



Activation of small molecules

-

Ethylene and Oxygen

16th December 2016

Elias Frei

Fritz Haber Institute, Inorganic Chemistry Department
efrei@fhi-berlin.mpg.de

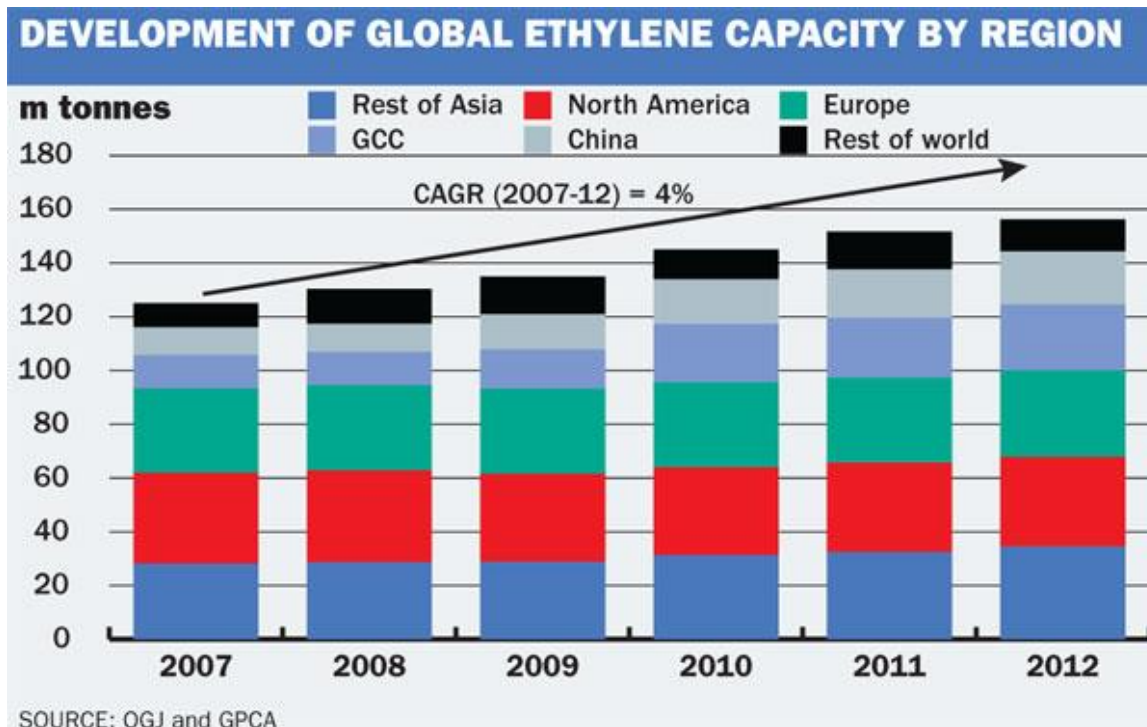
Literature

- 1. Handbook of Heterogenous Catalysis, G. Ertl, H. Knözinger, F. Schüth, J. Weitkamp (2. ed.), Vol 7., 2008
- 2. Industrial Catalytic Processes, C.H. Bartholomew and R.J. Farrauto, Wiley 2006.
- 3. Industrial Organic Chemistry, K. Weissermel, H.-J. Arpe (4. ed), Wiley VCH 2003
- 4. Mechanisms in Homogeneous and Heterogeneous Epoxidation Catalysis, S. Ted Oyama, Elsevier, 2008

+ references on the slides

Ethylene Production

- By far the most important organic chemical compound ~ 150 Mio tons/a
- World scale plant 1 Mio t/a (1970: 300 kt/a)
- Ethylene production: Steam Cracker (<https://youtu.be/QLmh0jJE2zE>)

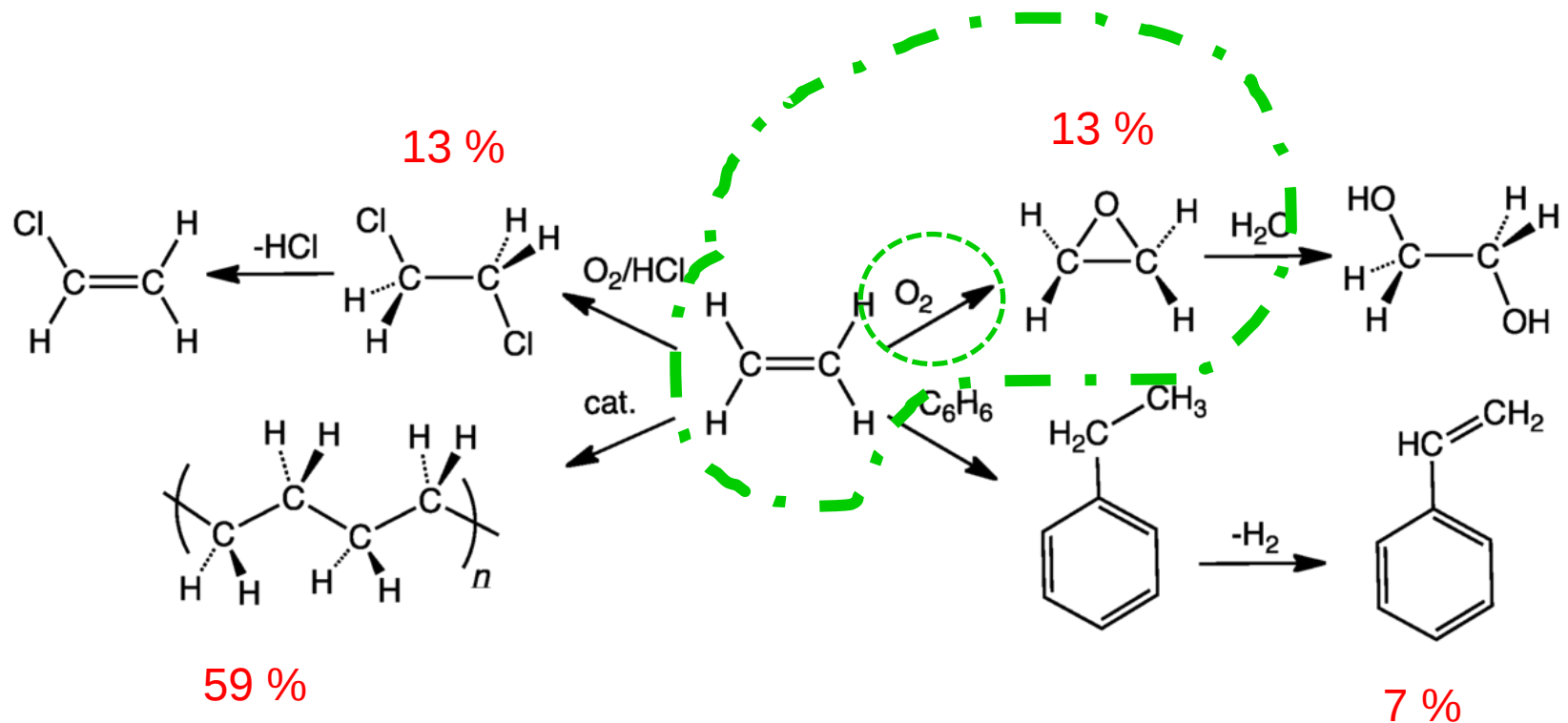


~4 % of Germany

http://www.researchandmarkets.com/research/2xl4dr/the_ethylene

The Ethylene Technology Report 2016: 7,000 \$

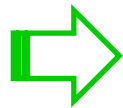
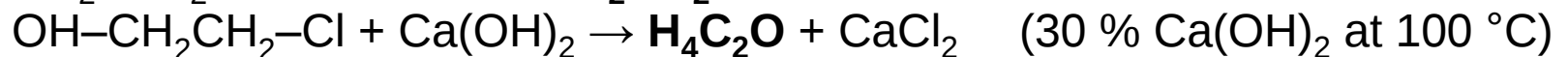
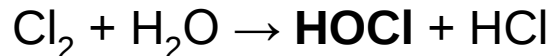
Ethylene Conversion



Ethylene Oxide Production

- World production capacity ~ 17 Mio tons/a
- Plant size: 400 kt/a
- Ethylene production (60-70 % invest for ethylene):

➤ 1863 Chlorohydrin process (Wurtz)

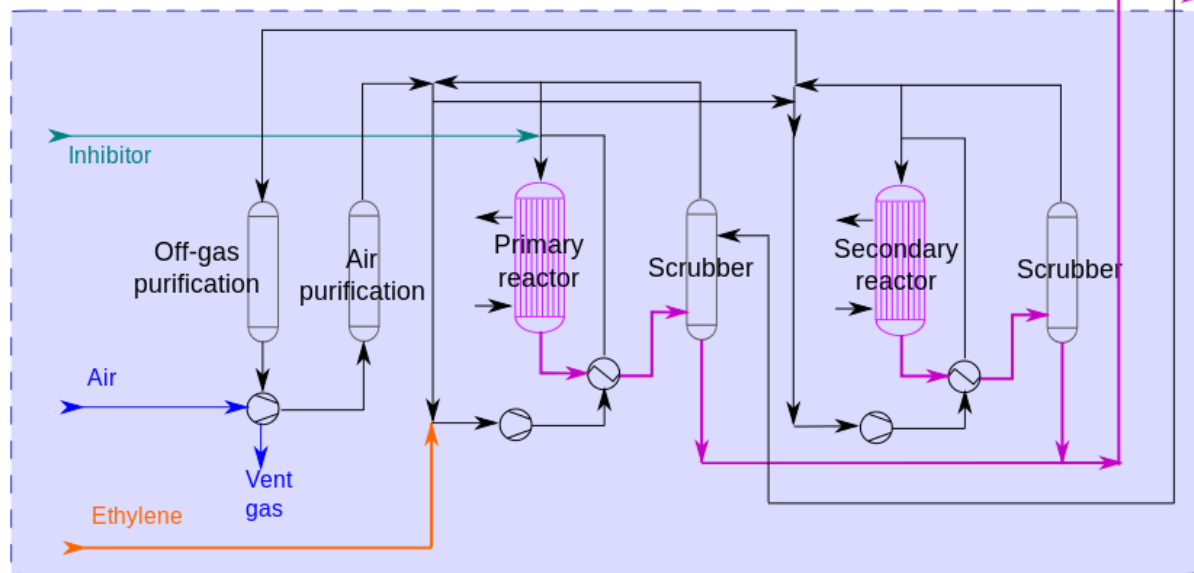
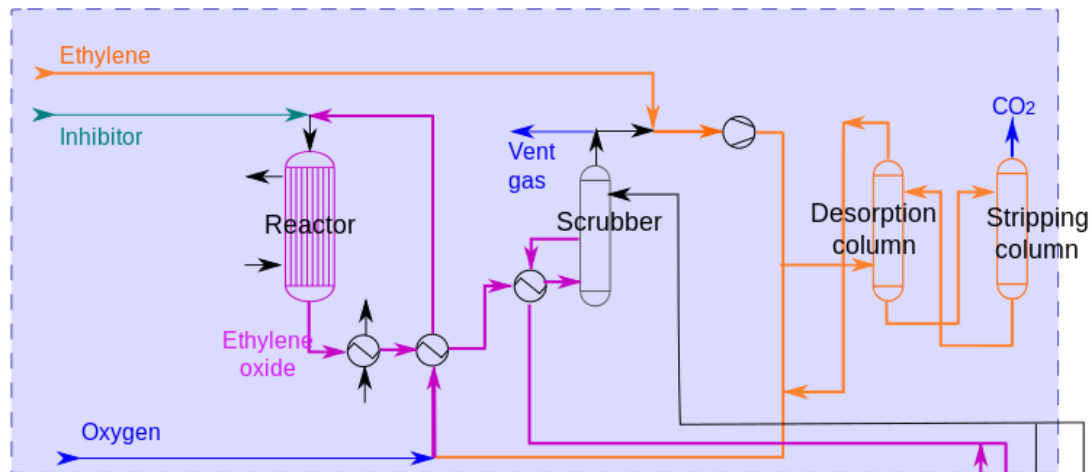


80 % S(EO)

- 1931 Direct oxidation with air (Lefort, Union Carbon → Dow)
- 1958 Direct oxidation with O_2 (Shell patent)

Catalyst: Ag supported on Al_2O_3 + promoters

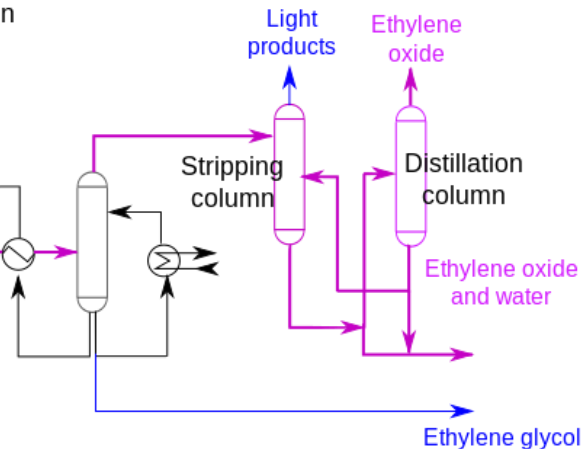
Oxygen process



Air process

Both:

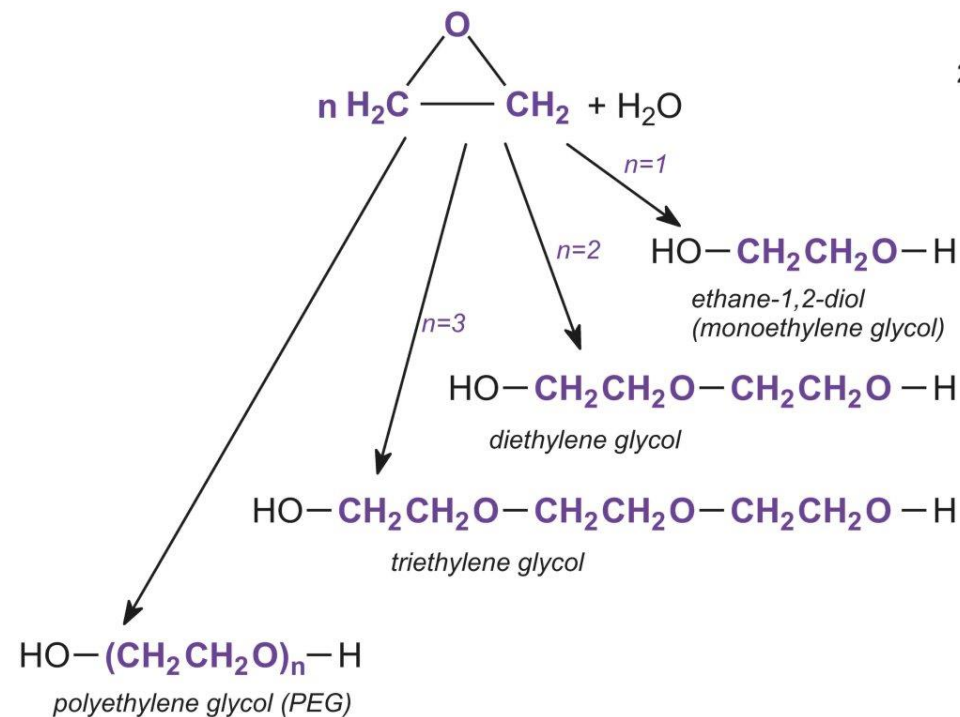
- reactor bundles of a few 1000 tubes
- recycle gas stream



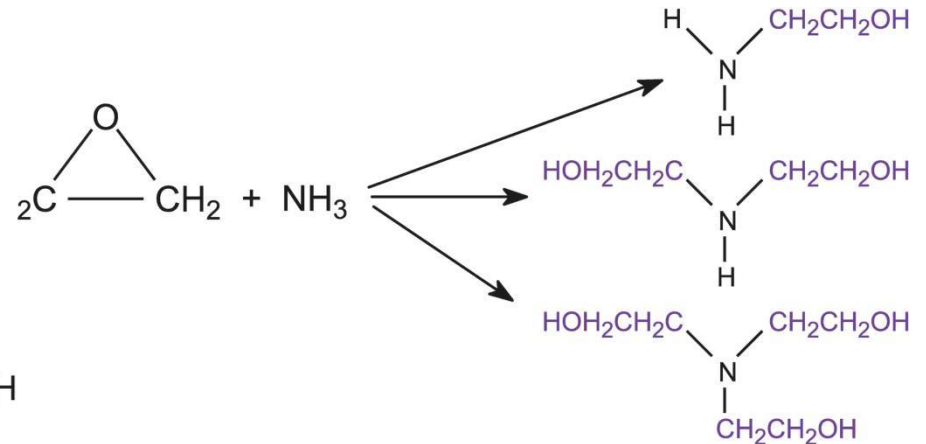
Differences:

- large amount of N_2
- most of the CO_2 vented
- higher conversion,
- less selective

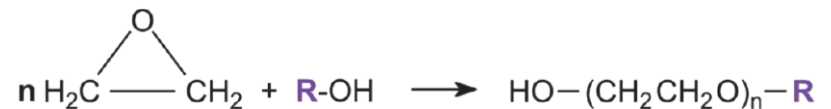
Ethylene Oxide Conversion



~ 67 % glycol + 12 % derivatives

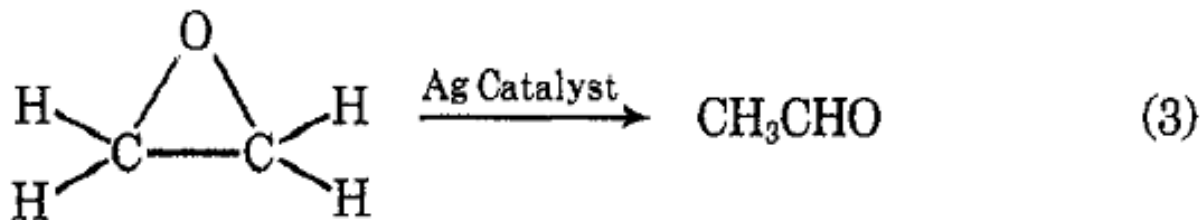
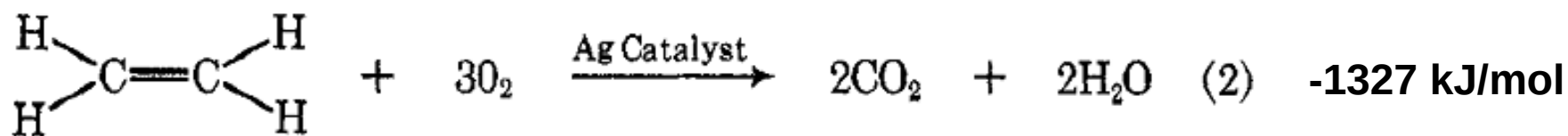
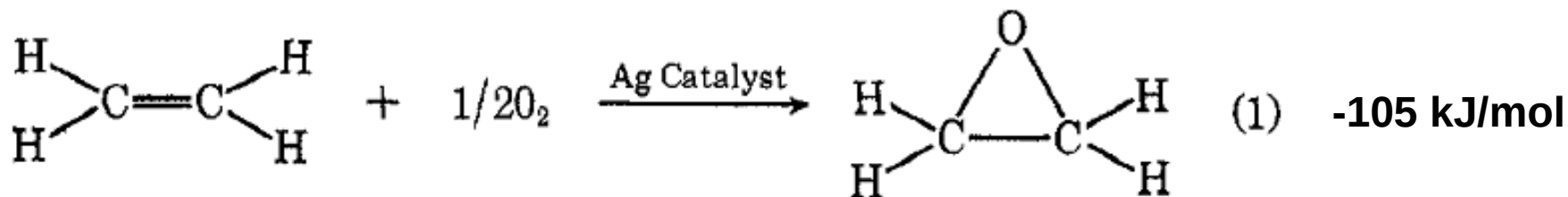


~ 7 % ethanolamine



~ 13 % ethoxylates

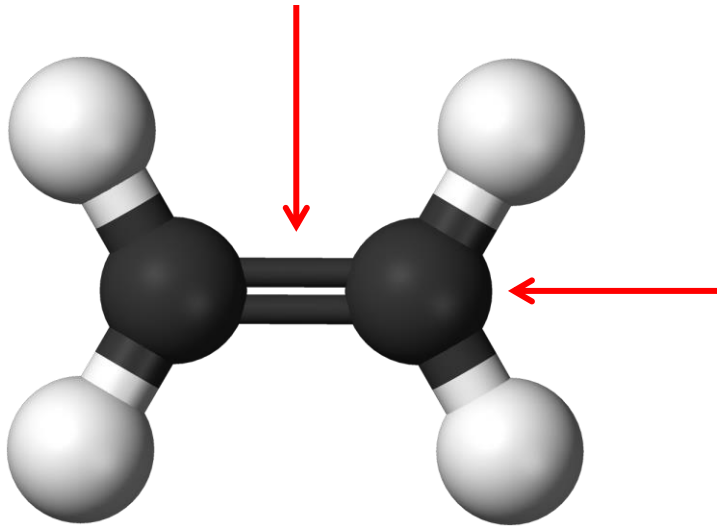
Ethylene + Oxygen



Important applied methods

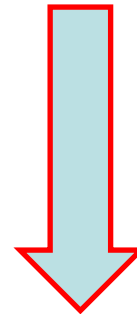
- **Desorption spectroscopy**
- **Raman and IR for the oxygen chemistry ($^{18}\text{O}_2$ isotope experiments), LEED**
- **XPS, EELS and XAS**
- **Electron microscopy**
- **Strong Theory support**

Activation of Ethylene



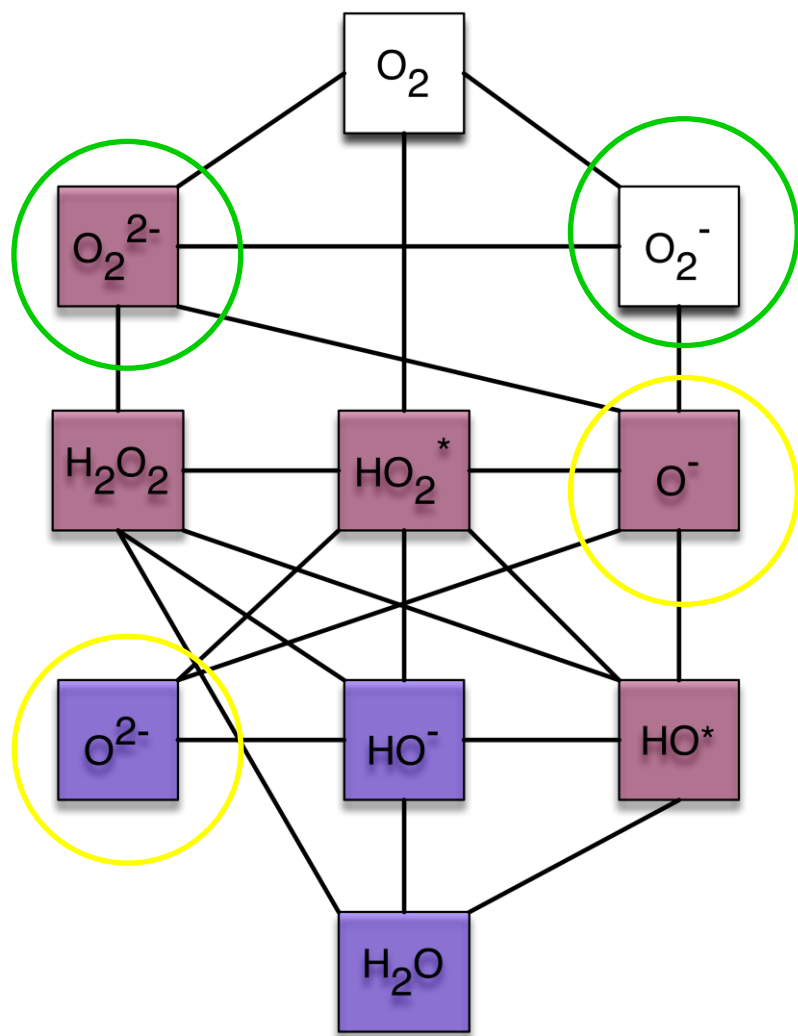
Ag or oxygen?

- fast adsorption /desorption
- low activation barrier (39-46 kJ/mol)



Increased 13 times
on oxidised surfaces

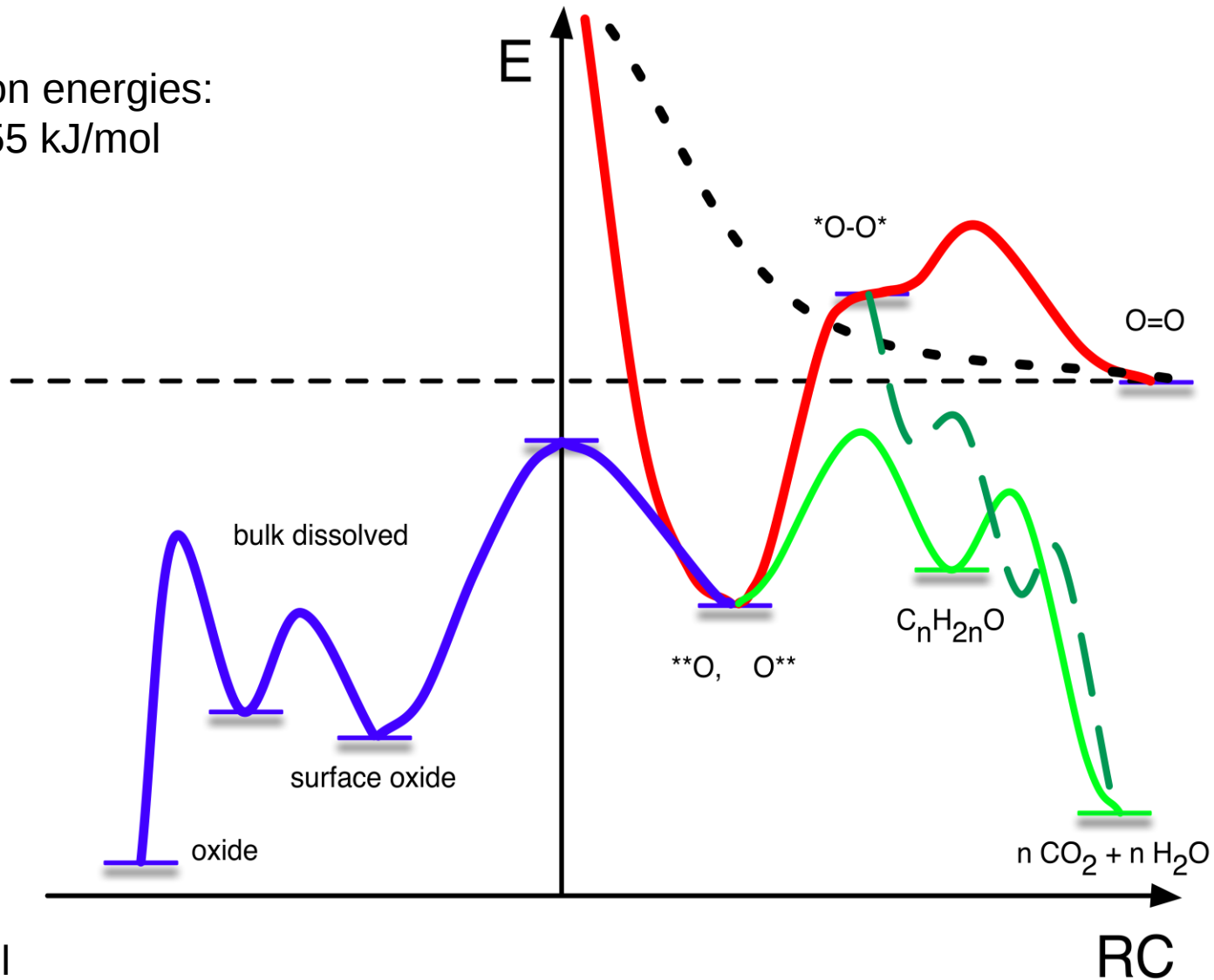
Activation of Oxygen



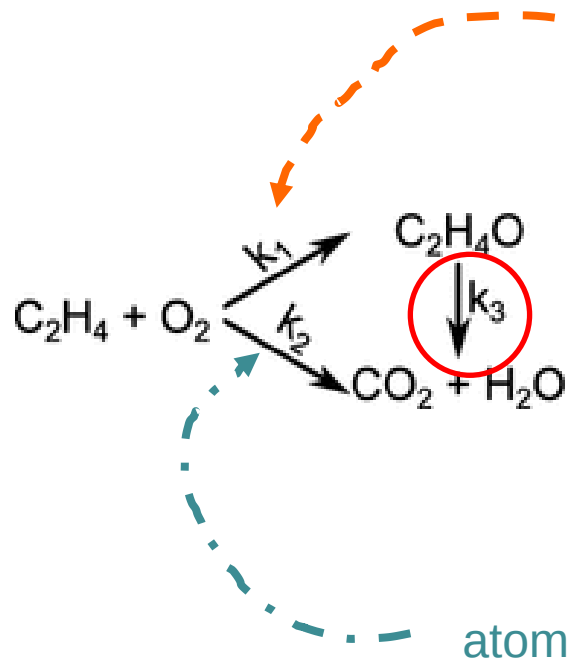
“A simple reaction network for the activation of oxygen. Hydrogen and an unnamed electron donor are needed. Red denotes the formal oxidation state -1 and blue the oxidation state -2”

Activation of Oxygen: dissociative?

Desorption energies:
140 – 155 kJ/mol

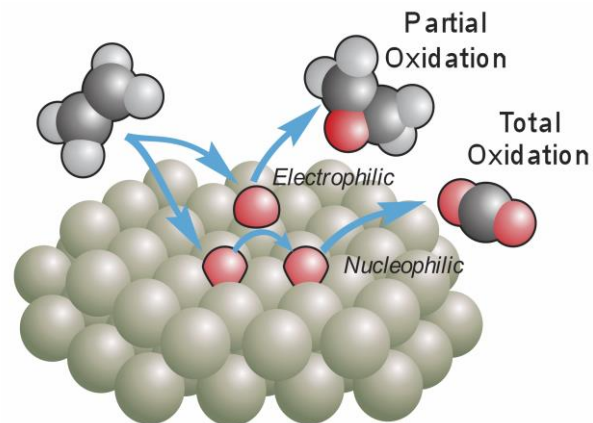
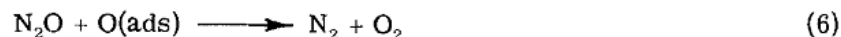


Molecular or atomic oxygen for EO?



Molecular oxygen: $\text{O}_{2,s}$

A similar conclusion regarding the nondissociative nature of oxygen on silver was reached by Herzog [98], who reacted ethylene with oxygen and nitrous oxide over silver catalysts. Although significant yields of ethylene oxide were obtained with oxygen, the use of nitrous oxide only produced CO_2 and H_2O except at higher temperatures where molecular oxygen is known to be produced due to the catalytic decomposition of nitrous oxide [99]:



Adsorption of EO on Ag? Isomerization!

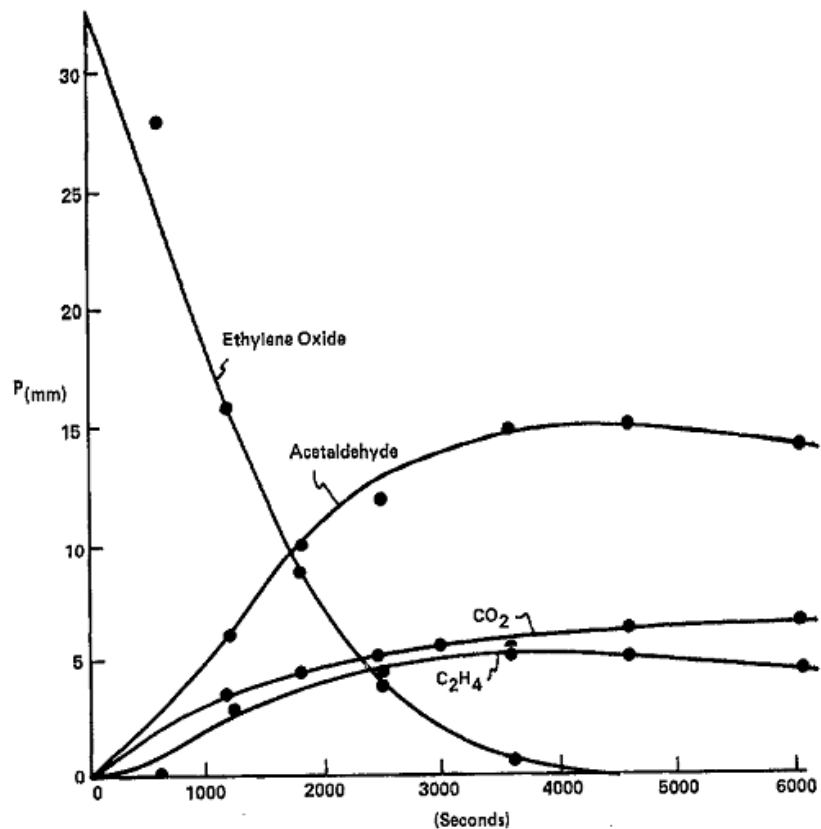
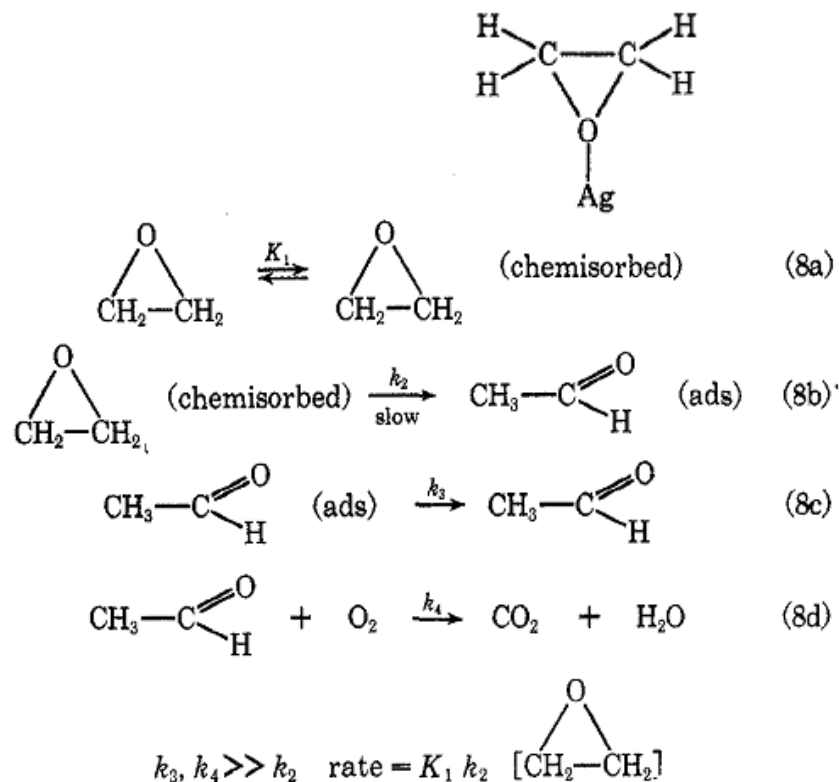
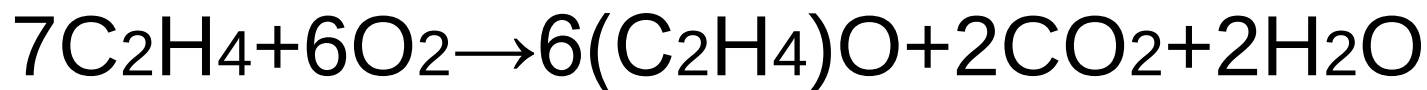


Figure 4. Plot of concentrations of reactants and products vs. time of kinetic run EO-1.



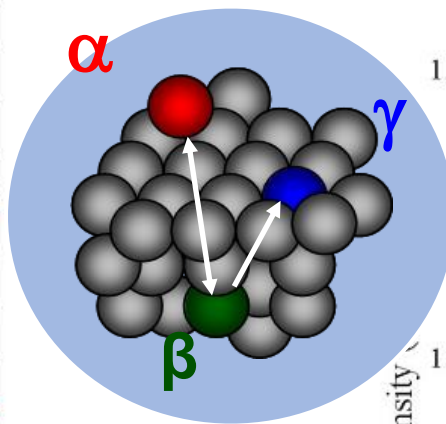
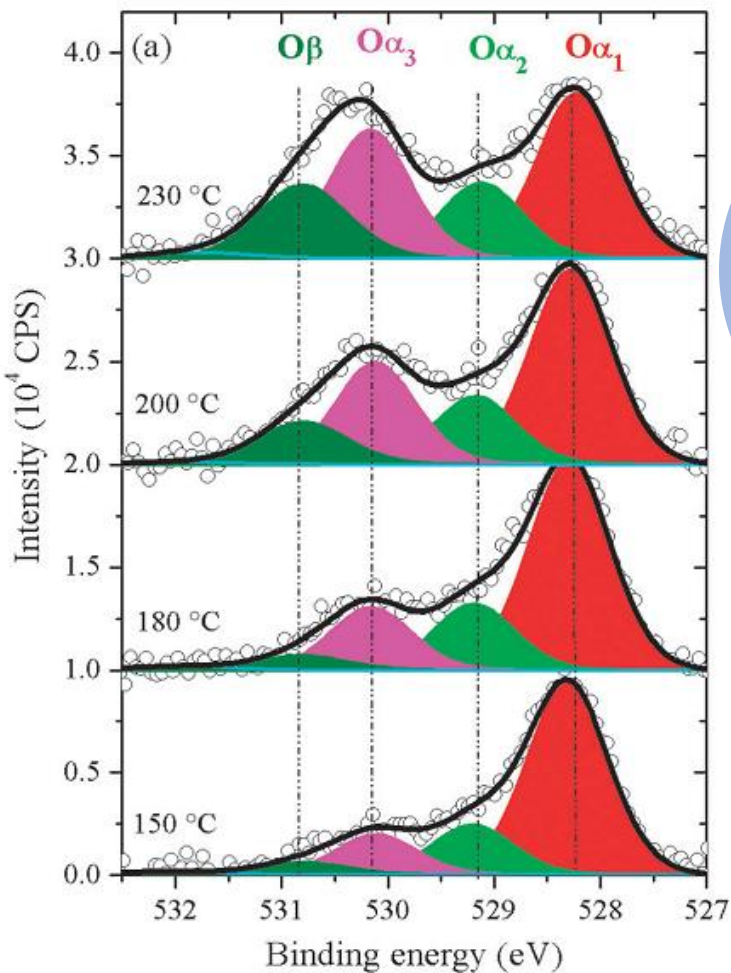
Molecular or atomic oxygen for EO?

**If only molecular oxygen,
selectivity limited to 87.5 % (6/7)!**

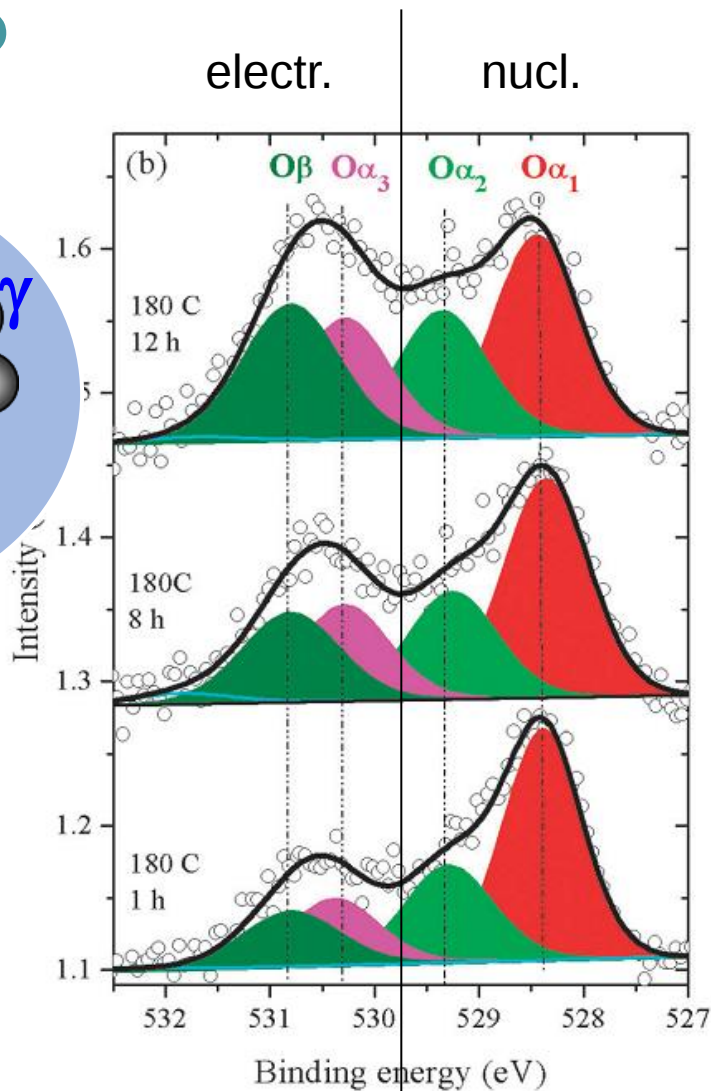


Atomic oxygen is involved!

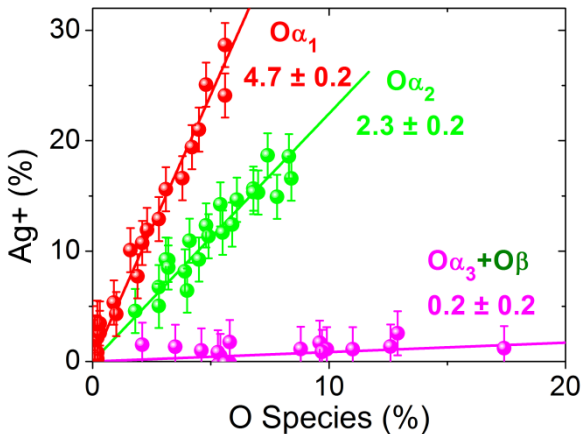
Which kind of oxygen species exist?



3 different on the surface + subsurface



exist?



Ag-O

charge transfer

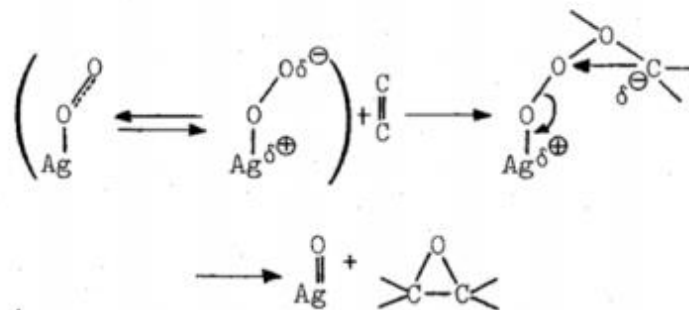
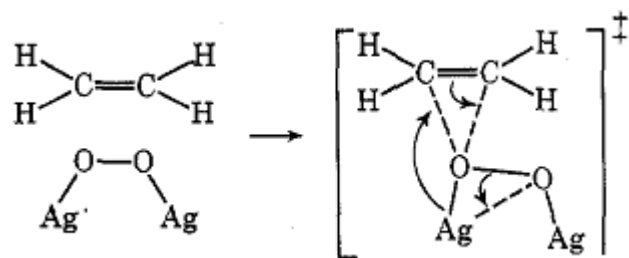
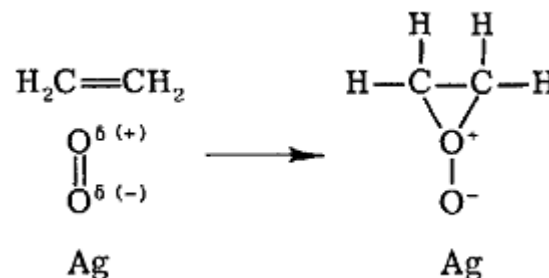
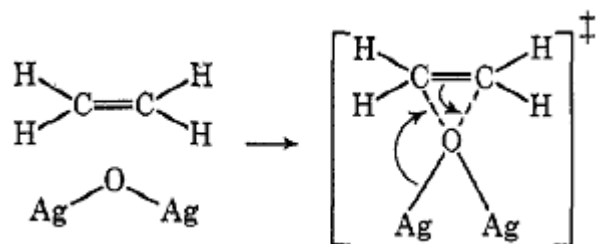
- Electrophilic O is “covalent O” : O_2 , SiO_x , SO_x , OH , CO_x , ...
- Nucleophilic O is “ionic O”: atomic O
- What about dynamics?

Let`s conclude: A complex situation?

- **Atomic and molecular oxygen is involved**
- **4 to 5 different oxygen species which co-exist:
nucleophilic + electrophilic**
- **Competing product formation:
Acetaldehyde or EO / Isomerization**
- **Surface dynamic**
- **No uniform mechanism**

Let`s conclude: A complex situation?

To cite this article: P. A. Kilty & W. M. H. Sachtler (1974) THE MECHANISM OF THE SELECTIVE OXIDATION OF ETHYLENE TO ETHYLENE OXIDE, Catalysis Reviews, 10:1, 1-16, DOI: [10.1080/01614947408079624](https://doi.org/10.1080/01614947408079624)

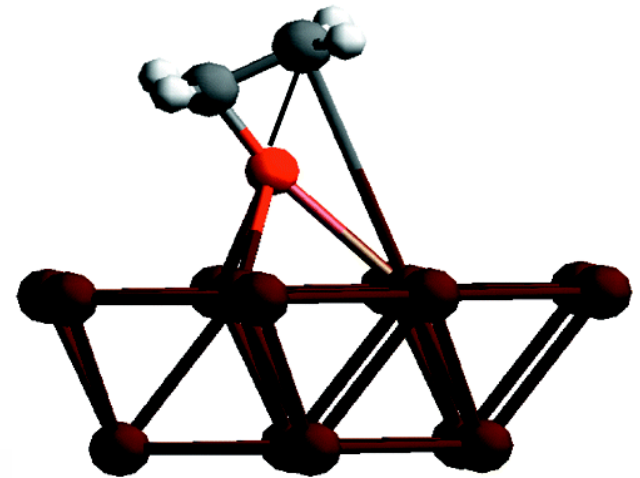
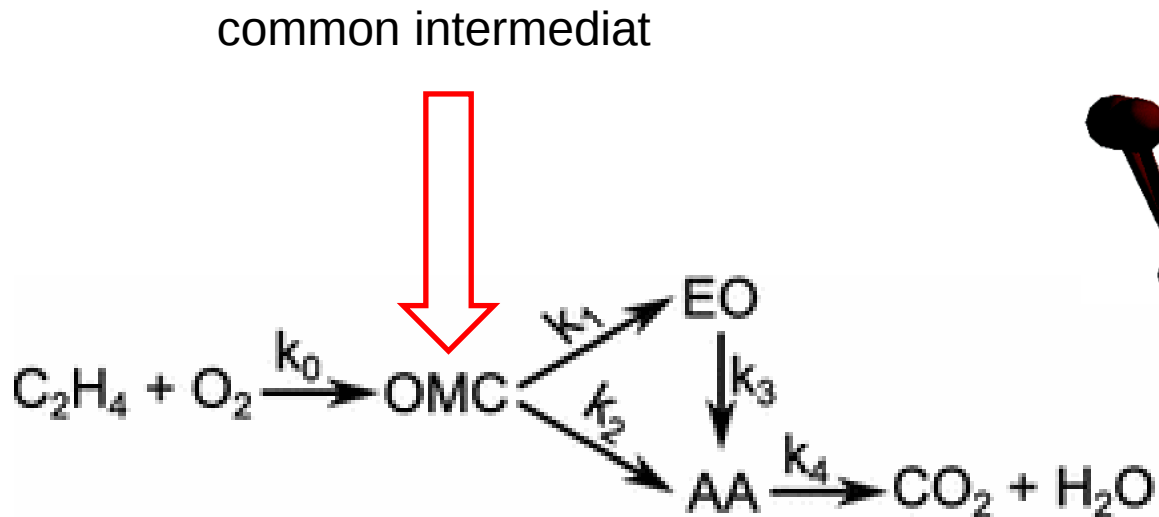


ROBERT E. KENSON AND M. LAPKIN

Volume 74, Number 7 April 2, 1970

CATAL. REV.—SCI. ENG., 23(1&2), 127-149 (1981)

A common stable intermediate: Oxametallacycle!



Stacchiola D, Wu G, Kaltchev M, Tysoe WT (2001) Surf Sci 486:9–23

Linic S, Medlin JW, Barteau MA (2002) Langmuir 18:5197–5204

Linic S, Barteau MA (2001) J Am Chem Soc 124:310–317

Oxametallacycle: What experimental evidence?

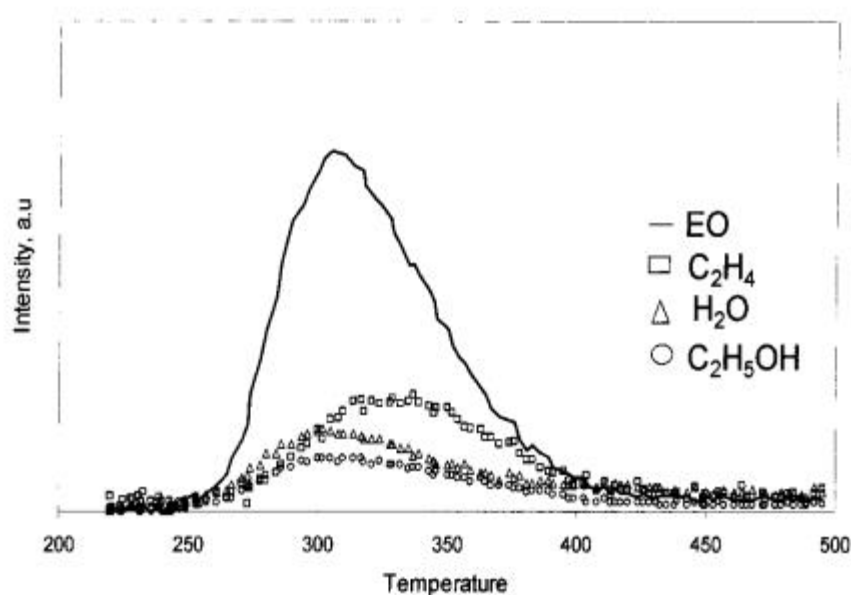


Figure 2. TPD spectra following a 250 K dose of EO on Ag(111).

b) molecularly adsorbed EO
c) Ring closure to OMC
in line with DFT prediction

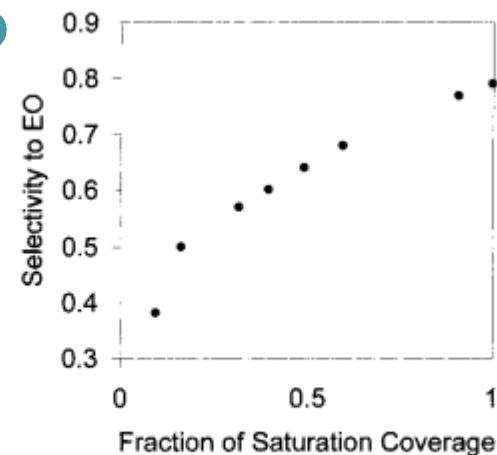


Figure 3. Selectivity to EO during TPD as a function of coverage of strongly bound intermediate, after 250 K dose.

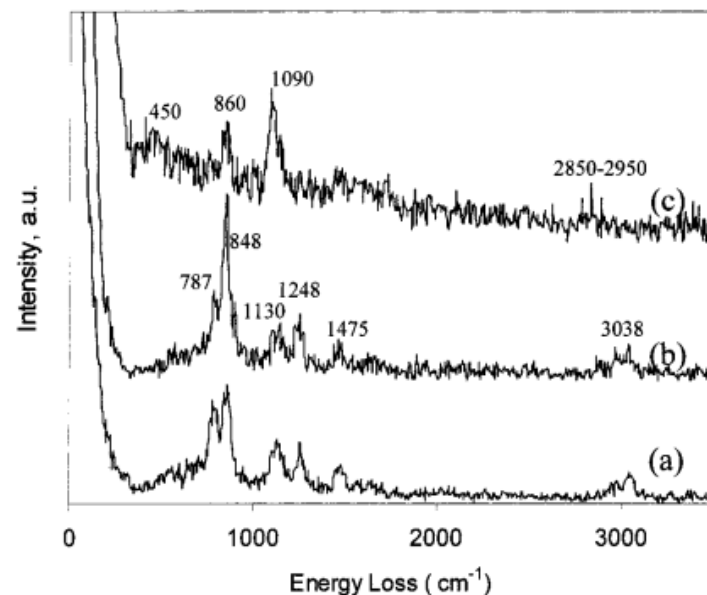
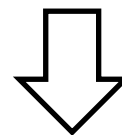
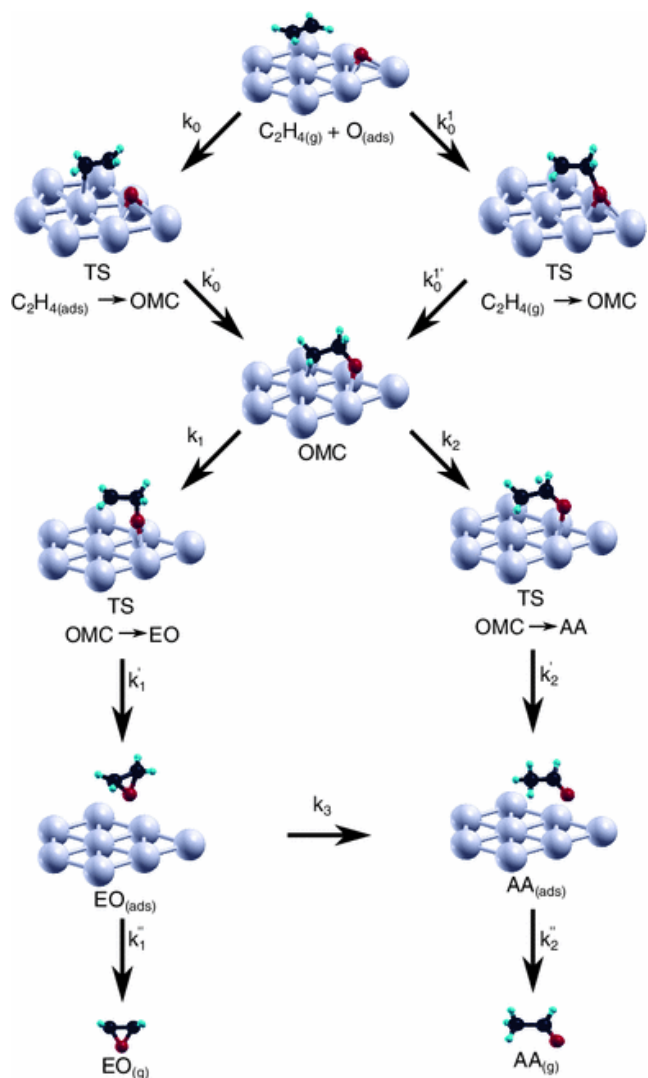


Figure 4. HREEL spectra collected after exposing EO to Ag(111) at varying dose temperatures. (a) 110 K; (b) 140 K; (c) 250 K.

Oxametallacycle: Langmuir-Hinshelwood mechanism



transition state

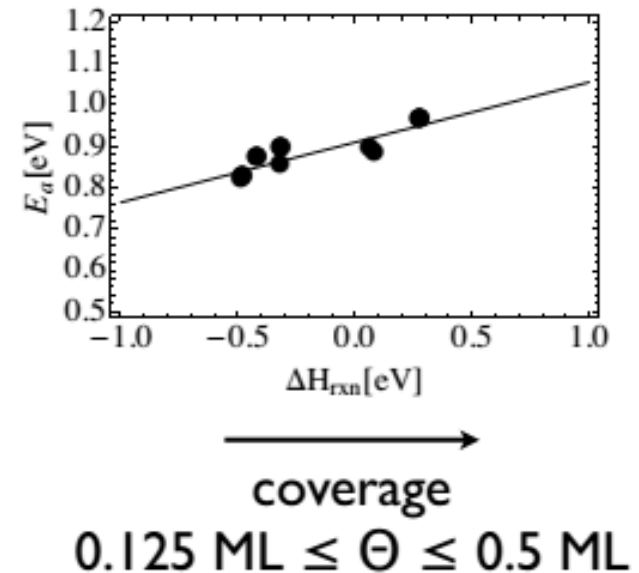
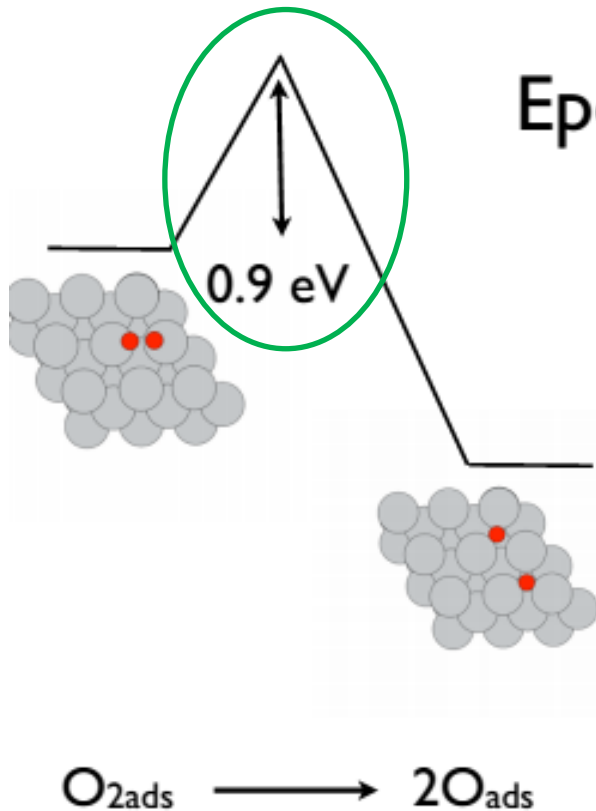
common intermediate

Product selectivity depends on the relative barriers:

$$E_{a,EO} \text{ vs. } E_{a,AA}$$

Let`s discuss the barriers

Atomic or molecular oxygen: dissociation barrier coverage dependend!

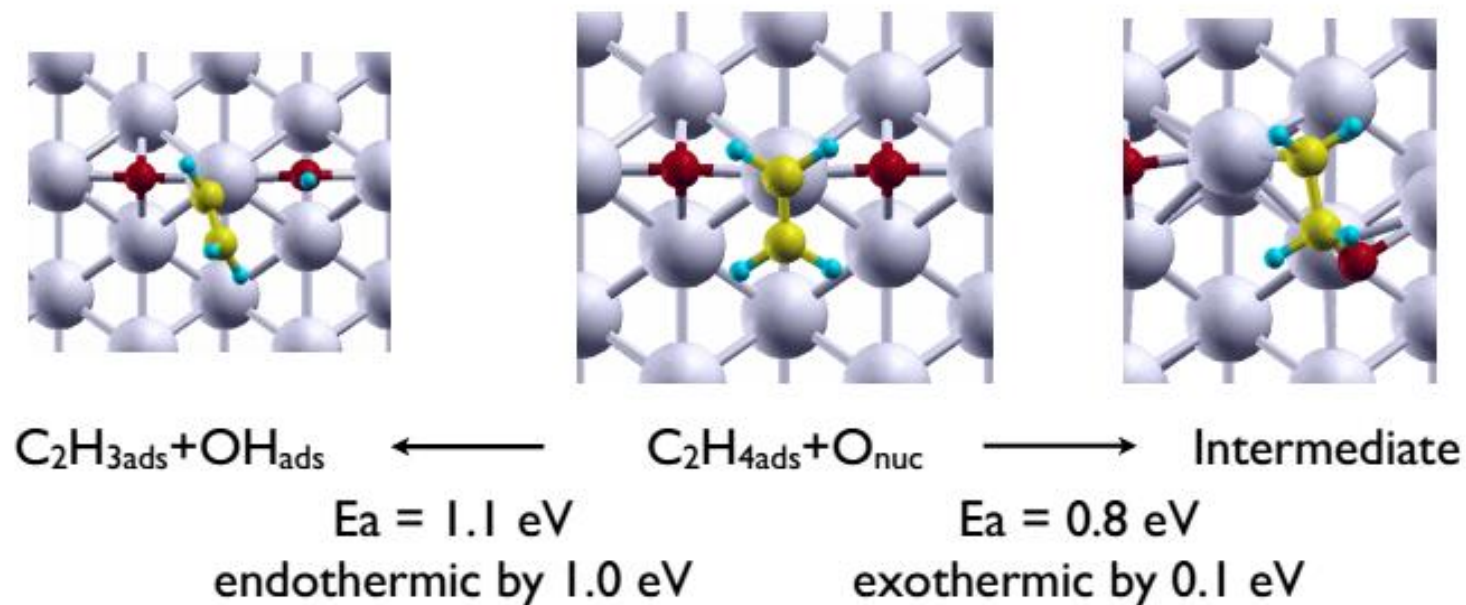


Ethylene pre-adsorbed reduces the barrier to 0.5 eV!

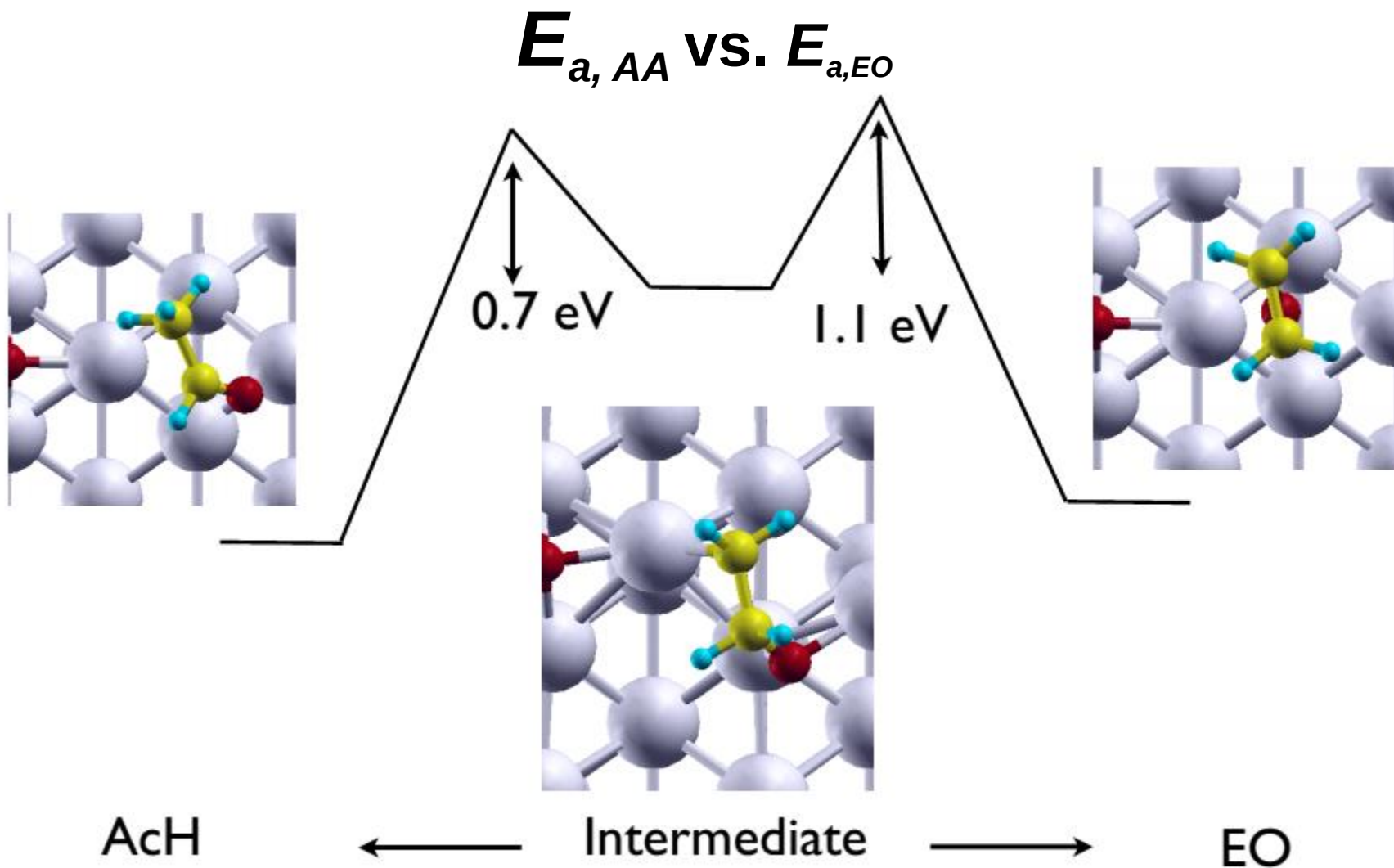
Let`s discuss the barriers

With nucleophilic oxygen direct combustion?

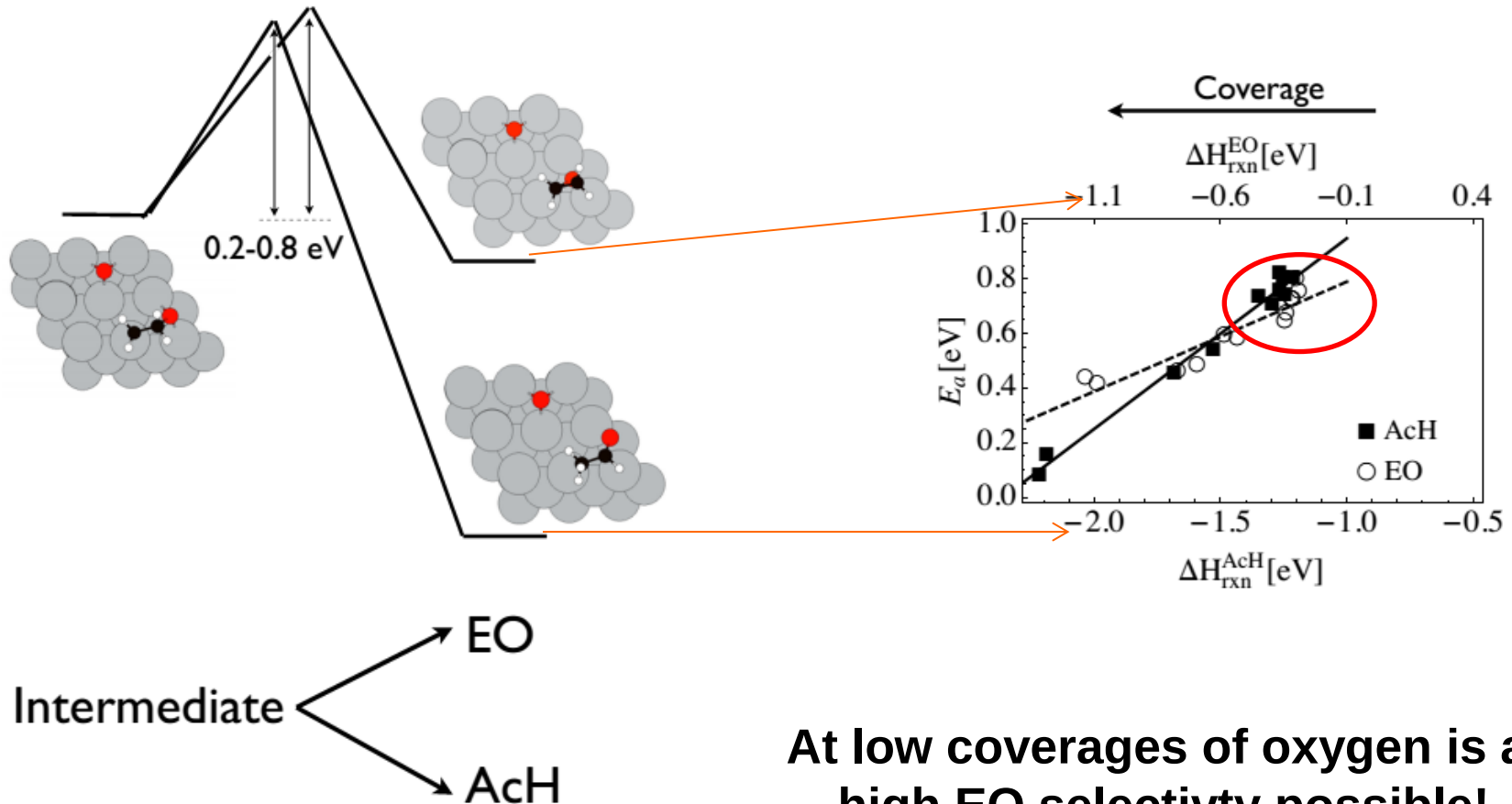
Epoxidation by O_{nuc}



Let`s discuss the barriers

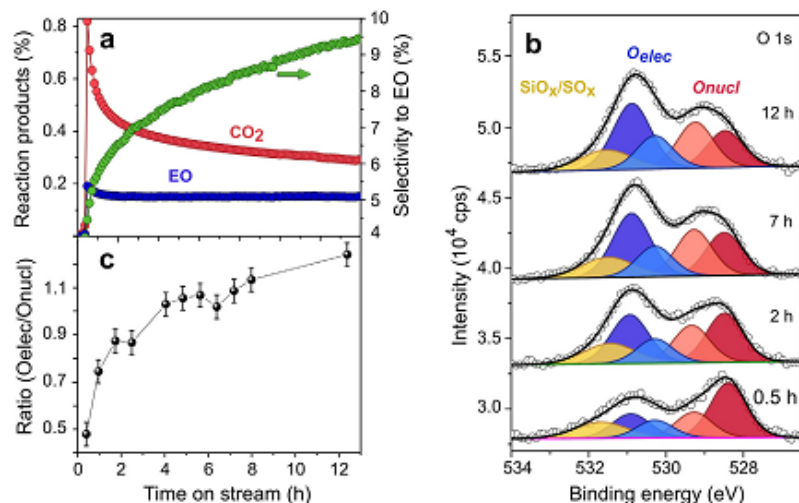


Let's discuss the barriers



At low coverages of oxygen is a high EO selectivity possible!

Co-feed with ethylene chloride: promotor and/or co-catalyst

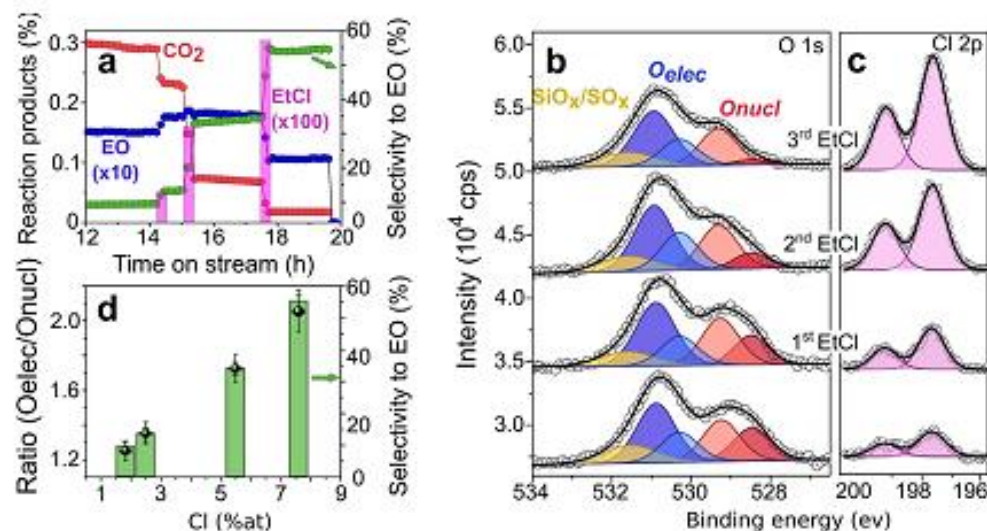


EC:

- oxygen management
- blocks active/unselective Ag-sites
- too much EC: Poisoning!

0.3 mbar, 230 °C, $\text{C}_2\text{H}_4:\text{O}_2 = 1:2$
+ pulsing with EC

0.3 mbar, 230 °C, $\text{C}_2\text{H}_4:\text{O}_2 = 1:2$

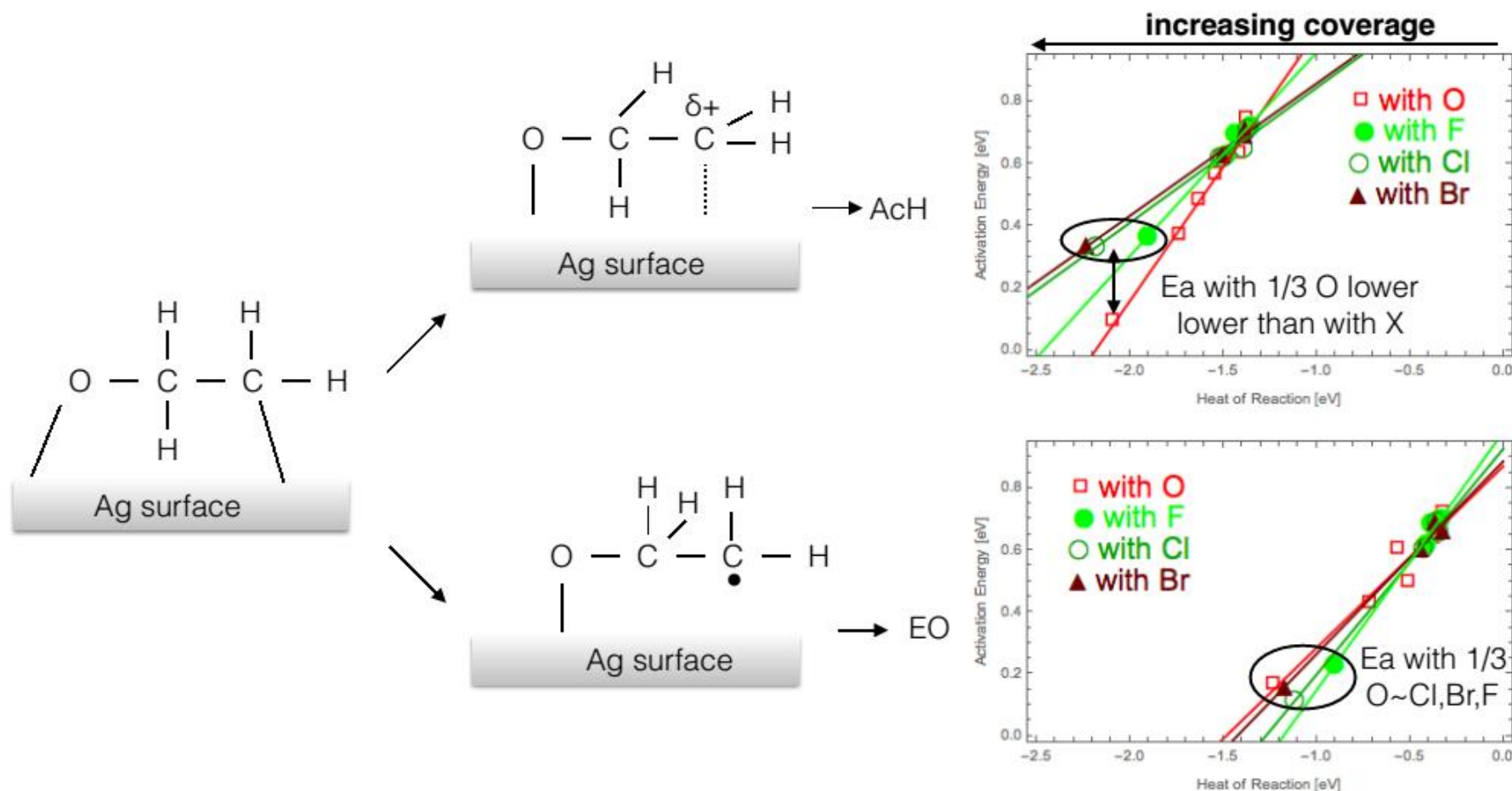


Co-feed with ethylene chloride: promtor and/or co-catalyst

Ethylene chloride effects:

- **oxygen management on the surface + in the bulk!**
- **blocks active/unselective Ag-sites**
- **prevents surface from reconstruction**
- **weakens the Ag-O bond, easier oxygen-transfer**
- **EC dosing + promoters has a strong impact on S(EO)**
- **too much EC: Poisoning!**

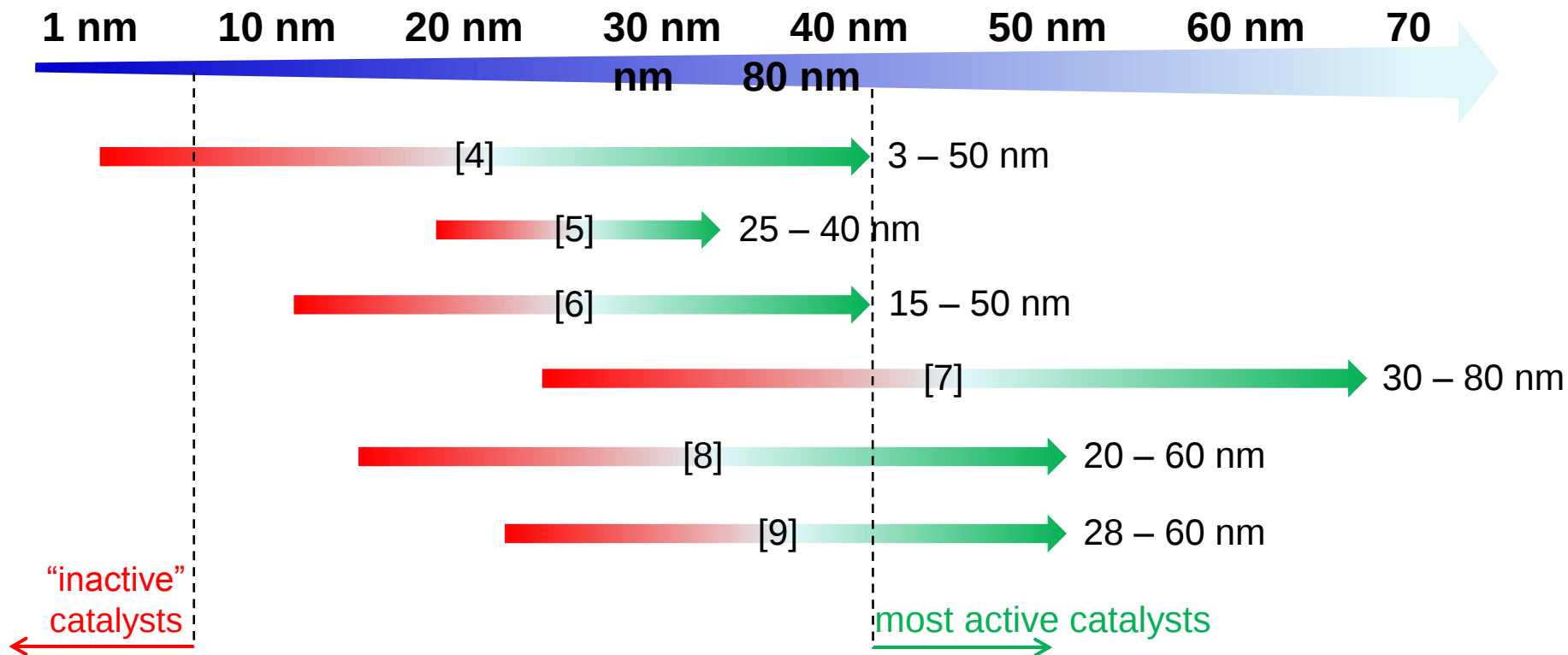
Co-feed with ethylene chloride: promtor and/or co-catalyst



The EO catalyst: Support + particle size

Ag particle size on supported catalysts

Arrows show increase in catalyst productivity with Ag particle size until a maximum is reached.



- Almost no selectivity observed for particles $< 2\text{nm}$ ^[4]
- Particles $< 10\text{ nm}$ are “known to exhibit no catalytic activity”^[8]

PhD-Proposal: M. Lamoth

[4] Wu and Harriott, *J. Catal.* **1975**, 39, 395-402 [5] Verykios *et al.*, *J. Catal.* **1980**, 66, 368-382 [6] Lee *et al.*, *Appl. Catal.* **1989**, 50, 17
 [7] Tsybulya *et al.*, *J. Catal.* **1995**, 154, 194-200 [8] Goncharova *et al.*, *Appl. Catal. A* **1995**, 126, 67-84 [9] Bukhtiyarov *et al.*, *J. Chem. Faraday Trans.* **1997**, 93, 2323-2329

The EO catalyst: Support + particle size

Carbides (SiC, TiC, ZrC, WC,)
Nitrides (TiN, ZrN, Si₃N₄, Zr₃N₄, Mg₃N₂)
Silicides (Fe₃Si, Ca₂Si, CaSi₂, TiSi₂,
WSi₂)
Oxides (α -Al₂O₃, BeO, CeO₂, ZrO₂,
MgO)
Borides (SiB₃, SiB₆, TiB₂, ZrB₂, FeB)
Spinel (MgAl₂O₄)
Silicates (MgSiO₃)



Inert supports

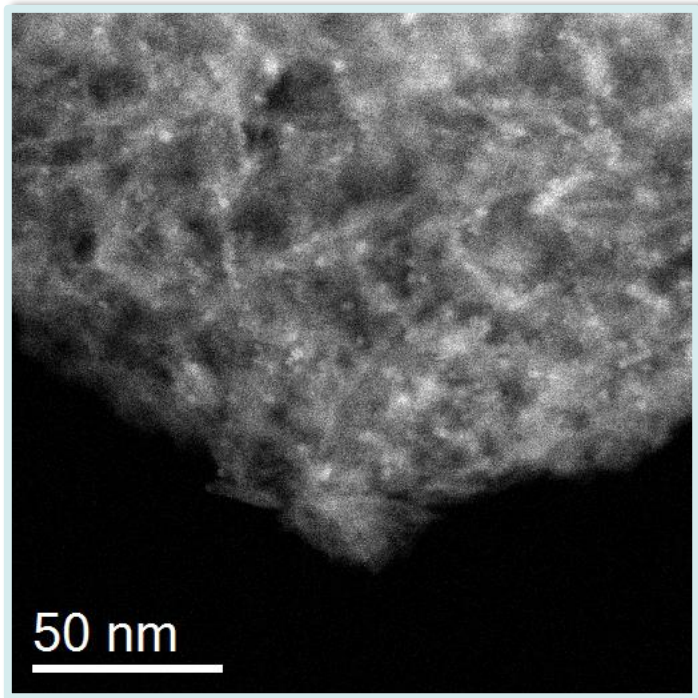
Active supports



Oxides (TiO₂, Fe₂O₃, MgO,
ZrO₂, FeTiO₃, CaTiO₃, SrTiO₃)
Zeolites (alumosilicates)
Transition-aluminas
Silicas
Silica-mixed oxides
(-titania, -alumina)
Carbonates (CaCO₃)

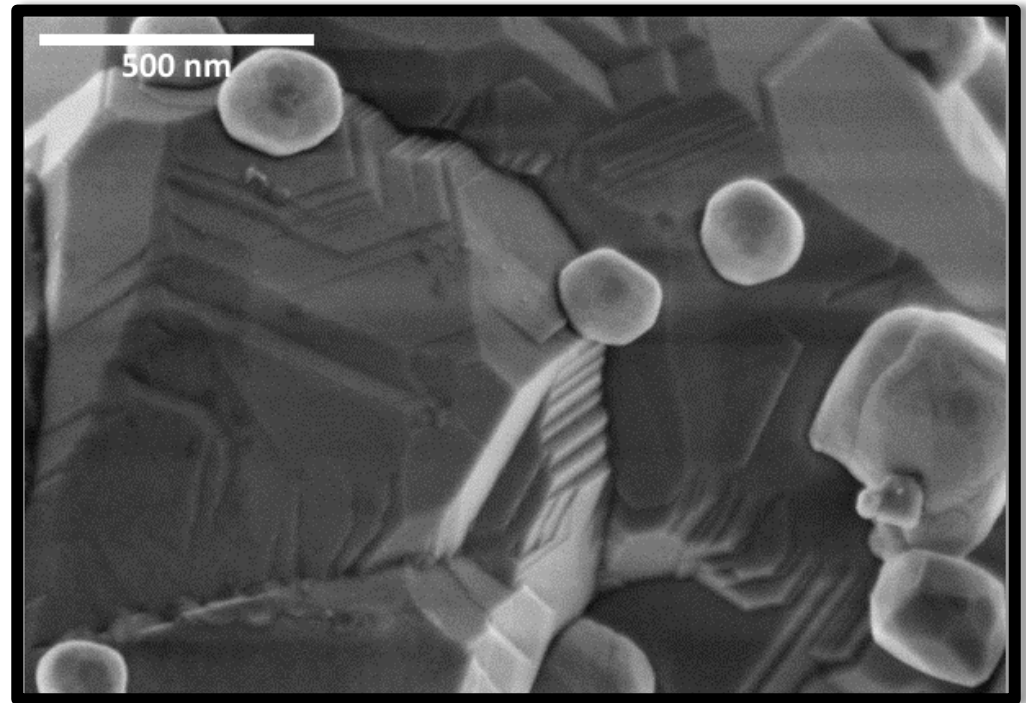
The EO catalyst: Support + particle size

Active supports



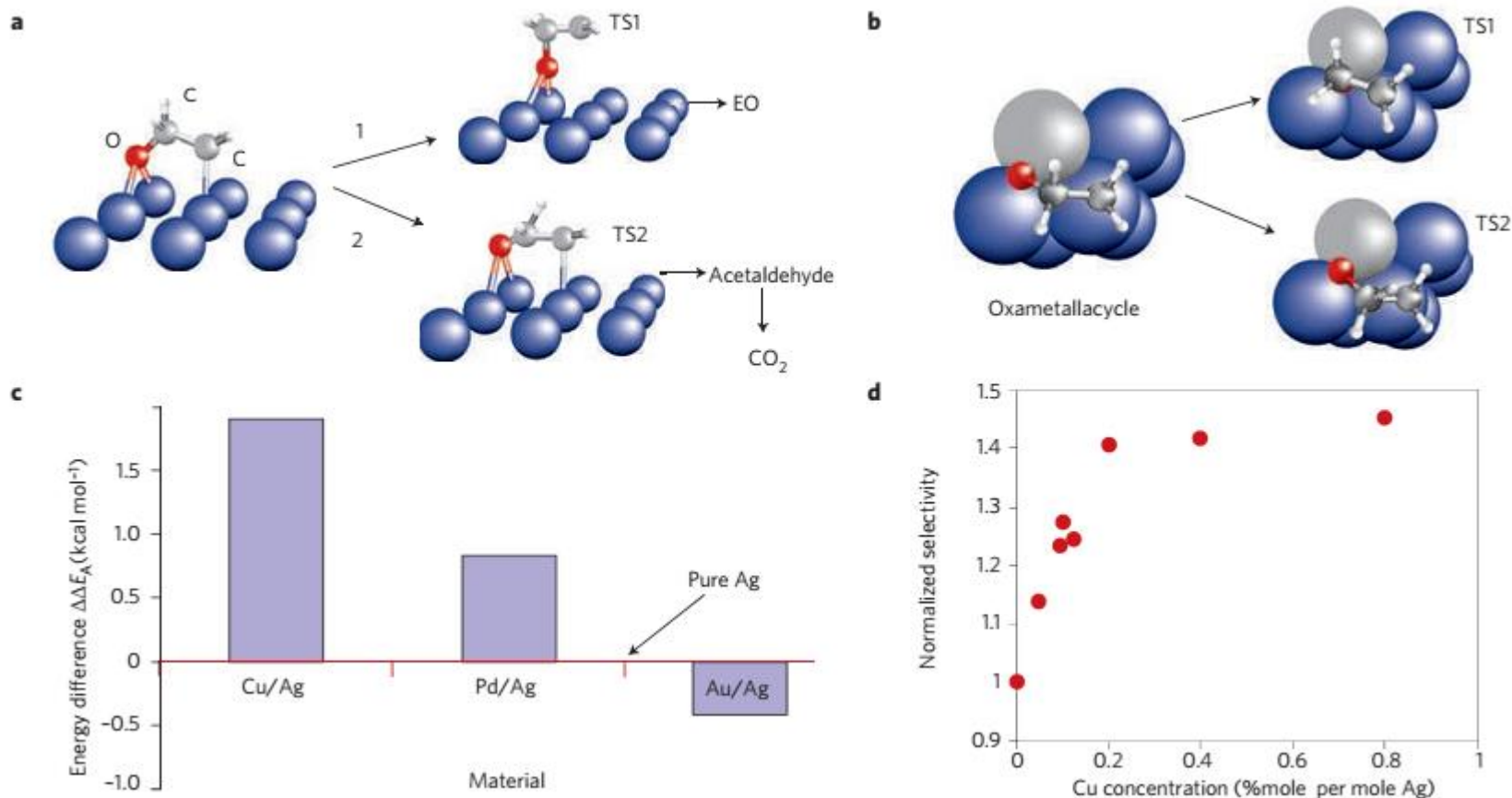
Siral 20 / 5 wt. Ag / calcined @ 500 °C

Inert supports



α -Al₂O₃ / 5 wt. Ag / calcined @ 500 °C

The EO catalyst: Perspectives!



$$\Delta\Delta E_A = (\Delta E_{TS2}(\text{alloy}) - \Delta E_{TS1}(\text{alloy})) - (\Delta E_{TS2}(\text{Ag}) - \Delta E_{TS1}(\text{Ag}))$$

nature chemistry| VOL 1 | APRIL 2009 | www.nature.com/naturechemistry

Linic, S., Jankowiak, J. & Barteau, M. A. Selectivity driven design of bimetallic ethylene epoxidation catalysts from first principles. *J. Catal.* 224,489–493 (2004).

Conclusion

- The ethylene epoxidation is an important industrial process via direct ox.
- The industrial catalysts is a $\text{Ag}@\alpha\text{-Al}_2\text{O}_3$ +promoters. Li, Cs, W, S, Re
- The O_2 -Ag chemistry is challenging and dynamic: nucl./electr./sub-surf.
- Molecular and atomic oxygen form EO
- The OMC is the most probable common intermediate + LH-mechanism
- The selectivity is strongly T and coverage dependent
- EC is an important co-feed and co-catalyst for the industrial process:
electronic + structural impact

Not discussed: Carbon (sub-surface), sulfur/sulfate promotion, Catalyst synthesis etc.