetry in the Studies of Oxide Catalysts and Mechanisms in Oxidative Heterogeneous Catalysis

Mikhail Sinev



Semenov Institute of Chemical Physics, Russian Academy of Sciences Moscow, RUSSIA FHI, Berlin, January 27th, 2017



In-Situ Differential Scanning Calorimetry in the Studies of Oxide Catalysts and Mechanisms in Oxidative Heterogeneous Catalysis

Mikhail Sinev



Semenov Institute of Chemical Physics, Russian Academy of Sciences Moscow, RUSSIA FHI, Berlin, January 27th, 2017



In-Situ Differential Scanning Calorimetry in the Studies of Oxide Catalysts and Mechanisms in <u>Oxidative Heterogeneous</u> <u>Catalysis</u>

Mikhail Sinev



Semenov Institute of Chemical Physics, Russian Academy of Sciences Moscow, RUSSIA

$A + \frac{1}{2}O_2 \rightarrow AO$



k – apparent rate constant





 $A + \frac{1}{2}O_2 \rightarrow AO$



k – apparent rate constant

 $k = k_1^* + k_2 =$ = $k_1 \theta_{[O]} + k_2$

FHI, Berlin, 27.01.2017



 $[O]_{S} + A \rightarrow []_{S} + AO$ $[]_{S} + O_{2} \Leftrightarrow [O_{2}]_{S} \rightarrow ... \rightarrow [O]_{S}$

"Classical" oxygen adsorptiondesorption (OAD) mechanism

$$W_{AO}^{*} = \frac{k_{red}^{*} P_{A} k_{ox} P_{O2}}{1 + K_{ox} P_{O2}}$$

 $[O]_{S} + A \rightarrow []_{S} + AO$ $[]_{S} + O_{2} \rightarrow ... \rightarrow [O]_{S}$

"Classical" oxygen rebound-replenish (ORR) mechanism

$$W_{AO} = \frac{k_{red} P_A k_{ox} P_{O_2}}{k_{red} P_A + k_{ox} P_{O_2}}$$





 $[O]_{S} + A \rightarrow []_{S} + AO$ $[]_{S} + O_{2} \Leftrightarrow [O_{2}]_{S} \rightarrow ... \rightarrow [O]_{S}$

"Classical" oxygen adsorptiondesorption (OAD) mechanism

$$W_{AO}^* = \frac{k_{red}^* P_A k_{ox} P_{O_2}}{1 + K_{ox} P_{O_2}}$$

 $[O]_{S} + A \rightarrow []_{S} + AO$ $[]_{S} + O_{2} \rightarrow ... \rightarrow [O]_{S}$

"Classical" oxygen rebound-replenish (ORR) mechanism

$$W_{AO} = \frac{k_{red} P_A k_{ox} P_{O_2}}{k_{red} P_A + k_{ox} P_{O_2}}$$

 $[O]_{S}$ vs. $P(O_{2,g})$ 'equilibration':

OAD (+), ORR (-)





 $[O]_{S} + A \rightarrow []_{S} + AO$ $[]_{S} + O_{2} \Leftrightarrow [O_{2}]_{S} \rightarrow ... \rightarrow [O]_{S}$

"Classical" oxygen adsorptiondesorption (OAD) mechanism

$$W_{\rm AO}^* = \frac{k_{red}^* P_{\rm A} k_{ox} P_{\rm O2}}{1 + K_{ox} P_{\rm O2}}$$

 $[O]_{S} + A \rightarrow []_{S} + AO$ $[]_{S} + O_{2} \rightarrow ... \rightarrow [O]_{S}$

"Classical" oxygen rebound-replenish (ORR) mechanism

$$W_{AO} = \frac{k_{red} P_A k_{ox} P_{O_2}}{k_{red} P_A + k_{ox} P_{O_2}}$$

 $[O]_{S}$ vs. $P(O_{2,g})$ 'equilibration':

OAD (+), ORR (-)

None of the two says anything about the 'nature' of active O-species (lattice, adsorbed, ...)





 $[O]_{S} + A \rightarrow []_{S} + AO$ $[]_{S} + O_{2} \Leftrightarrow [O_{2}]_{S} \rightarrow ... \rightarrow [O]_{S}$

"Classical" oxygen adsorptiondesorption (OAD) mechanism

$$W_{AO}^* = \frac{k_{red}^* P_A k_{ox} P_{O_2}}{1 + K_{ox} P_{O_2}}$$

 $[O]_{S} + A \rightarrow []_{S} + AO$ $[]_{S} + O_{2} \rightarrow ... \rightarrow [O]_{S}$

"Classical" oxygen rebound-replenish (ORR) mechanism

$$W_{AO} = \frac{k_{red} P_A k_{ox} P_{O_2}}{k_{red} P_A + k_{ox} P_{O_2}}$$

 $[O]_{S}$ vs. $P(O_{2,g})$ 'equilibration':

OAD (+), ORR (-)

None of the two says anything about the 'nature' of active O-species (lattice, adsorbed, ...)

In both cases the properties of active O-species and the 'substrate' interaction with them are crucial for activity/selectivity





'Key' properties of active O-species:

- lifetime (\Rightarrow type of kinetics);
- reactivity qualitative (types of interactions with other species) and quantitative (rates)



'Key' properties of active O-species:

- lifetime (\Rightarrow type of kinetics);
- reactivity qualitative (types of interactions with other species) and quantitative (rates)

'Substrate' interactions with active O-species:

- qualitative (types of interactions & products formed);
- quantitative (rates / kinetic parameters)



Energy Factor:

- intrinsic reactivity
- interaction with environment

Reactivity:

- thermodynamic aspect (Free Energy 'driving force', feasibility)
- kinetic aspect (Activation Energy 'barrier on reaction coordinate')

Interaction with environment:

- external parameters ('conditions')
- subject to change

⇒ feedback

FHI. Berlin, 27.01.2017

Energy Factor:

- intrinsic reactivity
- interaction with environment

Reactivity:

- thermodynamic aspect (Free Energy 'driving force', feasibility)
- kinetic aspect (Activation Energy 'barrier on reaction coordinate')

Interaction with environment:

- external parameters ('conditions')
- subject to change

⇒ feedback

FHI, Berlin, 27.01.2017



Energy in oxidative catalysis over solid oxides

Energy Factor:

- intrinsic reactivity
- interaction with environment

Reactivity:

- thermodynamic aspect (Free Energy 'driving force', feasibility)
- kinetic aspect (Activation Energy 'barrier on reaction coordinate')

FHI. Berlin. 27.01.2017

Oxide catalysts and reactive oxygen:

- O-binding energy (\Rightarrow O-lifetime, defects, etc.);
- reactions with 'substrates' (activity, selectivity);
- mobility (surface and bulk)

Energy in oxidative catalysis over solid oxides

Energy Factor:

- intrinsic reactivity
- interaction with environment

Reactivity:

- thermodynamic aspect (Free Energy 'driving force', feasibility)
- kinetic aspect (Activation Energy 'barrier on reaction coordinate')

Oxide catalysts and reactive oxygen:

- O-binding energy (\Rightarrow O-lifetime, defects, etc.);
- reactions with 'substrates' (activity, selectivity);
- mobility (surface and bulk)

in situ DSC!!!

DSC in situ in oxidative catalysis over solid oxides

'Non-calorimetric' techniques:

- oxygen TPD;
- TPR (e.g., H₂, CO);
- TPO (O₂, N₂O, H₂O, CO₂, etc.)





DSC in situ in oxidative catalysis over solid oxides

'Non-calorimetric' techniques:

- oxygen TPD;
- TPR (e.g., H₂, CO);
- TPO (O₂, N₂O, H₂O, CO₂, etc.)

+ calorimetry:

- thermodynamics vs. kinetics;
- oxygen non-uniformity;
- mechanistic information
 - (e.g., 'E_a vs. Δ H' and 'S vs. E_[O]' correlations)



$$C_nH_{2n+2} + \frac{1}{2}O_2 \rightarrow C_nH_{2n} + H_2O$$
$$C_nH_{2n+2} + zO_2 \rightarrow nCO_X + (n+1)H_2O$$

Catalysts – V-containing bulk and supported oxides





$$C_nH_{2n+2} + \frac{1}{2}O_2 \rightarrow C_nH_{2n} + H_2O$$
$$C_nH_{2n+2} + zO_2 \rightarrow nCO_X + (n+1)H_2O$$

Catalysts – V-containing bulk and supported oxides

'Classical' Red-Ox Kinetics over V-containing catalysts – Mars-van-Krevelen* or oxygen rebound-replenish (ORR) mechanism

$$[O]_{S} + A \rightarrow []_{S} + AO$$
$$[]_{S} + O_{2} \rightarrow ... \rightarrow [O]_{S}$$

FHI, Berlin, 27.01.2017

* toluene oxidation over V-alumina catalyst



550°C, ethane pulses onto pre-oxidized VSb/Al₂O₃







550°C, ethane pulses onto pre-oxidized VSb/Al₂O₃





high selectivity to ethylene





550°C, ethane pulses onto pre-oxidized VSb/Al₂O₃




550°C, ethane pulses onto pre-oxidized VSb/Al₂O₃



6 'Chemical' factor (i.e. state of surface sites and their interaction with HC's) is more important than 'energy' one

ICP RAS

FHI, Berlin, 27.01.2017

550°C, ethane pulses onto pre-oxidized VSb/Al₂O₃



FHI, Berlin, 27.01.2017

ICP RAS



ICP RAS



FHI, Berlin, 27.01.2017

ICP RAS



FHI, Berlin, 27.01.2017

ICP RAS



ICP RAS



ICP RAS

Oxidative Coupling of Methane (OCM)





Oxidative Coupling of Methane (OCM):







Oxidative Coupling of Methane (OCM):



OCM product formation:

CH₄ + [O]_S → CH₃ + [OH]_S

$$\downarrow$$

C₂H₆



IGP RAS

Oxidative Coupling of Methane (OCM):



OCM product formation:

- how radicals form?
- how $[OH]_S$ returns back to $[O]_S$?



Oxidative Coupling of Methane (OCM):



OCM product formation:

$$CH_4 + [O]_S \rightarrow CH_3^{\bullet} + [OH]_S$$

$$\downarrow$$

$$C_2H_6$$

- how radicals form?
- how $[OH]_S$ returns back to $[O]_S$?





700°C, methane pulses onto pre-oxidized oxide catalysts







700°C, methane pulses onto pre-oxidized oxide catalysts

Li/MgO – no water evolved into the gas phase during reduction (CH₄, H₂) - !?







700°C, methane pulses onto pre-oxidized oxide catalysts

Li/MgO – no water evolved into the gas phase during reduction (CH₄, H₂) - !? Immediate water formation after O₂ pulsing - !?



ICP RAS



700°C, methane pulses onto pre-oxidized oxide catalysts

Li/MgO – no water evolved into the gas phase during reduction (CH₄, H₂) - !? Immediate water formation after O₂ pulsing - !? Reduction: [O] + CH₄ \rightarrow [OH] + CH₃• \Rightarrow D_[O-H]

Re-oxidation – ???

ICP RAS

Alternative mechanisms of re-oxidation

 $2 [OH]_{S} \rightleftharpoons [O]_{S} + []_{S} + H_{2}O (A)$





Alternative mechanisms of re-oxidation

- $2 [OH]_{S} \rightleftharpoons [O]_{S} + []_{S} + H_{2}O (A)$
- no water evolution after reduction with methane (ethane) and H₂
- no re-oxidation with N₂O
- fast water evolution after pulsing of O₂



Alternative mechanisms of re-oxidation

- $2 [OH]_{S} \rightleftharpoons [O]_{S} + []_{S} + H_{2}O (A)$
- no water evolution after reduction with methane (ethane) and $\rm H_2$
- no re-oxidation with N₂O
- fast water evolution after pulsing of O₂

$[OH]_{S} + O_{2} \rightarrow [O]_{S} + HO_{2}$	(B1)
$[OH]_{S} + HO_{2} \rightarrow [O]_{S} + H_{2}O_{2}$	(B2)
$H_2O_2 \rightarrow 2 OH$	(B3)
$[OH]_{S} + OH \rightarrow [O]_{S} + H_{2}O$	(B4)
	(P)

$$4 [OH]_{S} + O_{2} \rightarrow 4 [O]_{S} + 2 H_{2}O$$
 (B)



Alternative mechanisms of re-oxidation

 $2 [OH]_{S} \rightleftharpoons [O]_{S} + []_{S} + H_{2}O (A)$ $[OH]_{c} + O_{2} \rightarrow [O]_{c} + HO_{2}$ **(B1)** $[OH]_{s} + HO_{2} \rightarrow [O]_{s} + H_{2}O_{2}$ **(B2)** - no water evolution after reduction $H_2O_2 \rightarrow 2 OH$ with methane (ethane) and H_2 **(B3)** $[OH]_{s} + OH \rightarrow [O]_{s} + H_{2}O$ - no re-oxidation with N₂O **(B4)** - fast water evolution after pulsing of O₂ $4 [OH]_{s} + O_{2} \rightarrow 4 [O]_{s} + 2 H_{2}O$ **(B)** Pb/Al_2O_3 K/Al_2O_3 Li/MgO D_[0-H], kJ/mole 320 250 270

535

E_{ro1}, kJ/mole

Li/MgO: high $E_{[O]}$ and $D_{[O-H]}$ – no water evolved into the gas phase during reduction PbO/Al₂O₃: low $E_{[O]}$ and $D_{[O-H]}$ – rapid evolution of water during reduction K_2O/Al_2O_3 : moderate $E_{[O]}$ and $D_{[O-H]}$ – delayed evolution of water during reduction

407

450



Alternative mechanisms of re-oxidation

 $2 [OH]_{s} \rightleftharpoons [O]_{s} + []_{s} + H_{2}O (A)$ $[OH]_{s} + O_{2} \rightarrow [O]_{s} + HO_{2}$ **(B1)** $[OH]_{S} + HO_{2} \rightarrow [O]_{S} + H_{2}O_{2}$ **(B2)** - no water evolution after reduction $H_2O_2 \rightarrow 2 OH$ with methane (ethane) and H_2 **(B3)** $[OH]_{S} + OH \rightarrow [O]_{S} + H_{2}O$ - no re-oxidation with N₂O **(B4)** - fast water evolution after pulsing of O₂ $4 [OH]_{s} + O_{2} \rightarrow 4 [O]_{s} + 2 H_{2}O$ **(B)** Pb/Al_2O_2 K/Al_2O_2 Li/MaO

D _[о-н] , kJ/mole	320	250	270
E _[o] , kJ/mole	535	407	450

Li/MgO: high $E_{[O]}$ and $D_{[O-H]}$ – no water evolved into the gas phase during reduction PbO/Al₂O₃: low $E_{[O]}$ and $D_{[O-H]}$ – rapid evolution of water during reduction K_2O/Al_2O_3 : moderate $E_{[O]}$ and $D_{[O-H]}$ – delayed evolution of water during reduction

relative contribution of routes A and B is determined by thermochemistry

ICP RAS

Oxidative Coupling of Methane (OCM):



OCM product formation:

- how radicals form?
- how $[OH]_S$ returns back to $[O]_S$?



 $E_a - \Delta H$ Correlation

 $[O] + CH_4 \rightarrow [OH] + CH_3 \cdot \Delta H = D_{[O-H]} - D_{H-CH_3}$





ICP RAS

 $E_a - \Delta H$ Correlation

 $[O] + CH_4 \rightarrow [OH] + CH_3 \cdot \Delta H = D_{[O-H]} - D_{H-CH_3}$



 $CH_4 + X \rightarrow CH_3 + XH$ $\Delta H = D_{H-X} - D_{H-CH_3}$

X = F (1); OH (2); C_6H_5 (3); CF_3 (4); CH_3 (5); H (6); Cl (7); O (8); SH (9); CH_3O (10); Br (11); I (12); O_2 (13)

ICP RAS

 $E_a - \Delta H$ Correlation

 $[O] + CH_4 \rightarrow [OH] + CH_3 \cdot \Delta H = D_{[O-H]} - D_{H-CH_3}$



Analogy between heterogeneous and homogeneous reactions, i.e. [O] + $CH_4 \rightarrow [OH] + CH_3^{\bullet}$ is a collision-type elementary process

 $E_a - \Delta H$ Correlation

 $[O] + CH_4 \rightarrow [OH] + CH_3 \cdot \Delta H = D_{[O-H]} - D_{H-CH_3}$



Analogy between heterogeneous ('gas – s.s.') and homogeneous Interactions of the same type (e.g., H-transfer, O-transfer)

 $E_a - \Delta H$ Correlation

 $[O] + CH_4 \rightarrow [OH] + CH_3 \cdot \Delta H = D_{[O-H]} - D_{H-CH_3}$



Analogy between heterogeneous ('gas – s.s.') and homogeneous Interactions of the same type (e.g., H-transfer, O-transfer) microkinetic (multi-step) model of OCM and related processes









700°C, methane pulses onto pre-oxidized oxide catalysts

PbO/Al₂O₃ – near-steady-state - !?





Re-oxidation of PbO/Al₂O₃ at 700°C after reduction with methane pulse (varied Δt between reduction and re-oxidation)





Re-oxidation of PbO/Al₂O₃ at 700°C after reduction with methane pulse (varied Δt between reduction and re-oxidation)





Re-oxidation of PbO/Al₂O₃ at 700°C after reduction with methane pulse (varied Δt between reduction and re-oxidation)



spatial re-distribution of oxygen / energetic relaxation of reduced lattice





Re-oxidation of PbO/Al₂O₃ at 700°C after reduction with methane pulse (varied Δt between reduction and re-oxidation)



spatial re-distribution of oxygen / energetic relaxation of reduced lattice

In 'standard' tabulated data do not reflect actual relations taking place under reaction conditions





Case study 3: oxygen storage materials (oxides)

Oxygen-storage materials – oxides capable of reversible oxygen uptake/release

Areas of application :

- oxygen capture (deep purification of gases);
- gas sensors;
- catalysis (automobile TWC washcoat component);

- ...

Key characteristics:

- oxygen storage capacity (bulk storage, i.e. lattice oxygen);
- oxygen uptake/release conditions (O-binding energy)



FHI. Berlin. 27.01.2017

Case study 3: oxygen storage materials (oxides)

Oxygen-storage materials – oxides capable of reversible oxygen uptake/release

Areas of application :

- oxygen capture (deep purification of gases);
- gas sensors;
- catalysis (automobile TWC washcoat component);

- ...

Key characteristics:

- oxygen storage capacity (bulk storage, i.e. lattice oxygen);
- oxygen uptake/release conditions (O-binding energy)

ideal objects to study using in situ DSC





Case study 3: oxygen storage materials (oxides)

Typical oxygen-storage materials – oxides with cubic or slightly distorted cubic structure, e.g. spinels, perovskites, fluorites, pirochlores, etc.




Typical oxygen-storage materials – oxides with cubic or slightly distorted cubic structure, e.g. spinels, perovskites, fluorites, pirochlores, etc.



Cubic fluorites (e.g., Y/ZrO₂):

- tend to form oxygen vacancies with no restructuring;

FHI. Berlin. 27.01.2017

- very fast O-transport

 $Ce_{0.55}Pr_{0.45}O_2 - CeO_2$ -based cubic fluorite





 $Ce_{0.55}Pr_{0.45}O_2 - CeO_2$ -based cubic fluorite

Vacuum / inert gas atmosphere, > 350°C:

 $Ce(IV)_{0.55}Pr(IV)_{0.45}O_2 \implies Ce(IV)_{0.55}Pr(III/IV)_{0.45}O_{2-X} + O_2 (X \le 0.225)$

 O_2 -containing atmosphere, < 250°C:

$$\begin{split} \text{Ce(IV)}_{0.5} \text{Pr(III/IV)}_{0.5} \text{O}_{2\text{-X}} + \text{O}_2 \implies \text{Ce(IV)}_{0.5} \text{Pr(IV)}_{0.5} \text{O}_{2\text{-X}} - \\ \text{nearly instantaneously} \end{split}$$







[®] different character of O-uptake kinetics on different stages









FHI, Berlin, 27.01.2017

ICP RAS

Pulse re-oxidation of $Ce_{0.55}Pr_{0.45}O_2$ after O-removal in He at 500°C



FHI, Berlin, 27.01.2017

ICP RAS





- 1 rapid uptake on 'strong' surface sites
- 2 rapid uptake on 'weak' surface sites
- 3 slow re-distribution from 'weak' surface to 'strong' bulk sites

FHI, Berlin, 27.01.2017







1 – rapid uptake on 'strong' surface sites

- 2 rapid uptake on 'weak' surface sites
- 3 slow re-distribution from 'weak' surface to 'strong' bulk sites

Box DSC provides with 'visualization' of O-redistribution (surface to bulk)

ICP RAS

FHI, Berlin, 27.01.2017

Summary & Concluding remark

- Direct measurements of thermal effects accompanying interactions of reactants with solid catalysts is a valuable tool that allows one to reveal the role of energy factor(s) in catalytic reactions
- 2. Like any other method, *in situ* DSC has specific applications, as well as its own advantages and limitations; in some cases it provides with a unique information about dynamic behaviour of oxide systems and valuable complementary information about reaction mechanism(s)





Summary & Concluding remark

- Direct measurements of thermal effects accompanying interactions of reactants with solid catalysts is a valuable tool that allows one to reveal the role of energy factor(s) in catalytic reactions
- 2. Like any other method, *in situ* DSC has specific applications, as well as its own advantages and limitations; in some cases it provides with a unique information about dynamic behaviour of oxide systems and valuable complementary information about reaction mechanism(s)

Combining of calorimetric measurements with other (structure-sensitive) techniques is highly desirable





Acknowledgement

Prof. Oleg V. KRYLOV[⊕]

Dr. Viktor Yu. BYCHKOV







Thank You for Your Attention!



