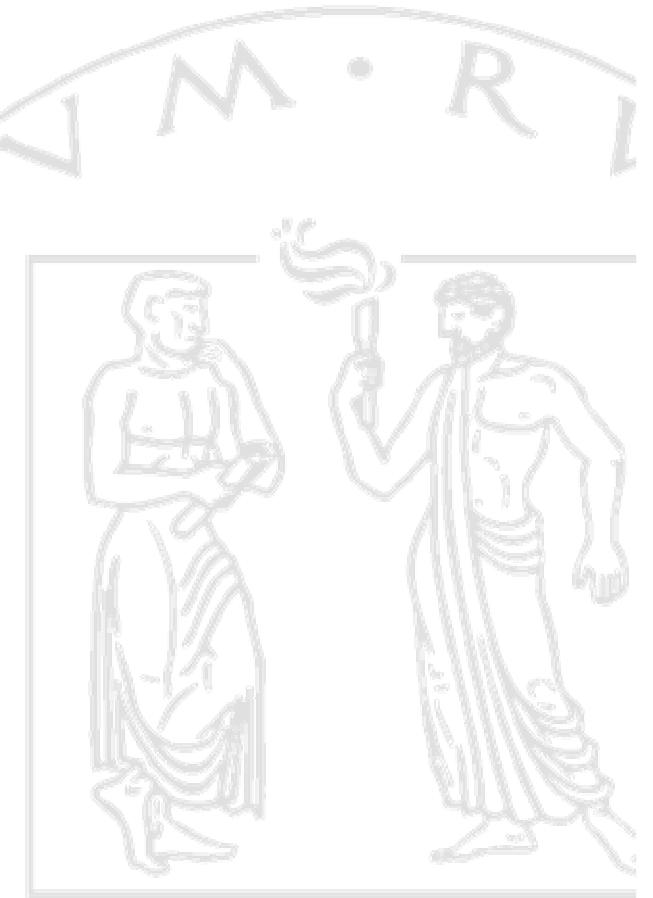
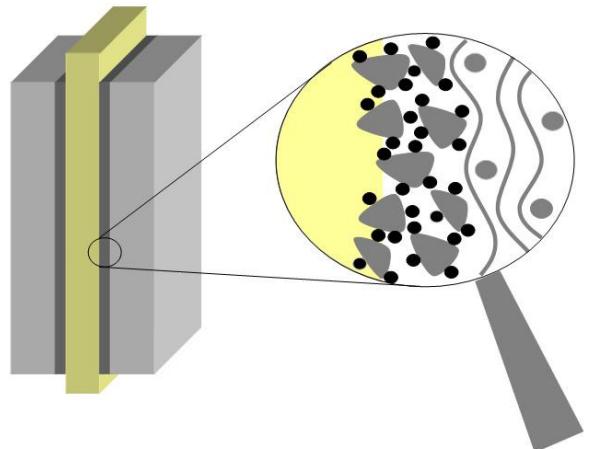


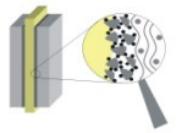
Electrocatalysis in fuel cells

Michael Bron

Nachwuchsgruppe Brennstoffzellen
Ruhr-Universität Bochum

Berlin, 01.02.2008





Outline

Principles of fuel cells and electrocatalysis

Important electrocatalytic reactions:

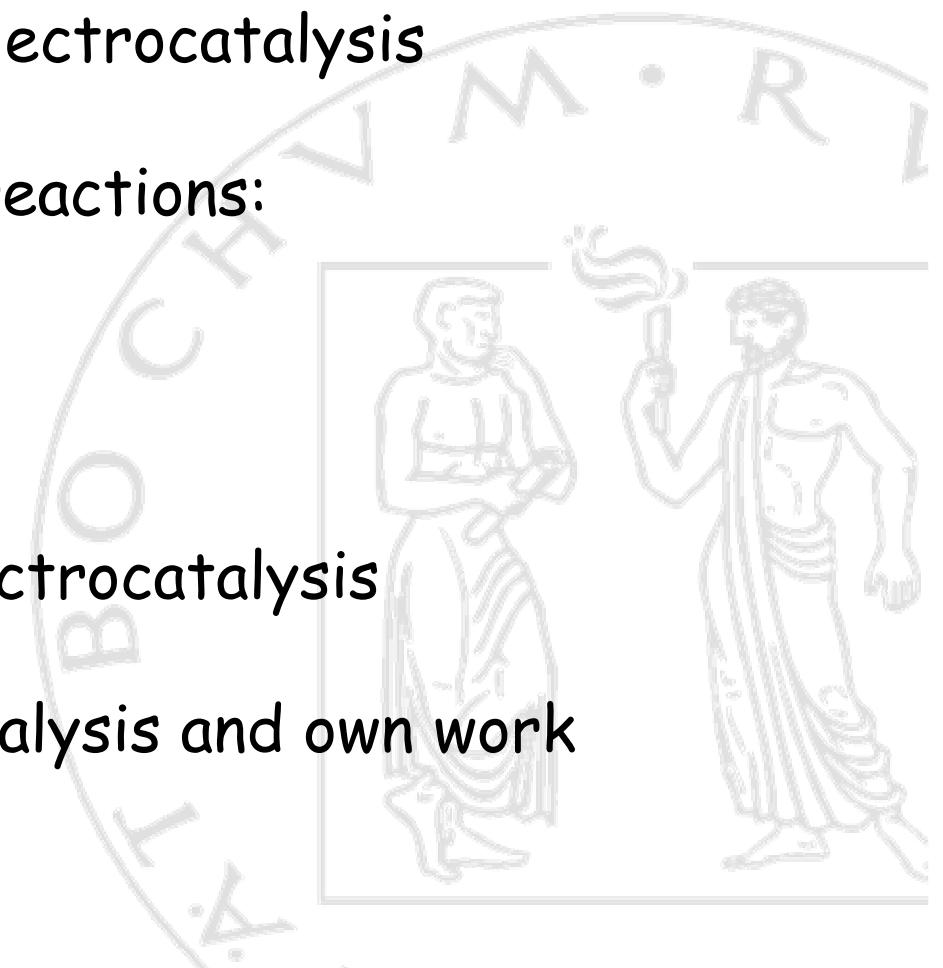
Oxygen reduction

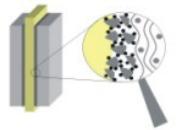
Hydrogen oxidation

Methanol oxidation

Experimental methods in electrocatalysis

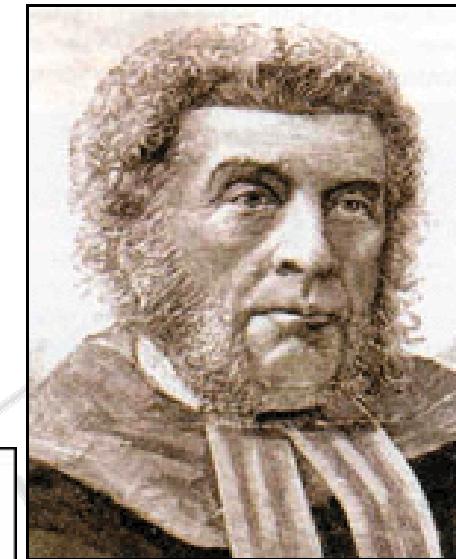
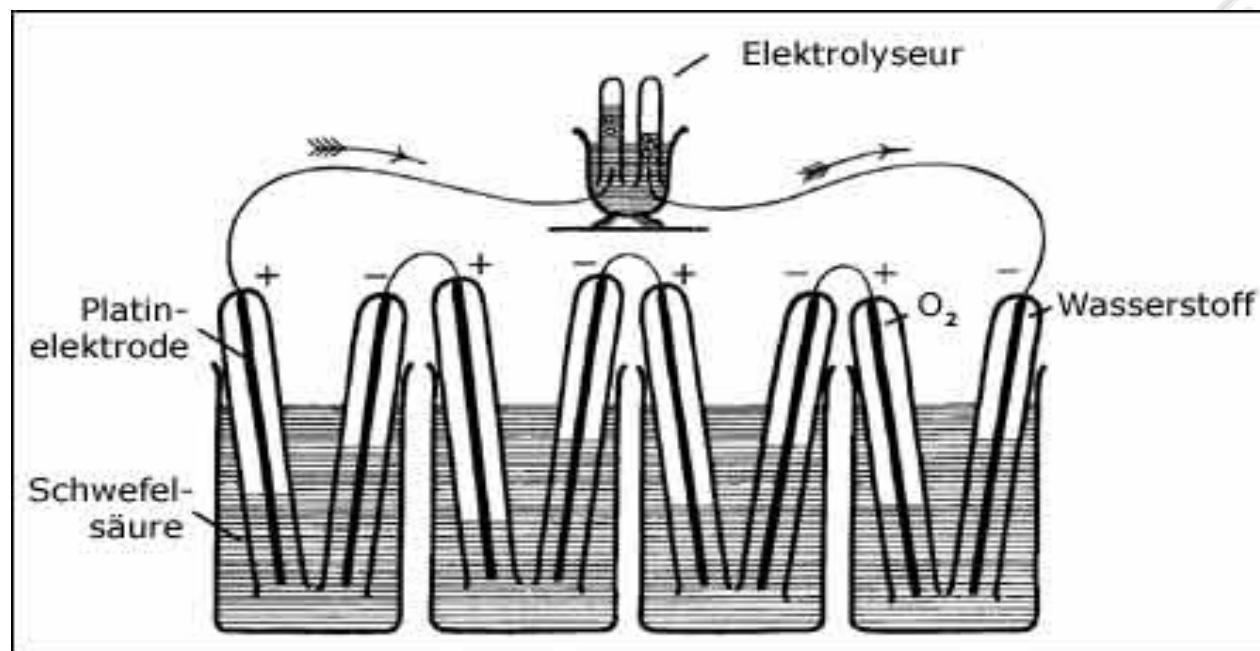
Current trends in electrocatalysis and own work



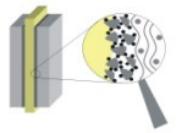


The “invention” of the fuel cell

Scheme of Groves fuel cell

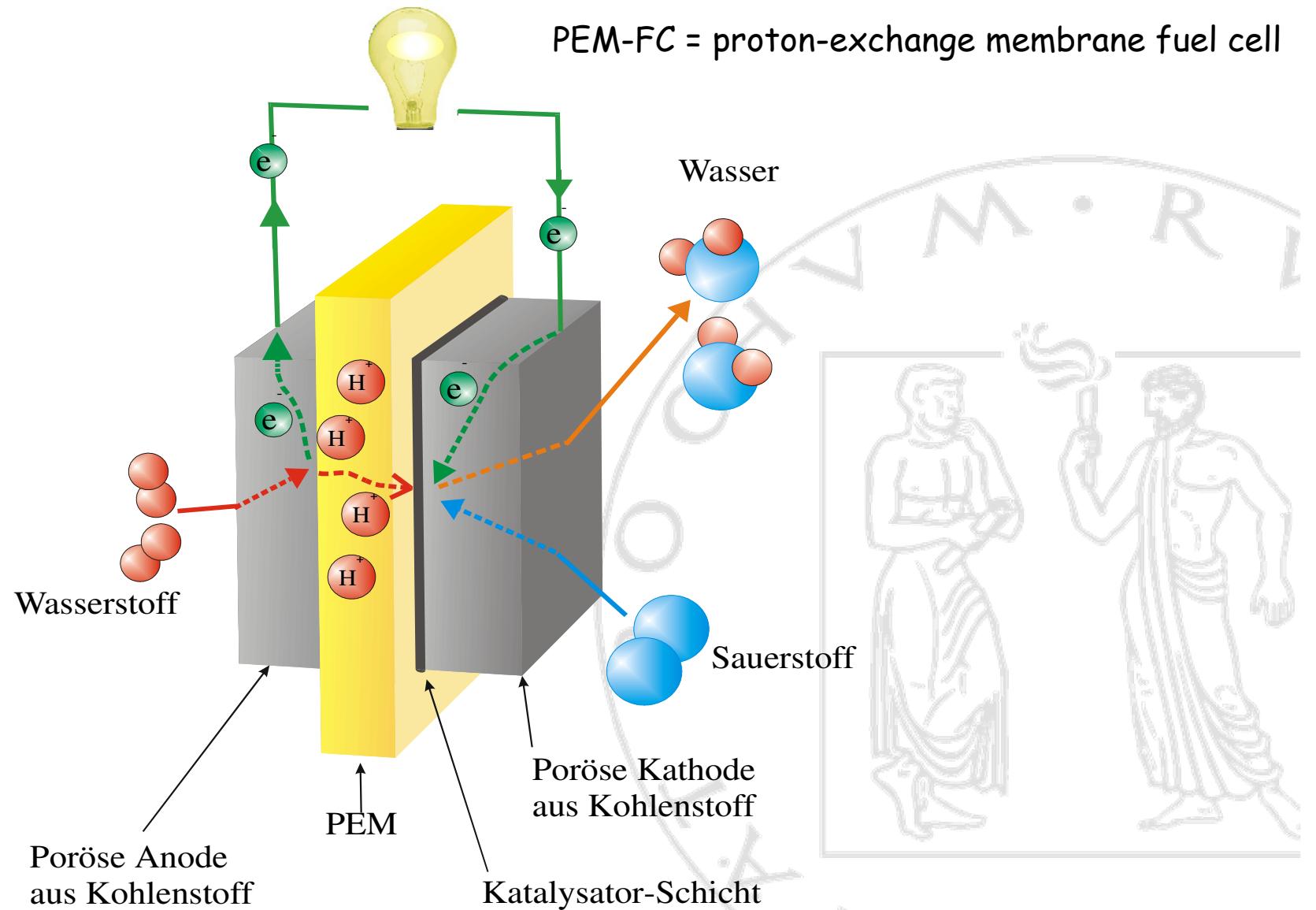


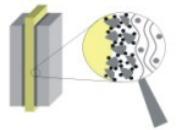
Sir William Robert Grove



Schematic setup of a PEM fuel cell

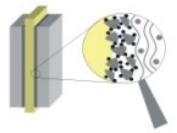
PEM-FC = proton-exchange membrane fuel cell





"HydroGen3", Opel/GM





Components of the "HydroGen3", Opel/GM



FC-Stack



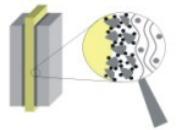
Liquid hydrogen tank



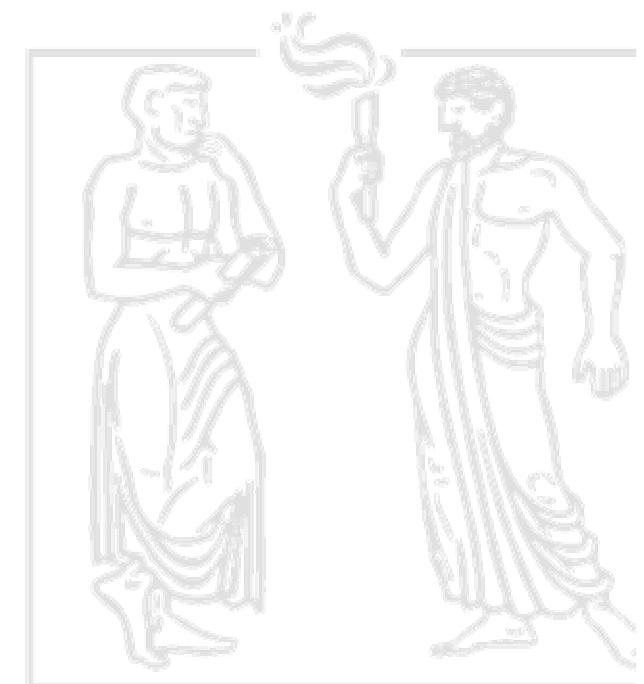
Pressure tank



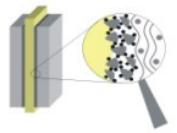
Fuel cell



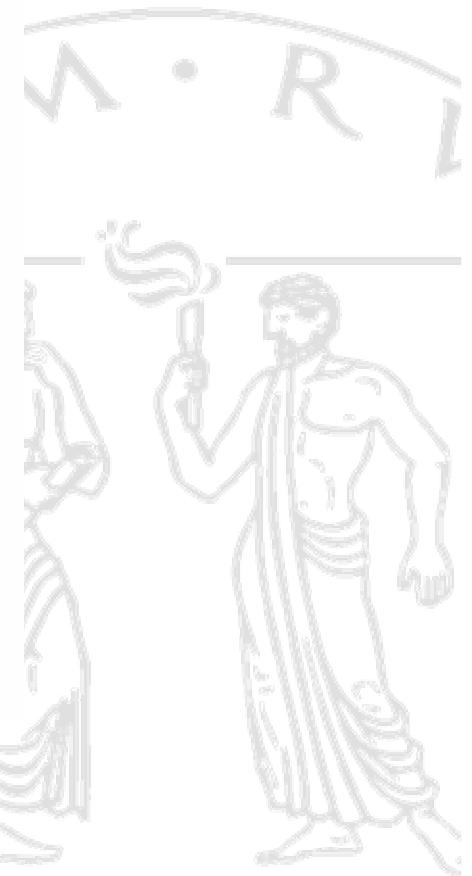
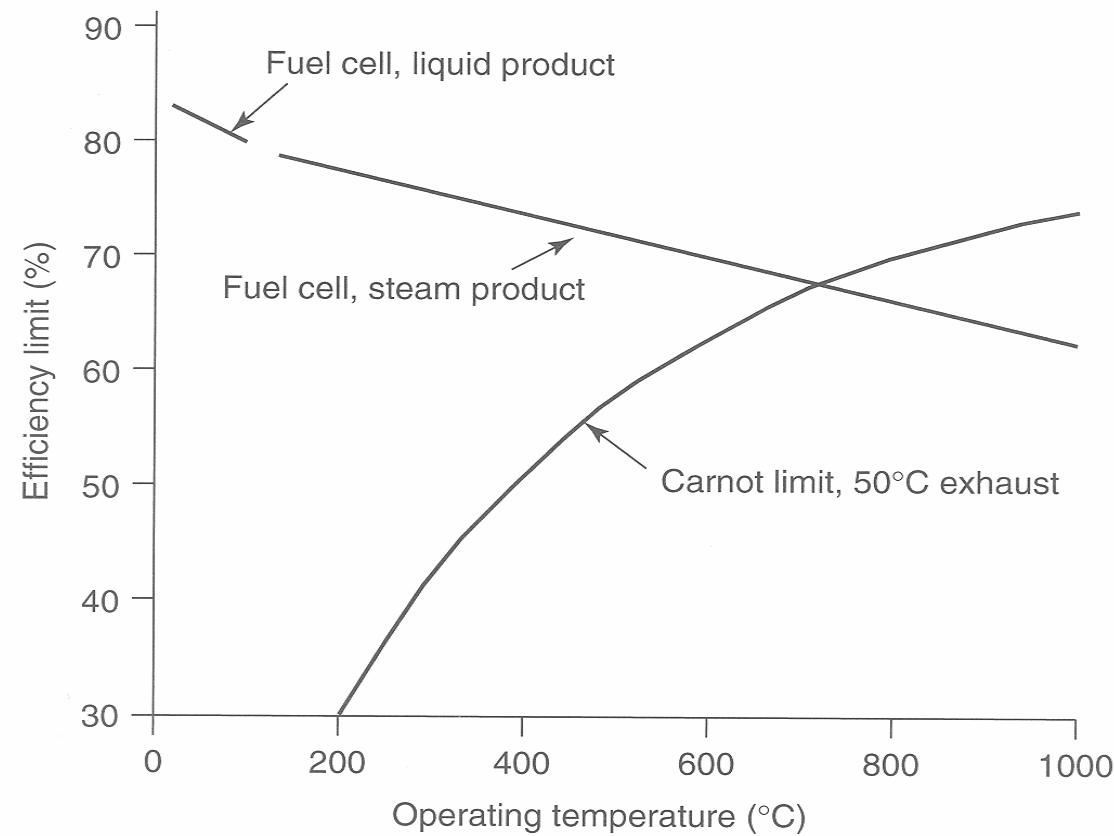
Direct methanol fuel cell (DMFC)
12 V/25 W
120 ml MeOH-cartridges
> 7 h power supply
1.1 kg overall/150 g per cartridge



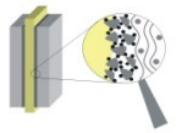
www.smartfuelcell.de



Comparison: Efficiency limit of Carnot process and fuel cell

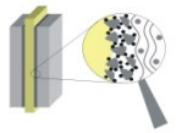


Taken from: "Fuel Cell Systems Explained", J. Larminie, A. Dicks, Wiley 2003

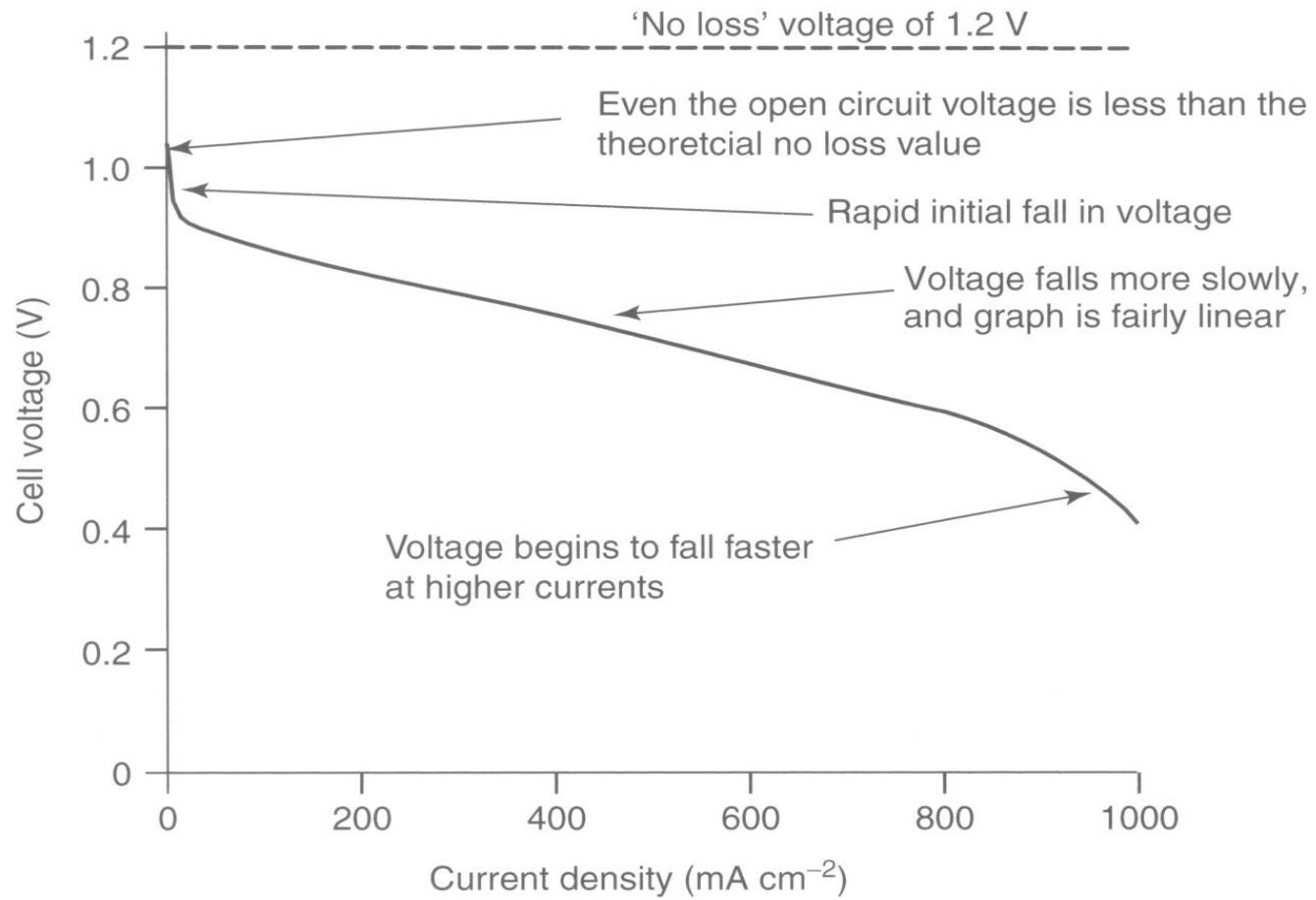


Overview: different types of fuel cells

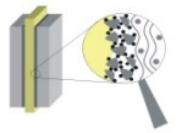
Name	Alkaline Fuel Cell (AFC)	Polymer Electrolyte Membrane Fuel Cell (PEM-FC)	Direct Methanol Fuel Cell (DMFC)	Phosphoric Acid Fuel Cell (PAFC)	Molten Carbonat Fuel Cell (MCFC)	Solid Oxide Fuel Cell (SOFC)
Electrolyte	KOH	Proton-Exchange-membrane	PEM	H_3PO_4 (immobilis.)	LiKCO_3	Zr(Y)O_2
Operating temperature	50-200 °C	30-100 °C	20-90 °C	190-220 °C	650 °C	800-1000 °C
Reactands	H_2 , $\text{NH}_2 \text{NH}_2$, O_2	H_2 O_2/Luft	MeOH O_2/Luft	H_2 O_2/Luft	H_2 , $\text{CH}_4\ldots$ O_2/Luft	H_2 , $\text{CH}_4\ldots$ O_2/Luft
Catalysts	A: Raney-Ni K: Ag	A: Pt/C K: Pt/C	A: PtRu/C K: Pt/C	A: Pt/C K: Pt/C	A: NiCr-Leg. K: LiNiO	A: NiZrO_2 K: LaSrMnO_3
Electrical Efficiency	60 %	55 %		40 %	55 %	55 %
Area of Application	Space flight, navy	Mobile applications 50-100 kW, de-centralised energy supply few Watt to 10 kW	Mobile/portable (100 mW to 100 W) applications, de-centralised energy supply	Combined heat and power plants (50-500 kW) Power plants (1-100 MW)	Combined heat and power plants (50-500 kW) Power plants (1-100 MW)	Combined heat and power plants (50-500 kW) Power plants (1-100 MW)



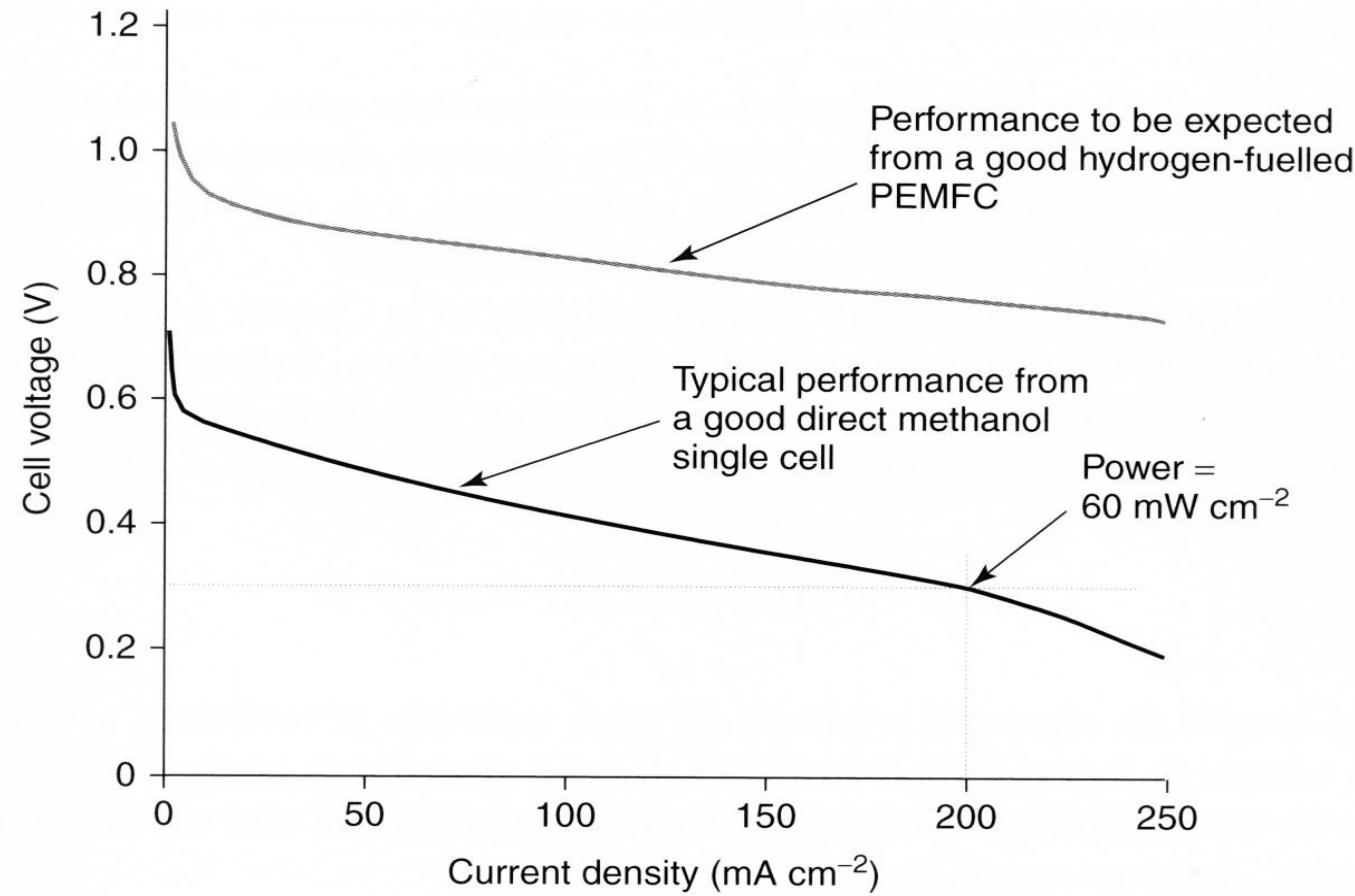
Typical current-voltage-curve of a PEM-FC



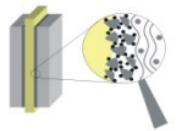
From: "Fuel Cell Systems Explained", J. Larminie, A. Dicks, Wiley 2003



Comparison: PEM-FC using MeOH or hydrogen as fuel

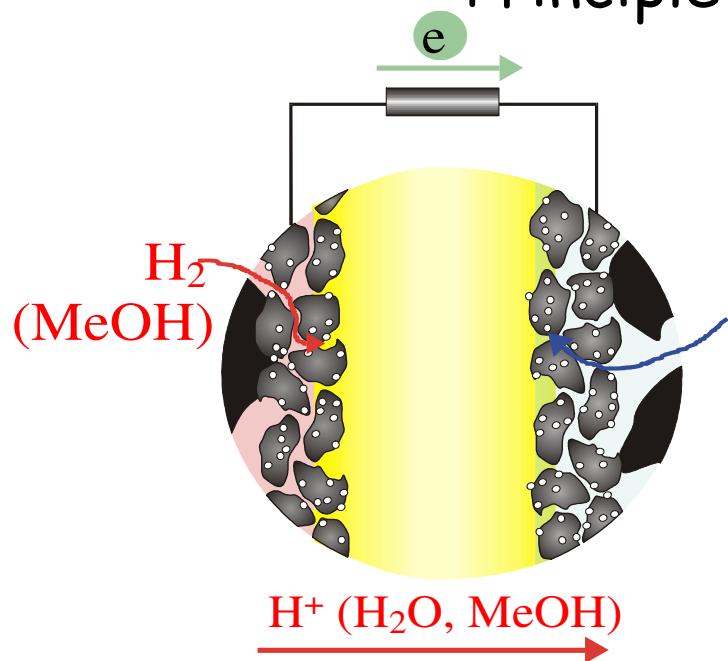


Aus: "Fuel Cell Systems Explained", J. Larminie, A. Dicks, Wiley 2003



Principle and reactions of the PEM-FC

PEM-FC = proton-exchange membrane fuel cell



O₂ Hydrogen fuel cell:

Anode

Cathode

Overall



0 V vs. NHE

1.23 V vs. NHE

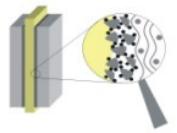
$$E_0 = 1.23 \text{ V}$$

$$\Delta G^R = -nFE_0$$

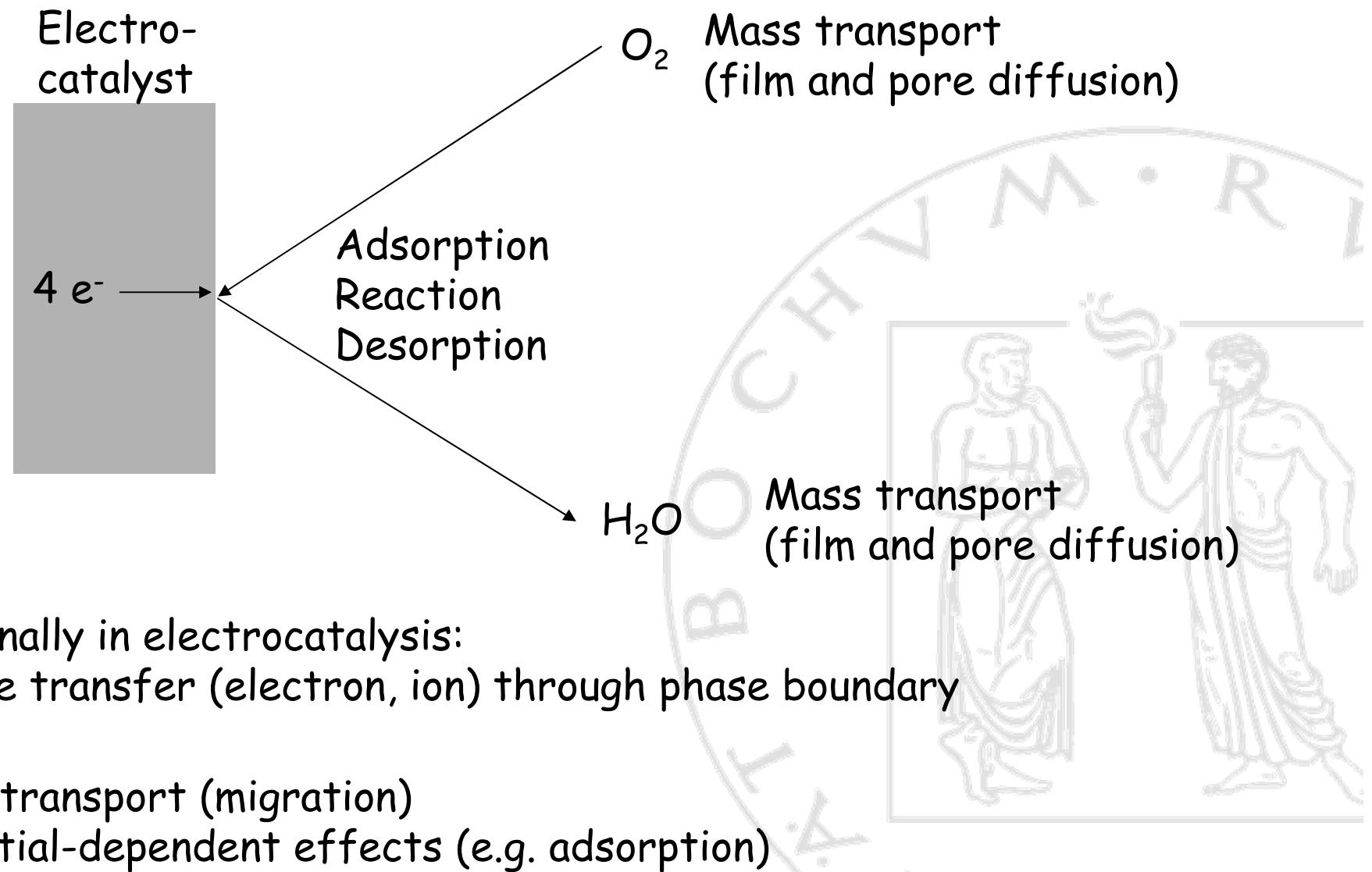
Efficiency losses due to

- mass transport problems in the porous electrode
- high overpotential of orr (oxygen reduction reaction)
- (ohmic losses)

Demand for efficient (and cheap) electrocatalysts

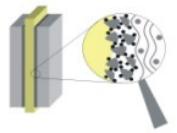


Comparison heterogeneous catalysis/electrocatalysis



Additionally in electrocatalysis:

- Charge transfer (electron, ion) through phase boundary
- Mass transport (migration)
- Potential-dependent effects (e.g. adsorption)



Rate of electrocatalytic reactions

Electrode potential

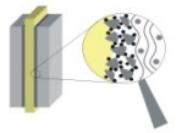
Concentration of reactants at active site

- Three-phase-boundary
- Pressure
- Mass transport/water management
- Pore structure/-distribution

Concentration and structure of active sites

- Nature of metal/second metal
- Particle size/-distribution
- Particle shape
- Metal-support interactions
- Alloys: Segregation, leaching, exact position of atoms in active site

Ligand effect
Ensemble effect
Structure sensitivity



Electrode kinetics: Butler-Volmer equation (see also talk of Prof. D. Kolb)

$$i = i_0 \left[\exp\left(\frac{\alpha_A nF}{RT} \eta\right) - \exp\left(-\frac{\alpha_C nF}{RT} \eta\right) \right]$$

where i_0 = exchange current density

η = overpotential ($= E - E_{\text{eq}}$)

n = number of electrons

α_A = anodic transfer coefficient

α_C = cathodic transfer coefficient

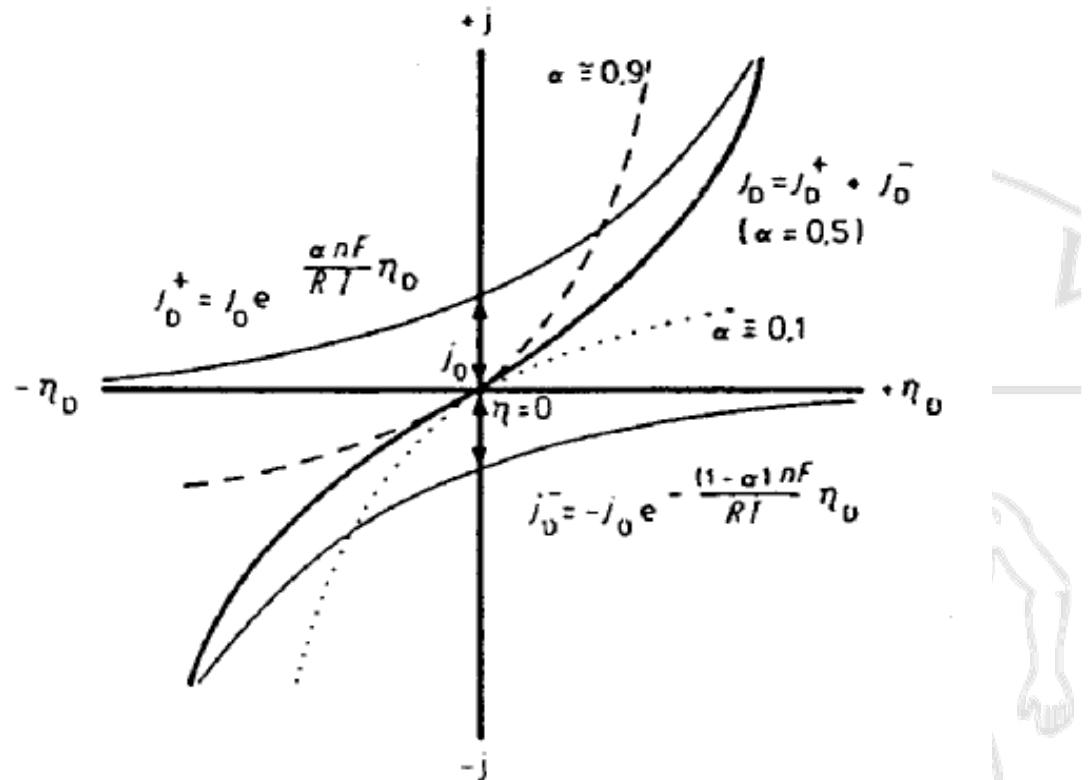
$i_C \gg i_A$: Tafel equation

$$i = i_0^* \exp[-(\alpha_C nF/RT) \eta]$$

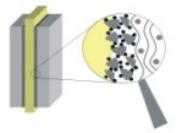
i = current

j = current density

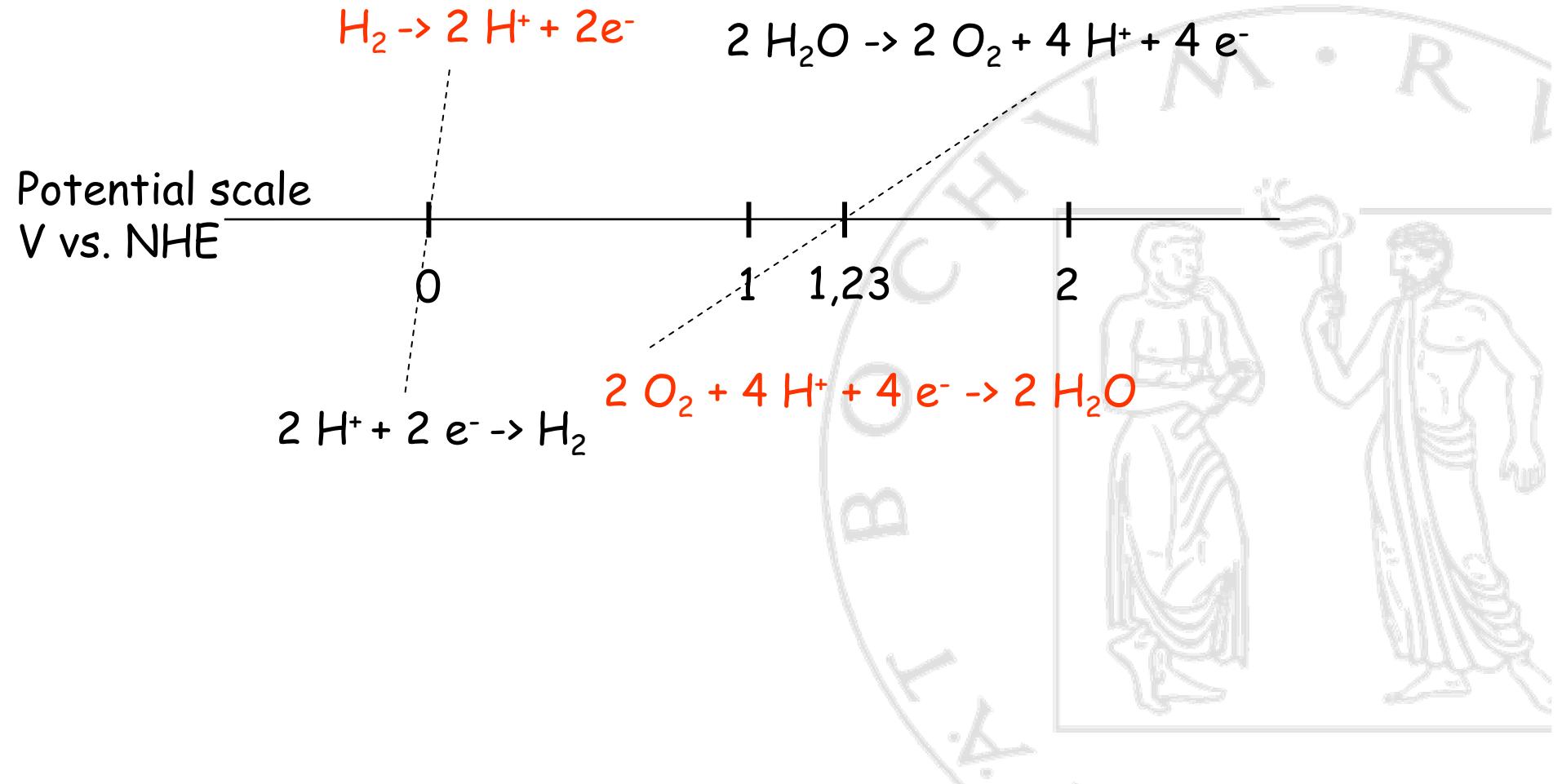
$$\alpha_C = 1 - \alpha_A$$

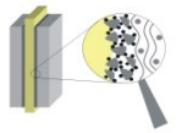


Elektrochemie Carl H. Hamann, Wolf Vielstich,
ISBN 3-527-27894-x



Overpotentials and cell voltages (schematic!!!!)



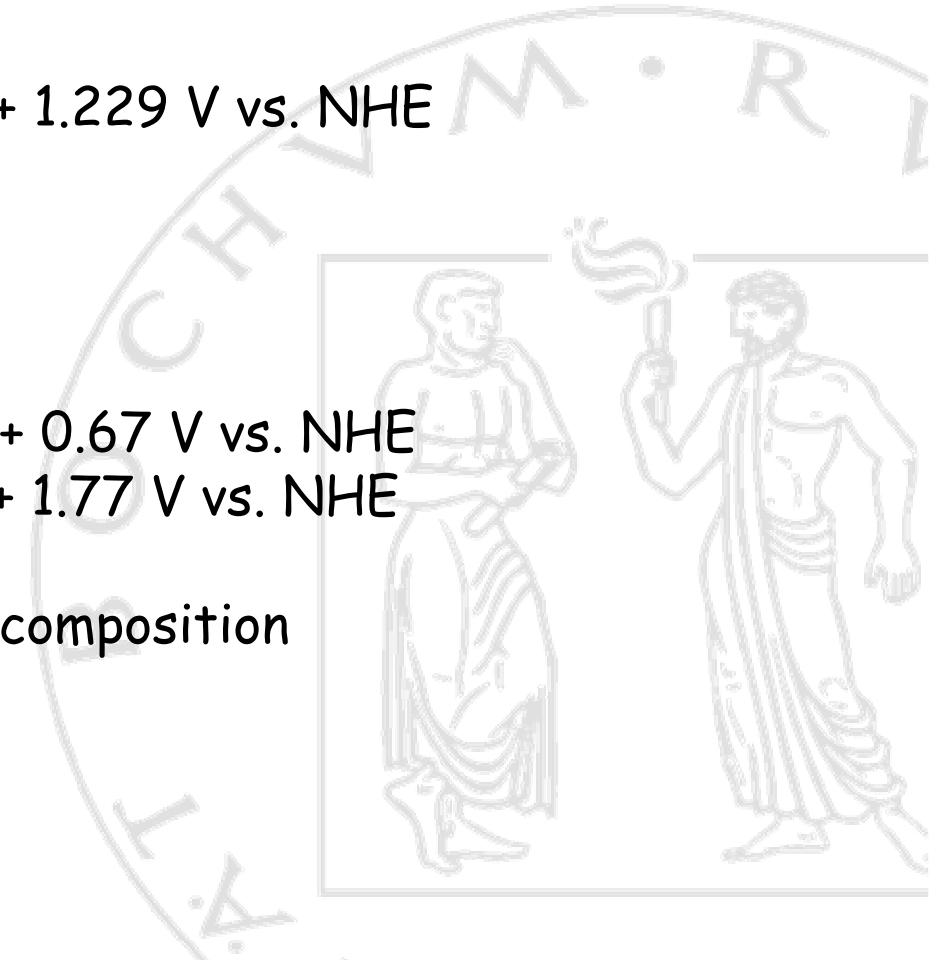
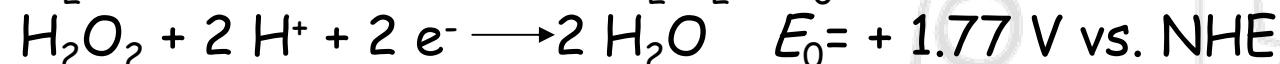
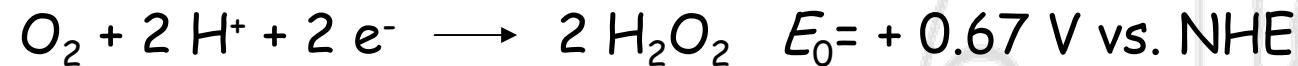


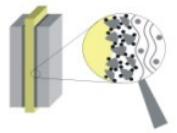
Example 1: Electrocatalytic oxygen reduction

4-electron-reduction

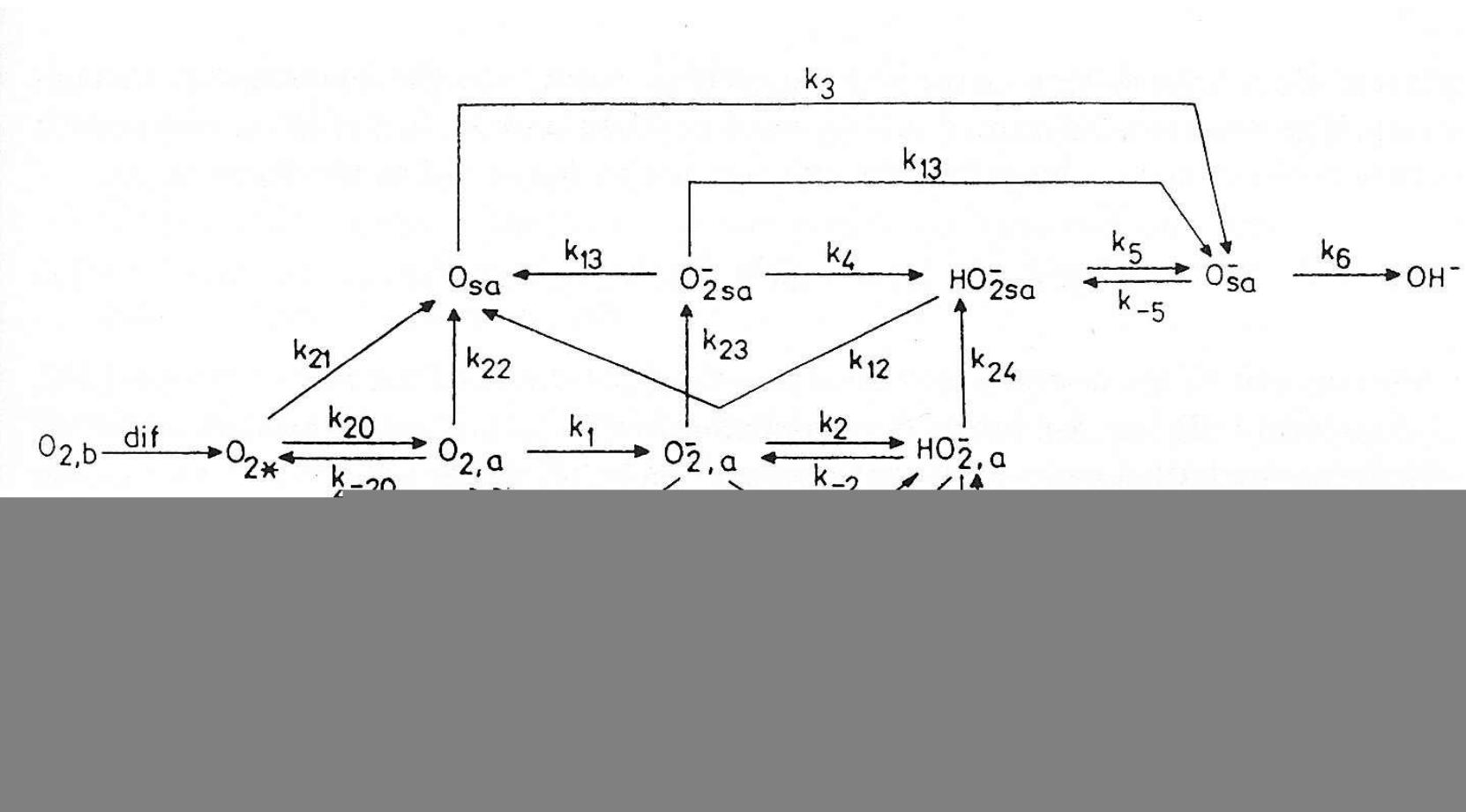


(2x)2-electron-reduction

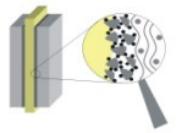




General scheme of electrocatalytic oxygen reduction

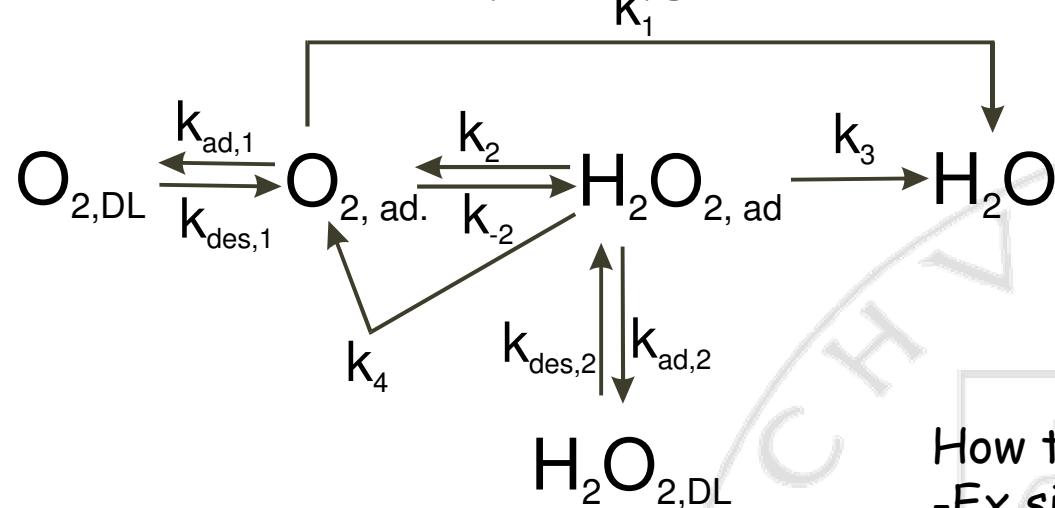


From: "Electrocatalysis", J. Lipkowski, P.N. Ross, Eds.; Wiley VCH, New York 1998.

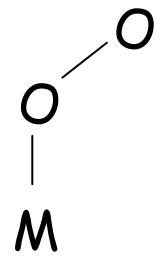


Electrocatalytic oxygen reduction

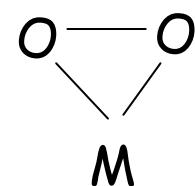
- Simplified scheme of electrocatalytic oxygen reduction:



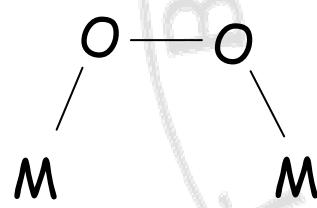
- 2-electron- or 4-electron-reduction?
- Adsorbate geometries



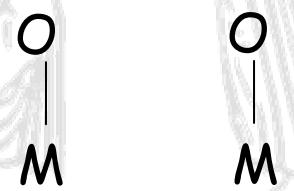
Pauling



Griffith

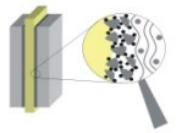


bridged



dissociative

How to investigate *in situ*?
- Ex situ: e.g. EELS, LEED, NEXAFS, XPS



Catalysts for oxygen reduction in PEM fuel cells

State of the art oxygen reduction catalyst:

Platinum

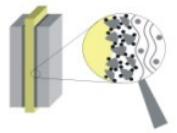
- Direct four-electron reduction
- Exact mechanism still not clarified
- Still large overpotential

Platinum alloys (Co, Fe, Ni, Cr,...)

Alternatives:

- Iron (and cobalt) based catalysts
- Catalysts based on ruthenium
- Surface modified ruthenium catalysts





Pt-alloy catalysts for oxygen reduction: structural and electronic characterisation

TABLE 5.1 Comparison of Activation Energy for Oxygen Reduction with Results from the in-Situ EXAFS and XANES Analysis on Pt and Pt-Alloy Electrocatalysts at 0.54 and 0.84 V vs RHE^a

Electrocatalyst	ΔH_{act} (kJ/mol)	0.54 V vs RHE						0.84 V vs RHE					
		Pt–Pt		Pt–M		M–M (Å)	M–Pt (Å)	Pt–Pt		Pt–M		M–M (Å)	M–Pt (Å)
		$(h_J)_{t.s}$	(Å)	N	(Å)	N	$(h_J)_{t.s}$	(Å)	N	(Å)	N		
Pt/C ^b	62.17	0.329	2.77	8.7				0.370	2.77	6.8			
Pt/Cr (ETEK)	28.72	0.360	2.70	7.2	2.67	3.1		0.361	2.71	7.0	2.67	3.2	
Pt/Cr (JMRC)	27.63	0.360	2.71	8.5	2.69	2.8		0.358	2.71	8.8	2.70	2.9	
PtCo (ETEK)	23.74	0.368	2.71	6.5	2.64	2.3	2.65	2.64	0.365	2.69	5.9	2.64	2.9
PtCo (JMRC)	35.44	0.401	2.68	6.9	2.63	2.5	2.62	2.51	0.300	2.68	7.6	2.62	2.3
	375	2.71	7.8	2.66	2.4	2.55	2.64	0.372	2.71	7.6	2.65	2.3	2.57
													2.66
													PtNi (ETEK)
													23.84
													0

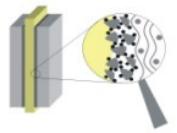
^a Activation energy determined at 0.54 V vs RHE; the Pt–Pt distance was 2.69 Å and 2.64 Å. Reproduced from Ref. 13 with permission.

^b $(h_J)_{t.s}$: d-orbital occupancy parameter.

"Electrocatalysis", J. Lipkowski, P.N. Ross, Eds., Wiley VCH, New York 1998.

electronic factors (electronic structure of surface atoms) and geometric factors (exact position of surface atoms)

here: geometric factors seem to be dominating



Crystallite size effects in oxygen reduction over Pt

Structure sensitive activity:

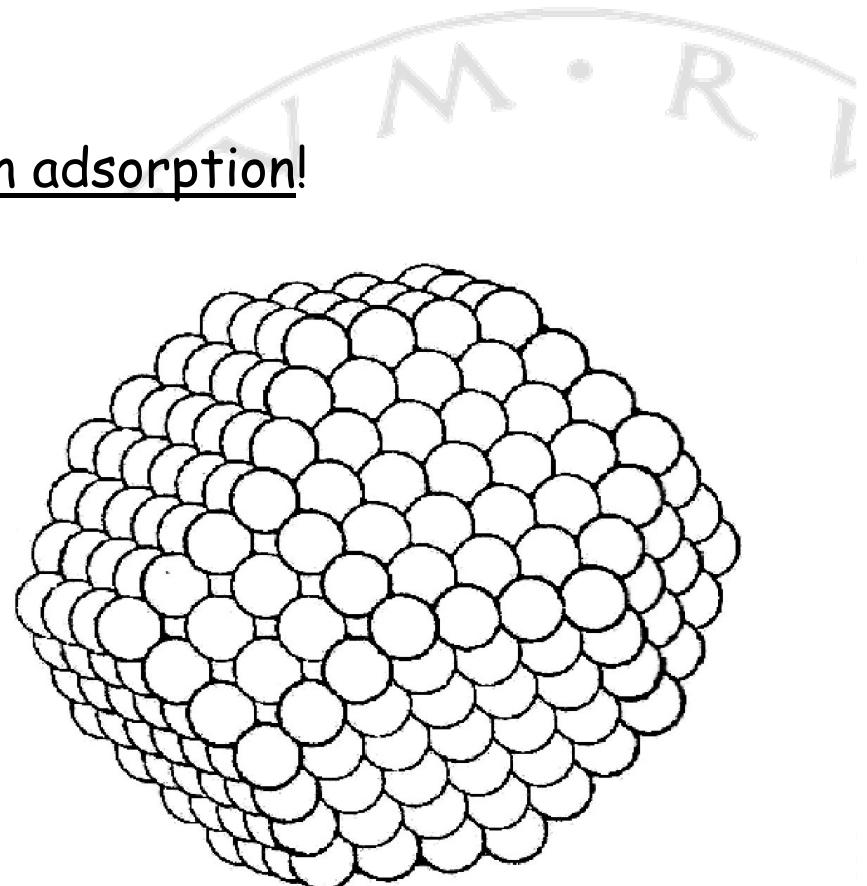
(111), (110) > 100 in aqueous HClO_4

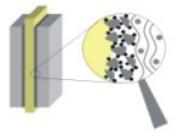
(111) << (100) < (110) in aqueous H_2SO_4

Explanation includes structure sensitive anion adsorption!

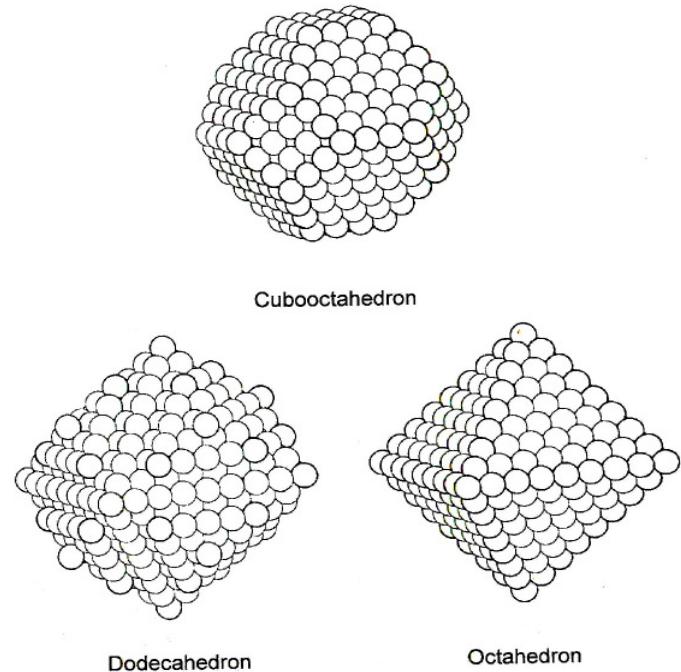
(N. Markovich, P. Ross, 1997)

Particle < 6 nm: (111)-surface dominating,
< 1.8 nm: (111) is nearly the only surface

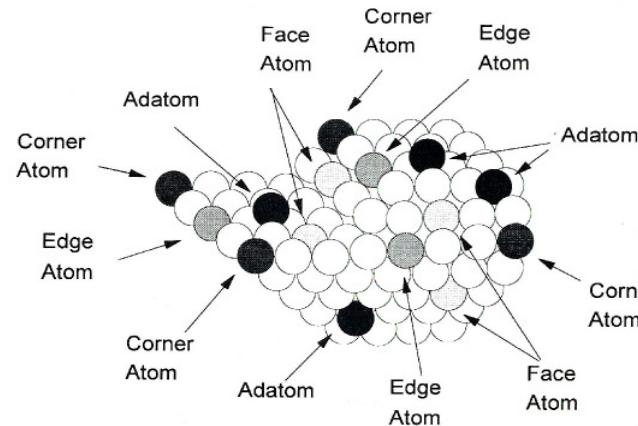
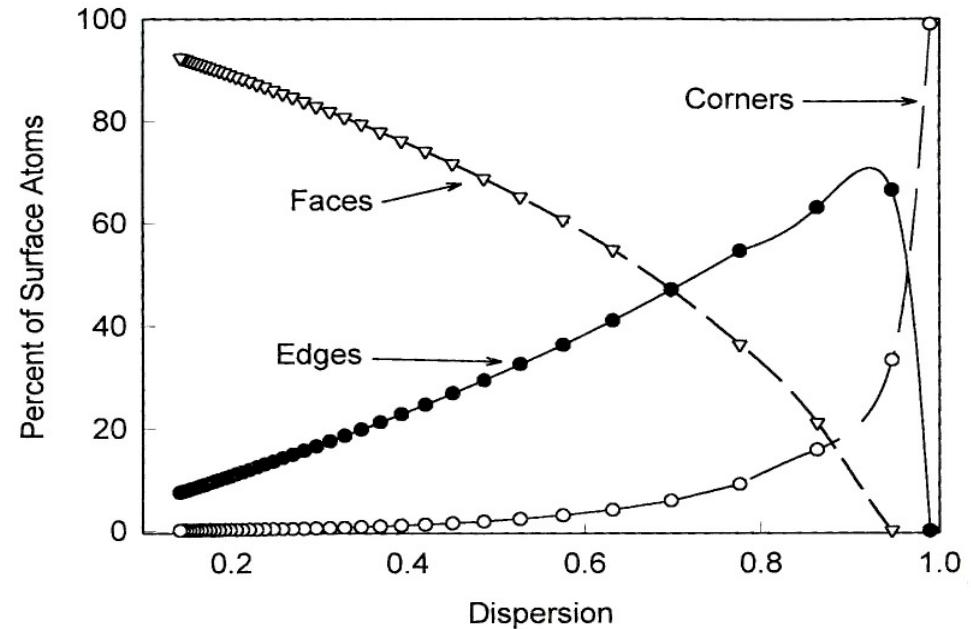




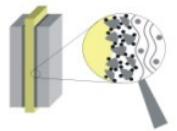
Structure sensitivity: particle size



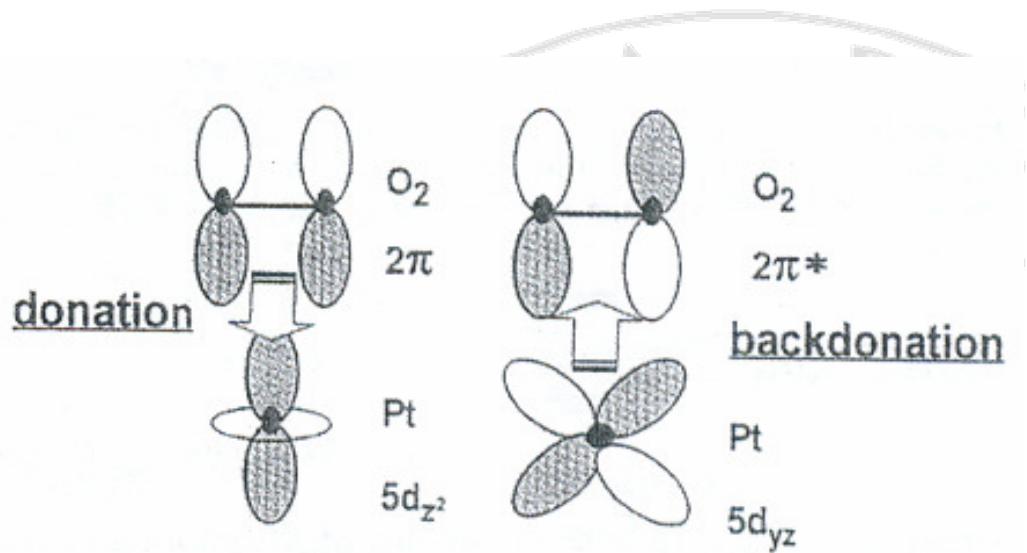
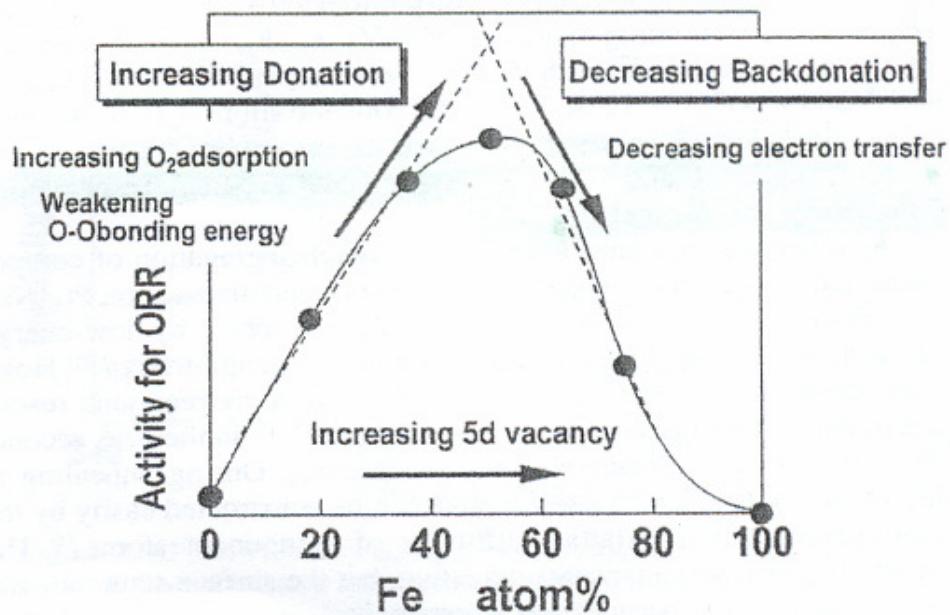
Idealized crystal shapes



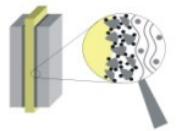
different types of
surface atoms



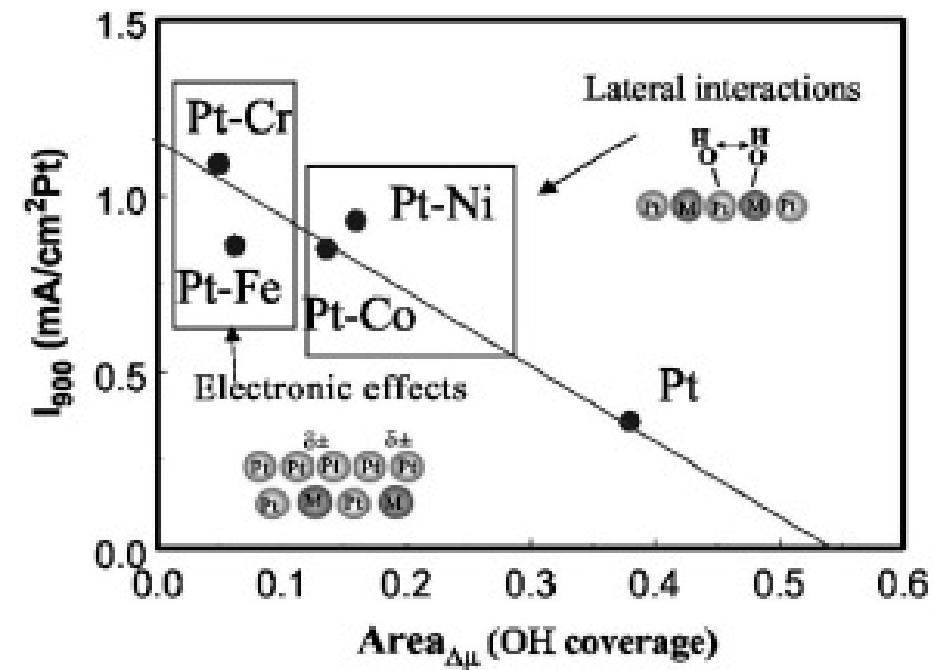
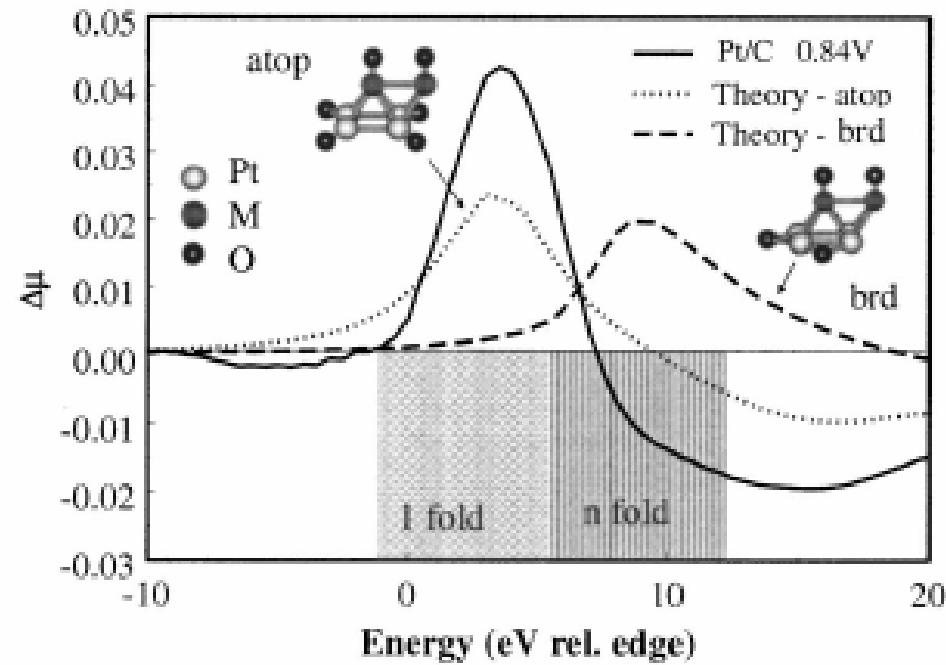
Another view: simplified model of donation-backdonation



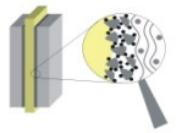
T. Toda, H. Igarashi, H. Uchida, and M. Watanabe, *J. Electrochem. Soc.*, 146, 3750 - 3756, 1999



Inhibition of oxygen reduction by adsorbed species

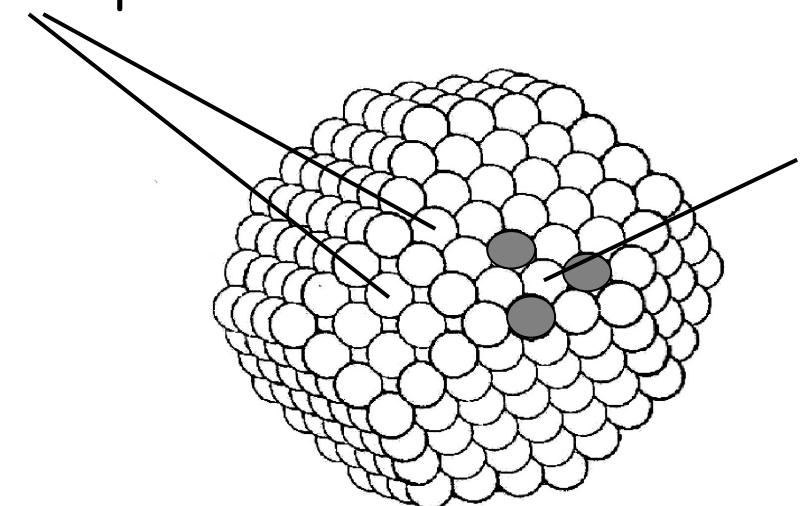


From: Teliska et al. J. Electrochem. Soc. 152 (2005) A2159-A2169.



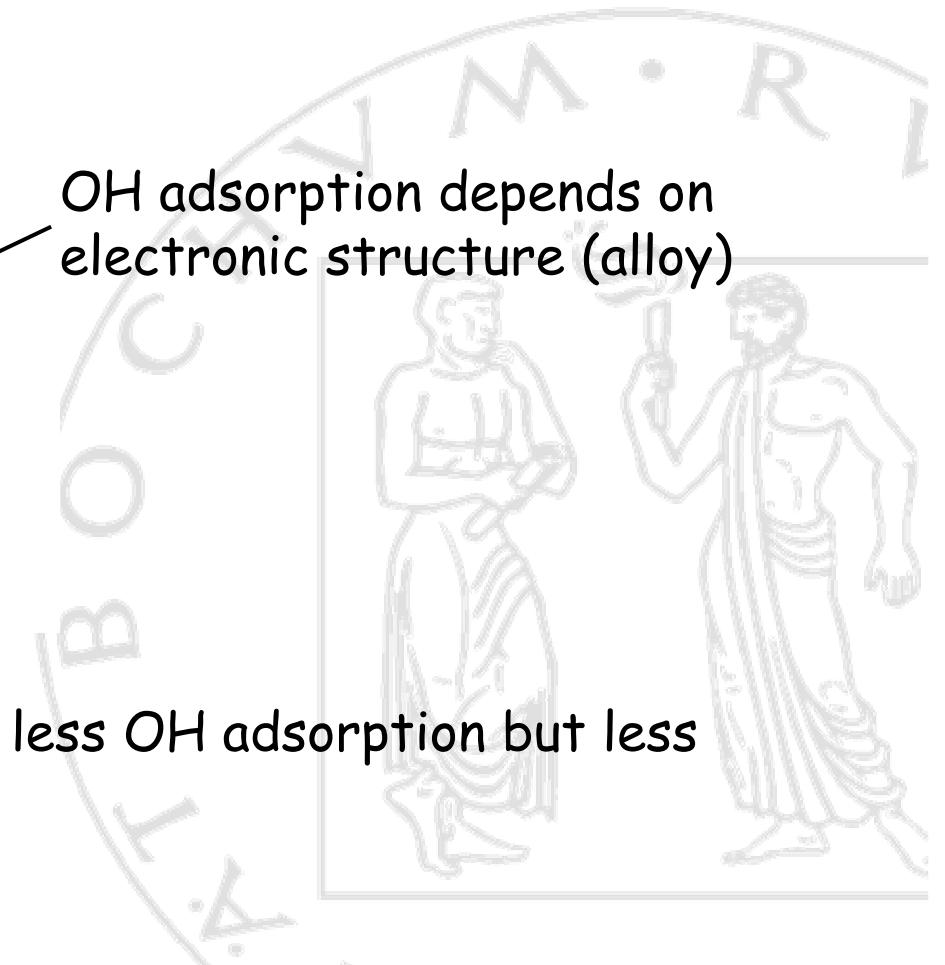
Influence of OH-adsorption

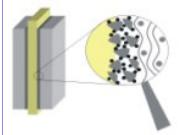
geometrical structure sensitivity
due to OH-adsorption



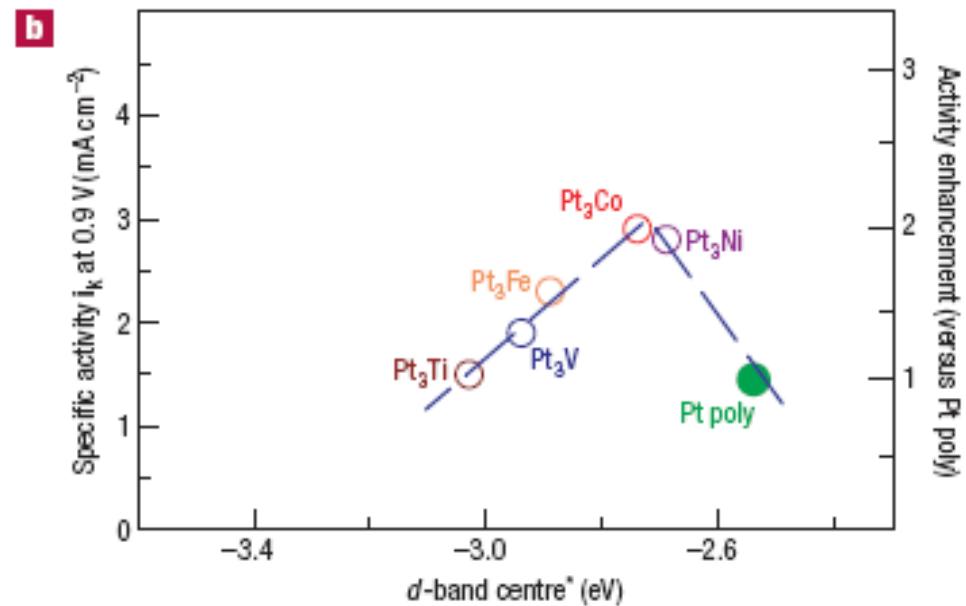
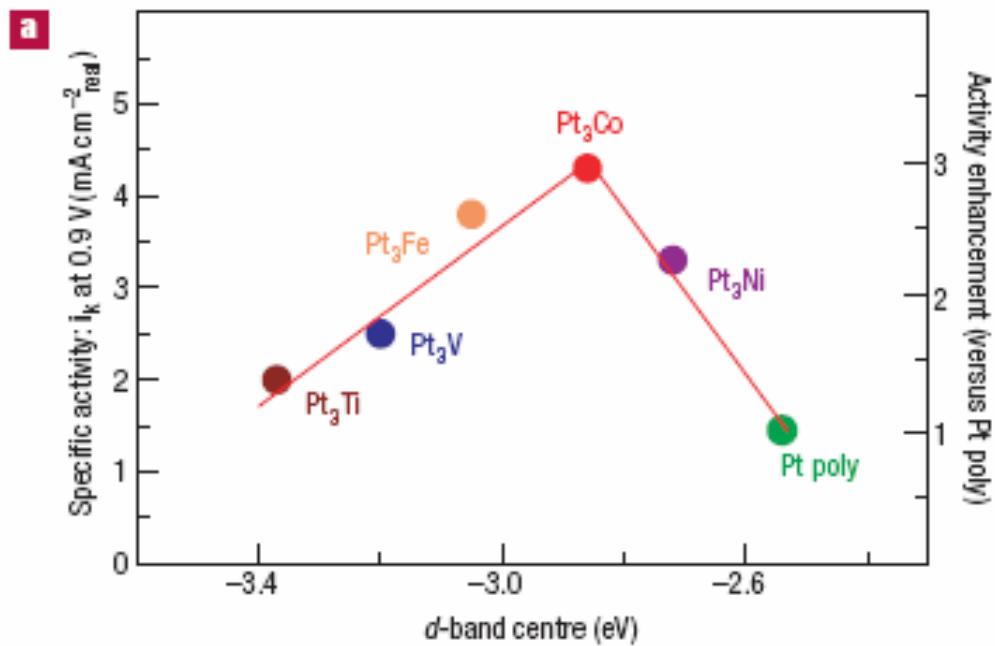
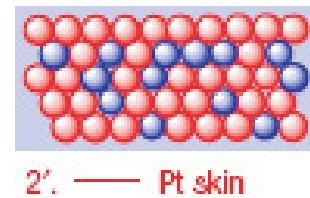
OH adsorption depends on
electronic structure (alloy)

optimum particle size (larger particles: less OH adsorption but less
surface area)

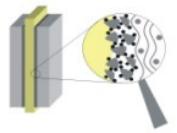




Volcano behaviour: Oxygen activation/inhibition



Stamenkovic et al., Nature Materials 6 (2007) 242



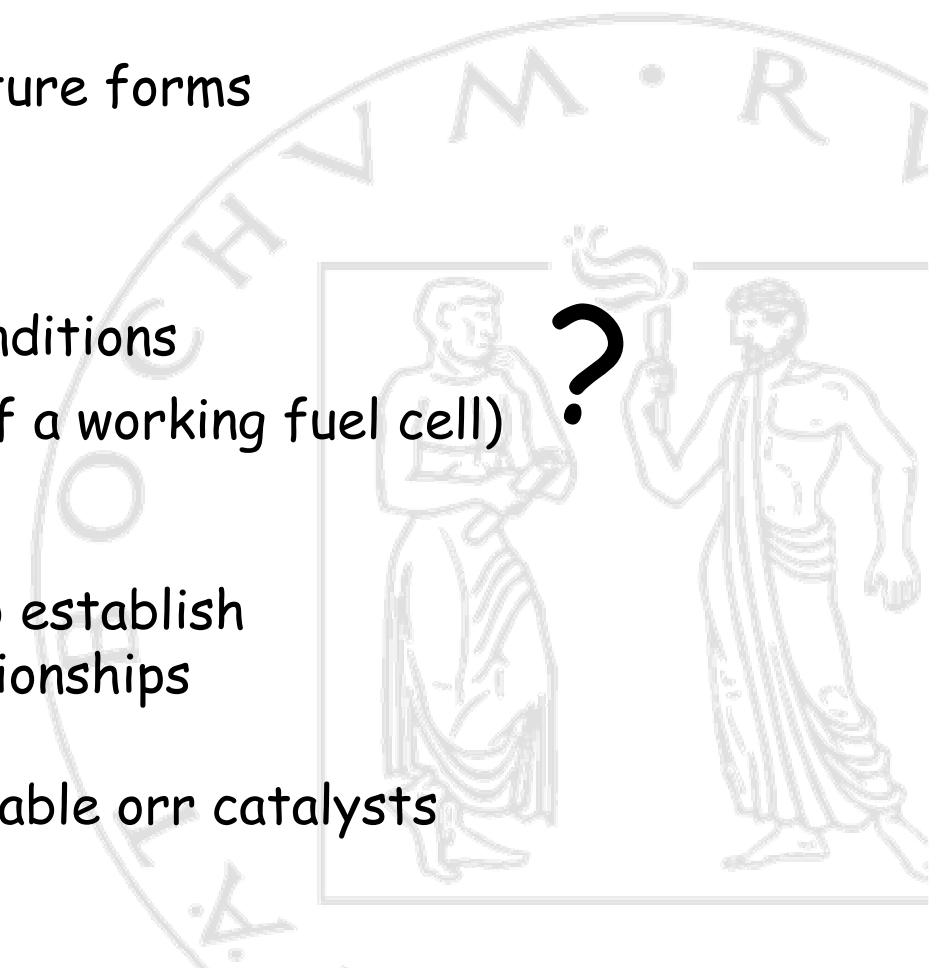
Stability of Pt(alloy) electrocatalysts

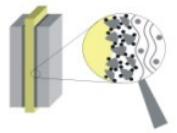
Pt-alloy:

- leaching of less noble metal
- poisoning of membrane
- kind of core-shell structure forms
- sintering

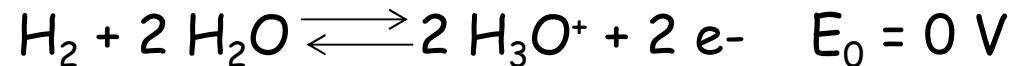
What is really present under reaction conditions
(i.e., in a membrane electrode assembly of a working fuel cell)

- Real in situ-measurements to establish true structure-activity relationships
- Development of long-term stable orr catalysts

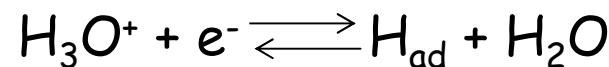




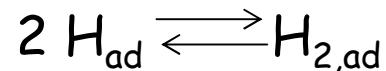
Hydrogen electrode reactions



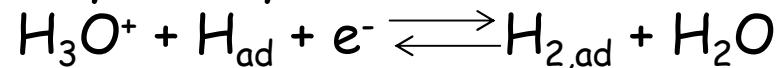
Volmer-reaction:



Tafel-reaction:

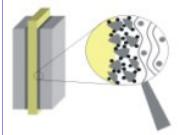


Heyrowsky-reaction



Volmer-Tafel- und Volmer-Heyrowsky-mechanism



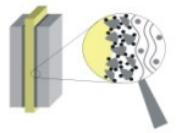


CO as anode poison

Table 5. Cell voltage (mV) at a current density of 0.5 A cm^{-2} for PtRu/C electrocatalysts with various Pt:Ru atomic ratio in different operating conditions [67]

Electrocatalyst	70 °C, H ₂	70 °C, H ₂ + CO	90 °C, H ₂	90 °C, H ₂ + CO
20% Pt	636	105	672	205
20% PtRu 3:1	630	201	657	476
20% PtRu 7:3	610	136	650	436
20% PtRu 1:1	592	413	621	557
20% PtRu 1:3	350	89	626	529
40% PtRu 1:1	649	415	674	611

From: E. Antolini, J. Appl. Electrochem. 34 (2004) 563-576.



CO oxidation



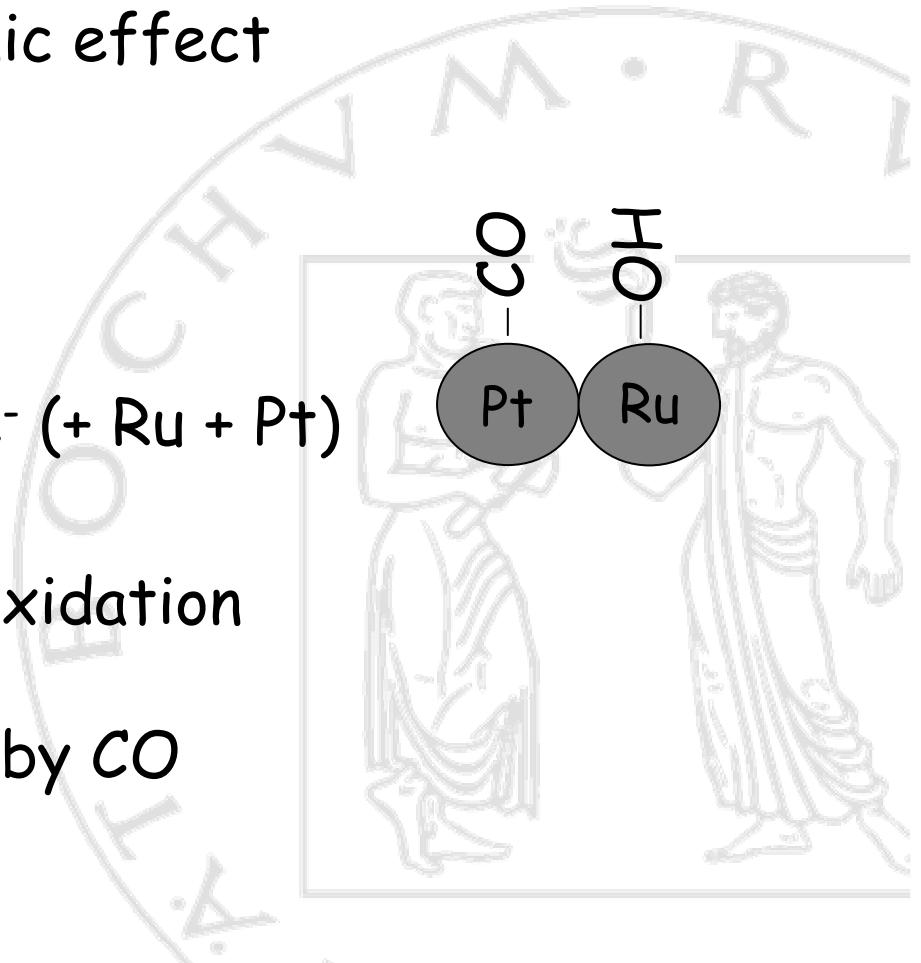
Bifunctional mechanism vs. electronic effect

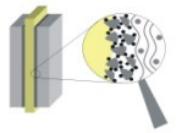
Bifunctional mechanism:



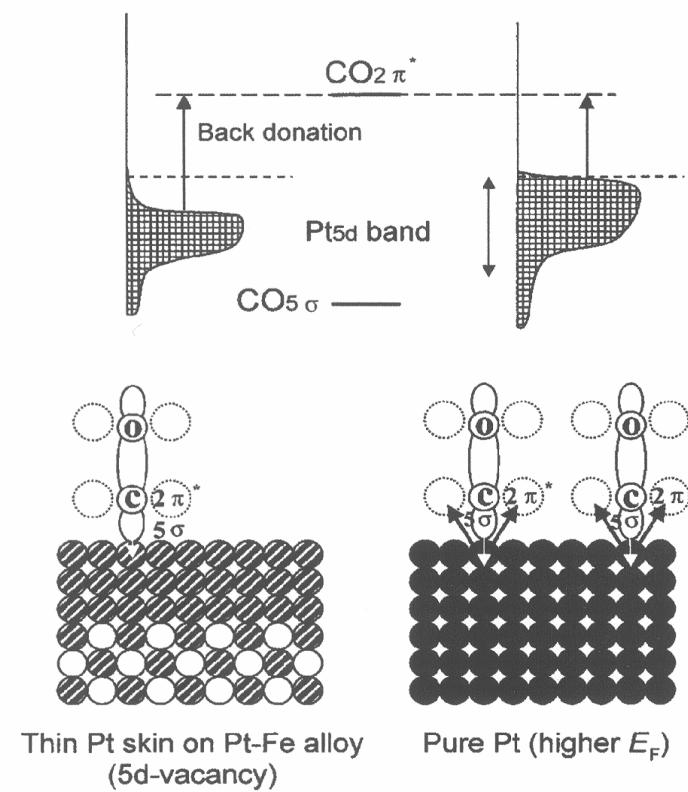
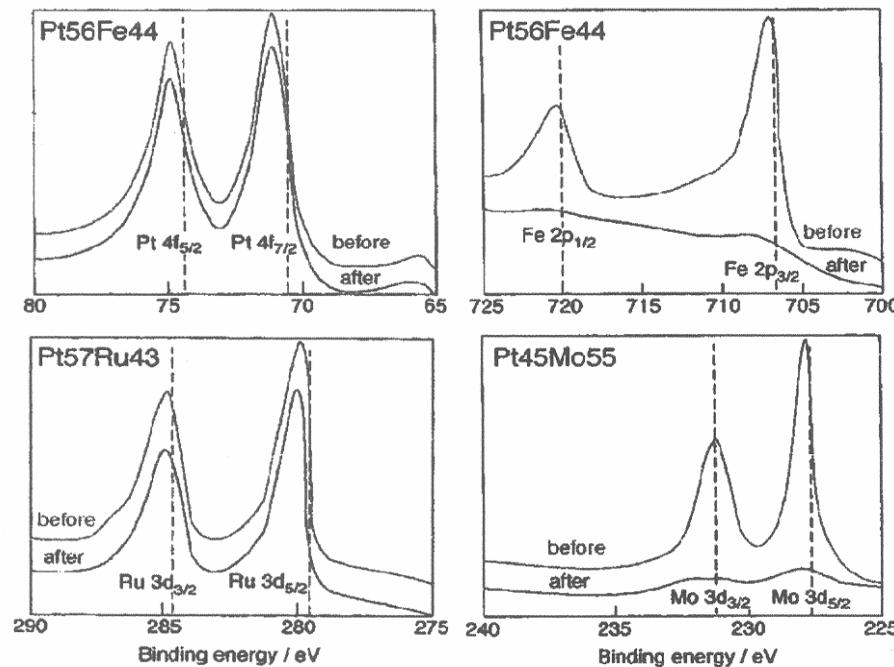
50:50-alloy PtRu highly active for oxidation of adsorbed CO

CO in solution: Blocking of Ru sites by CO
high activity with e.g. Pt_3Sn

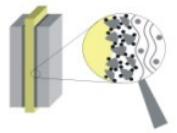




Electronic effects in CO-poisoning of fuel cell anodes

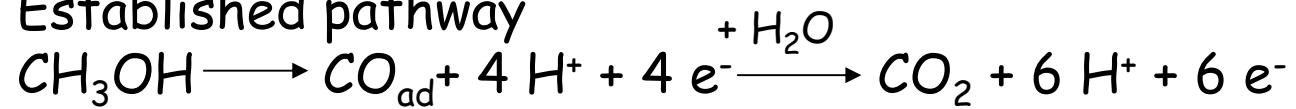


Igarashi et al., Phys. Chem. Chem. Phys. 3 (2001) 306-314

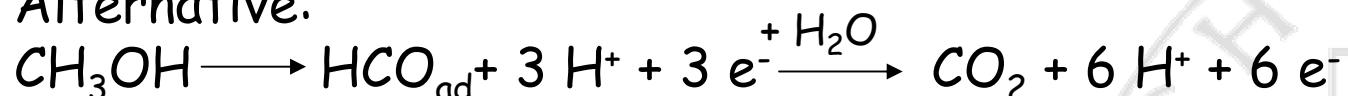


Methanol oxidation

Established pathway



Alternative:

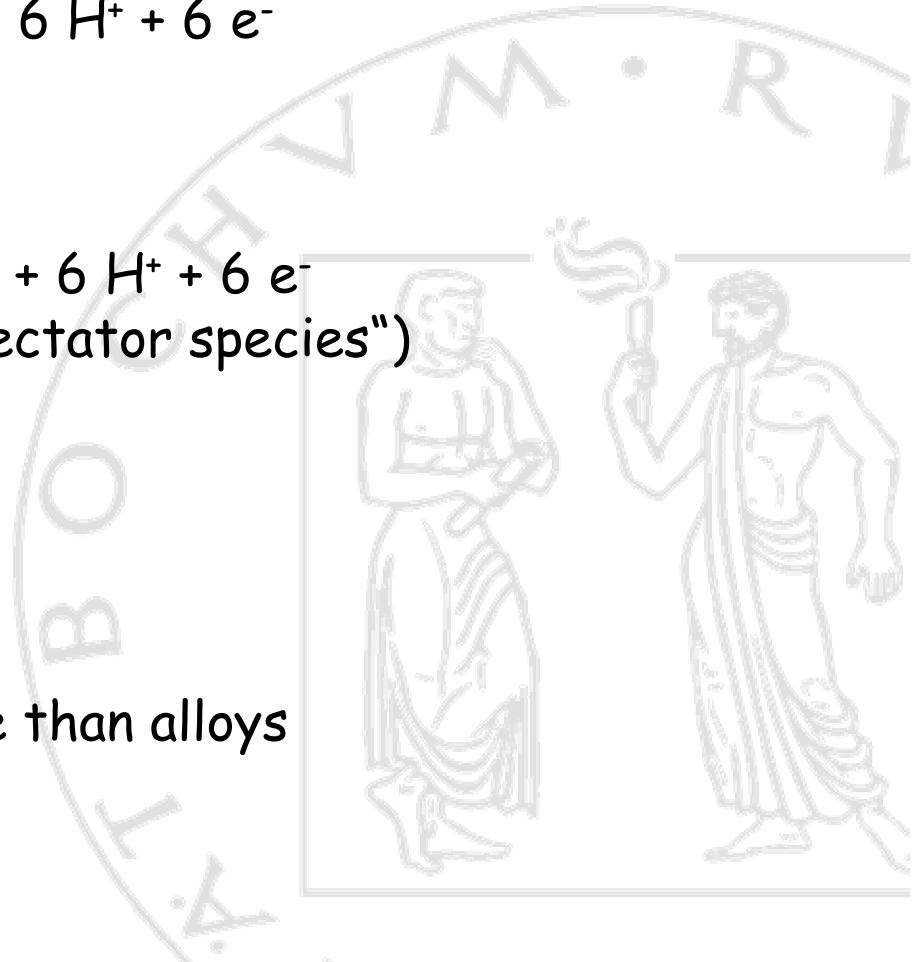


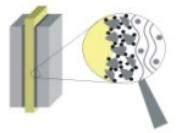
(with CO formation as side reaction („spectator species“))

Catalysts:

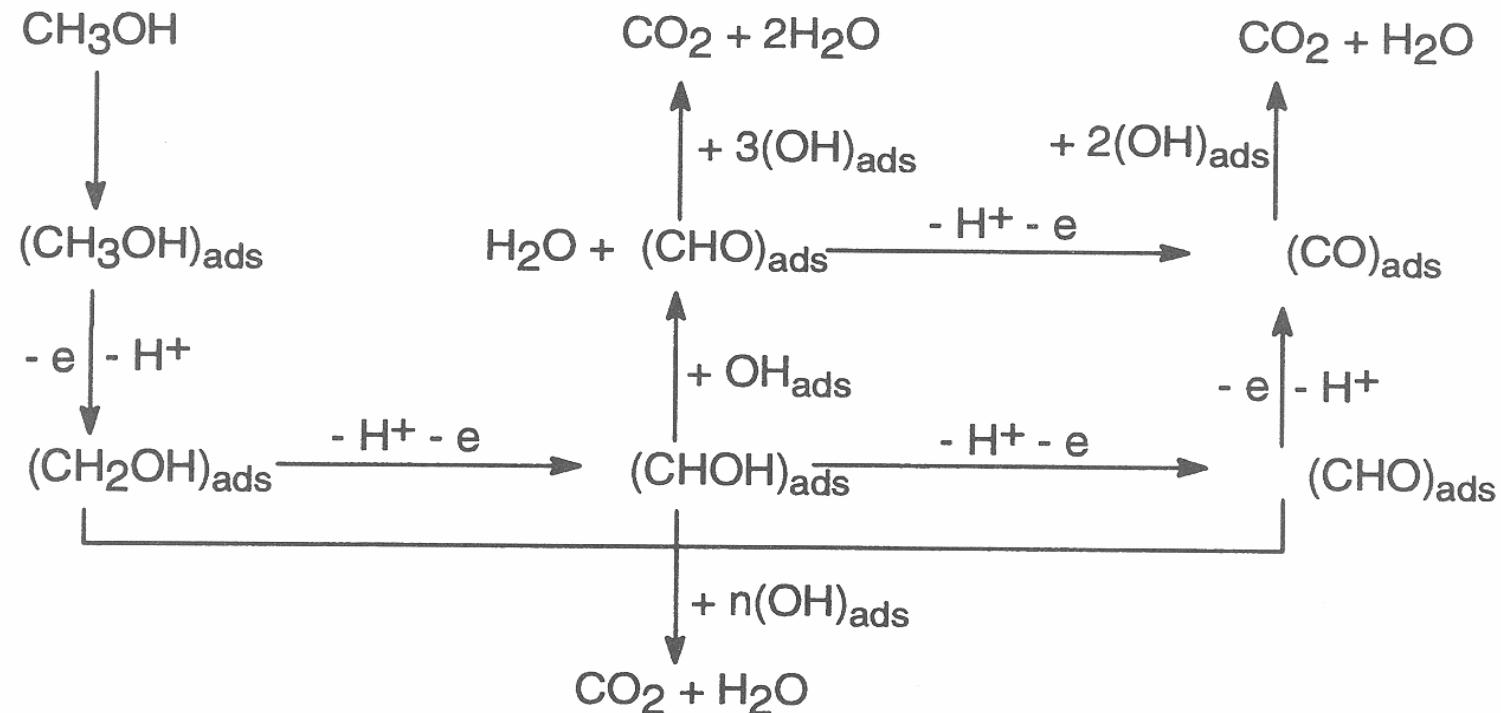
PtRu-Alloys

But: PtMeO_x is claimed to be more active than alloys
(Me: Ru, but also W, Mo,...)

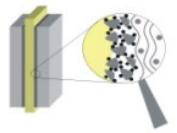




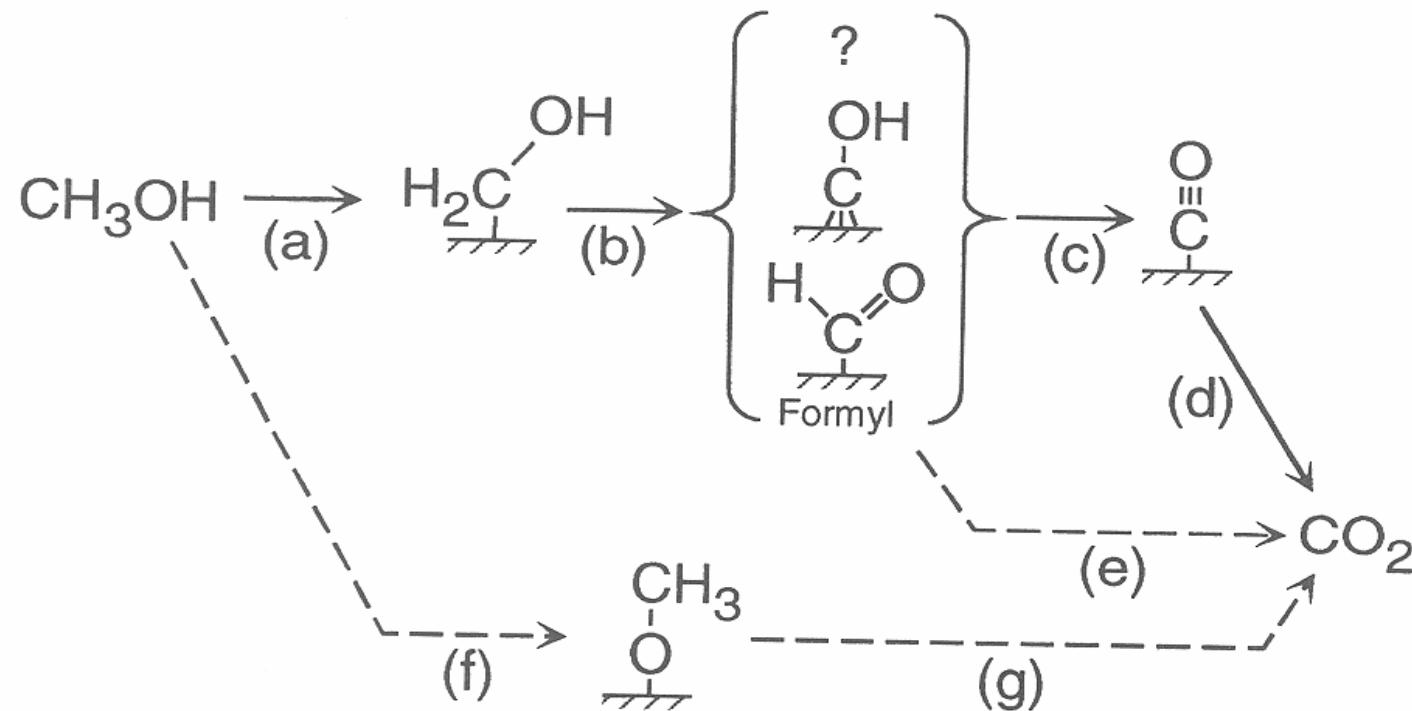
Reaction network of MeOH-Oxidation on Pt electrodes



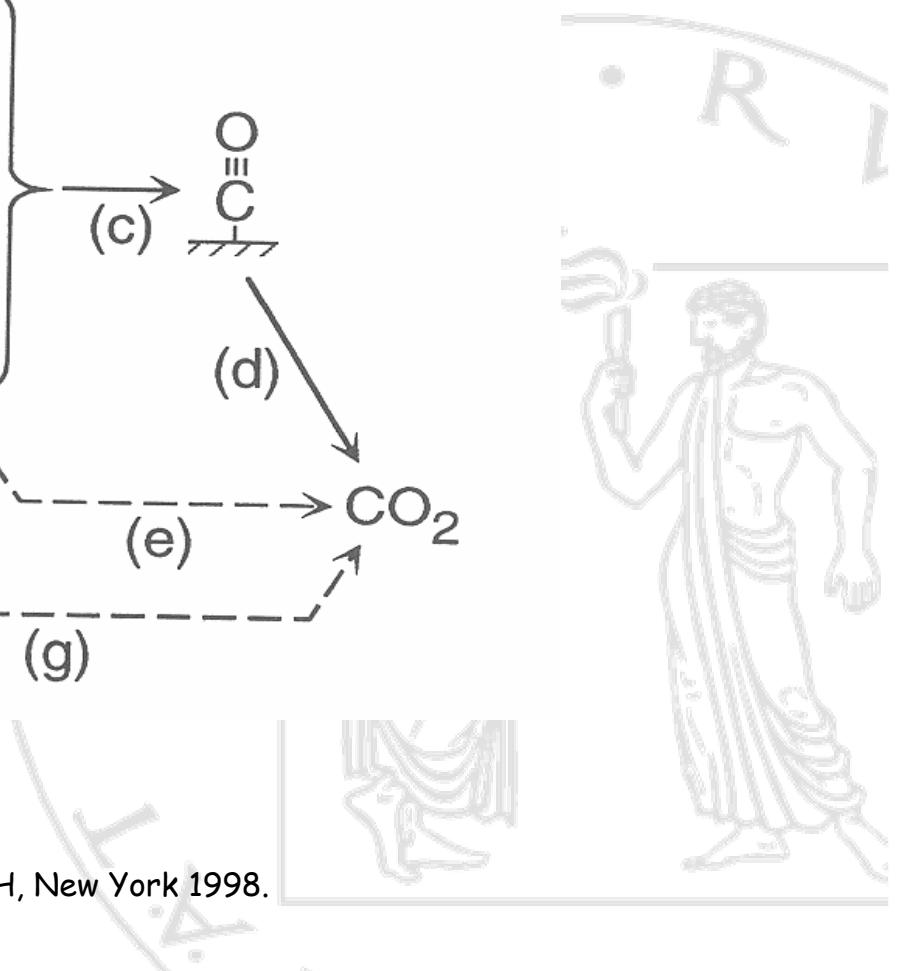
Aus: "Electrocatalysis", J. Lipkowski, P.N. Ross, Eds.; Wiley VCH, New York 1998.

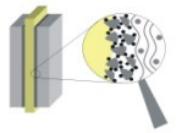


Surface species during methanol Oxidation



Aus: "Electrocatalysis", J. Lipkowski, P.N. Ross, Eds.; Wiley VCH, New York 1998.





Concentration and structure of active sites

- Nature of metal/second metal
- Particle size/-distribution
- Particle shape
- Metal-support interactions
- Alloys: Segregation, leaching, exact position of atoms in active site



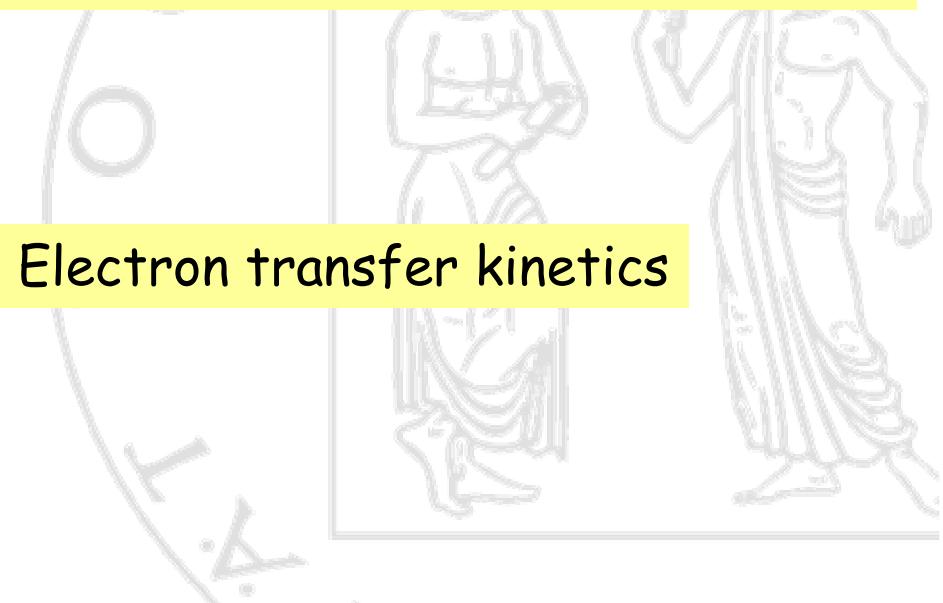
- strength of adsorption/stability of adsorbates (educts, intermediates, poisons, products, co-adsorbates)

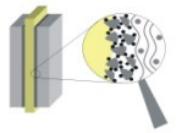
- adsorbate geometries: occupied surface sites, binding within adsorbates)

Electrode potential

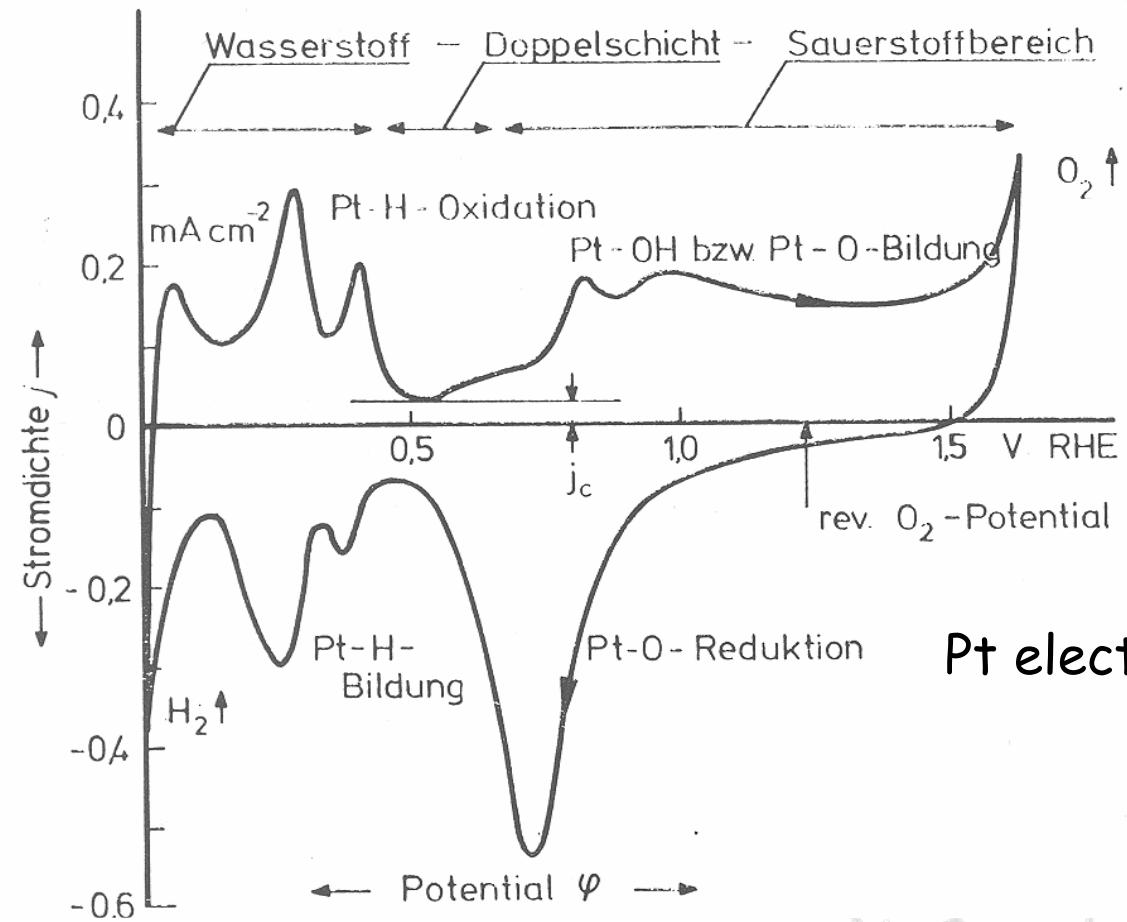


Electron transfer kinetics



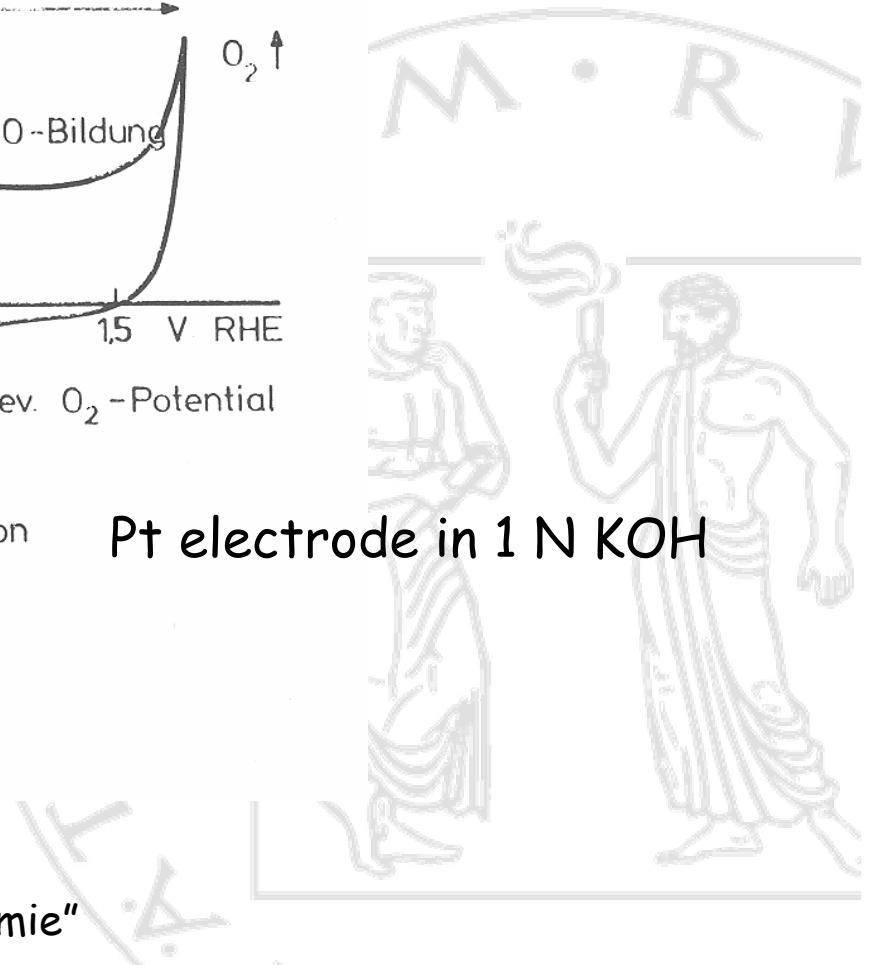


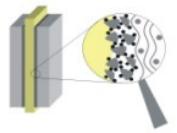
Cyclic voltammetry



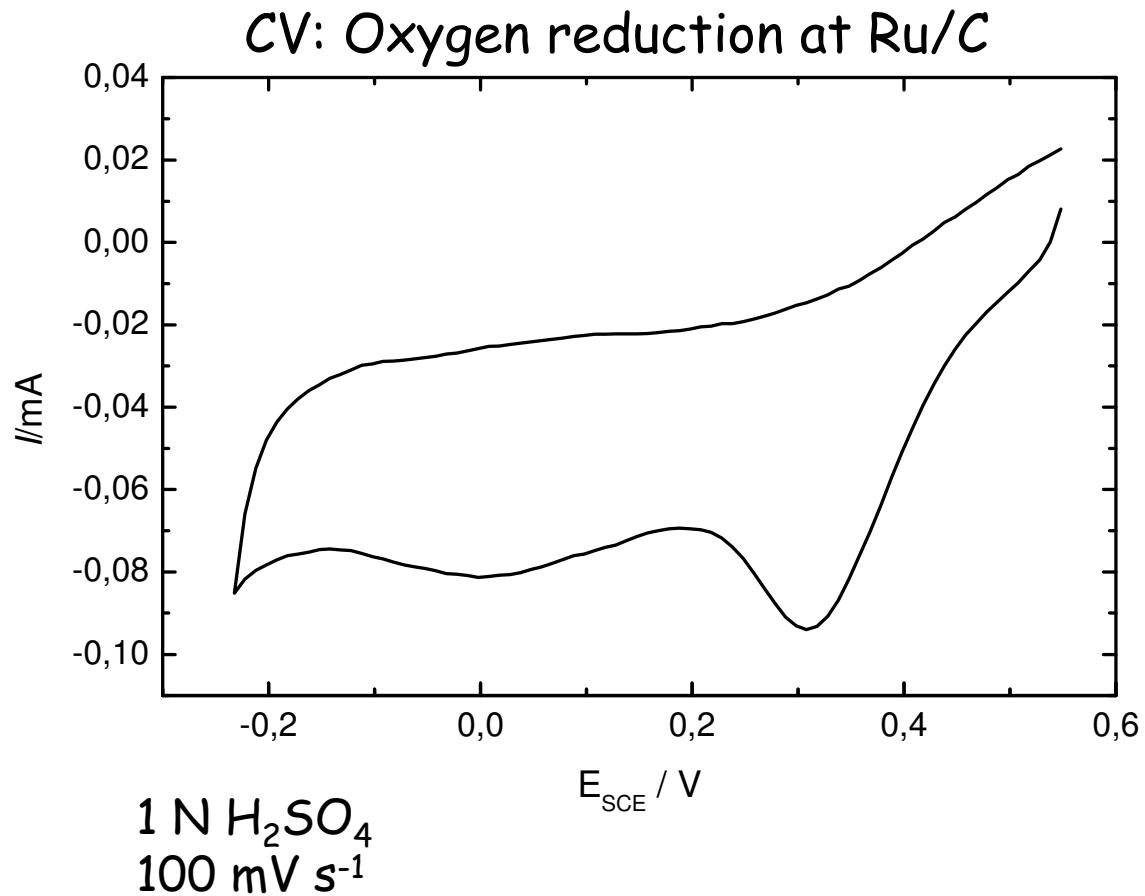
Pt electrode in 1 N KOH

From: C.H. Hamann, W. Vielstich: "Elektrochemie"

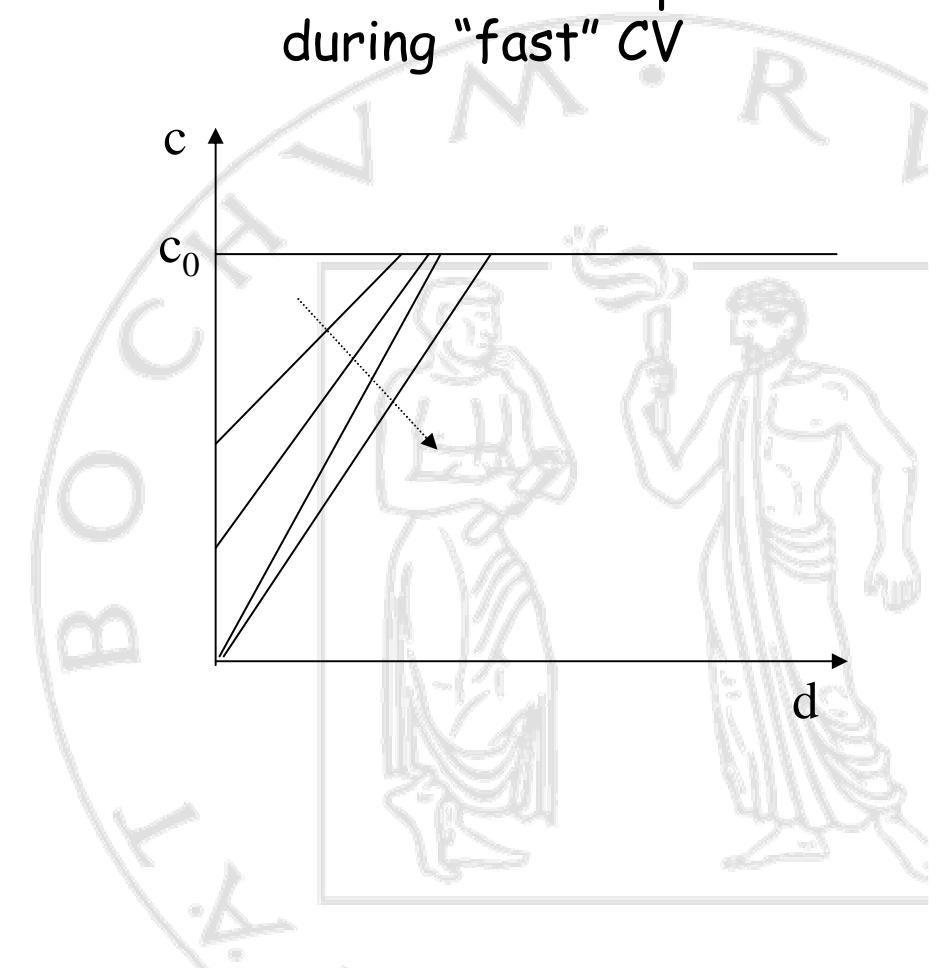


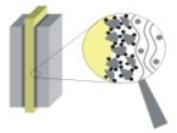


Cyclic voltammetry: influence of diffusion

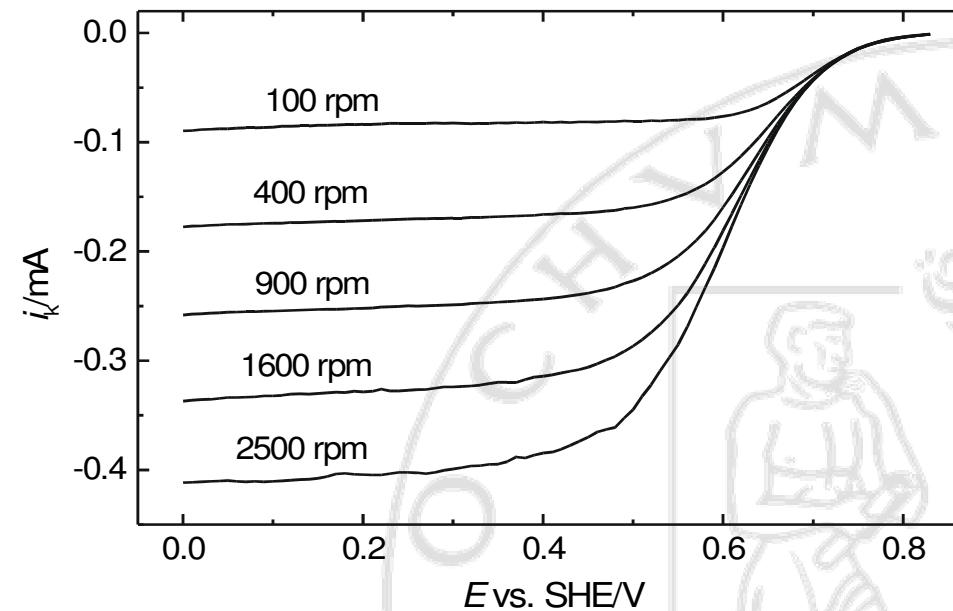
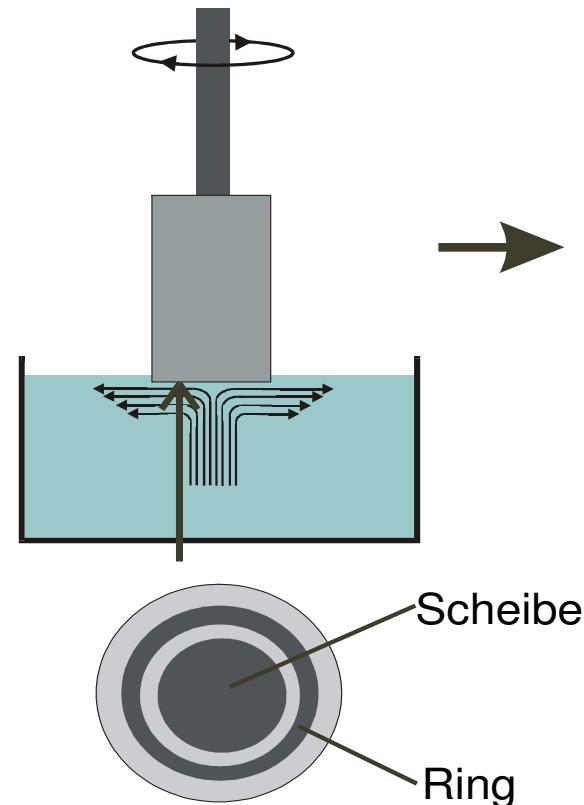


Schematic: Diffusion profiles during "fast" CV



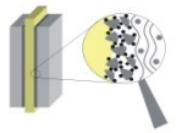


Principles of Rotating Ring-Disc Electrodes

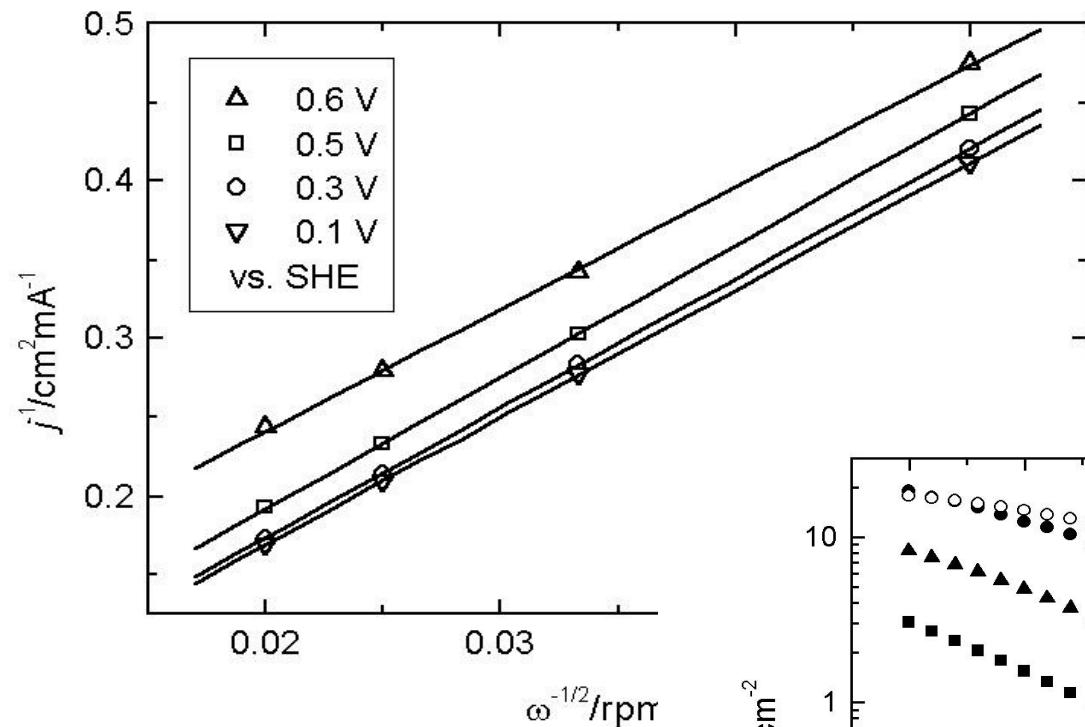


Koutecky-Levich-Analyse

$$1/i = 1/i_k + 1/i_d \quad \text{with } i_d = Bc_o \omega^{1/2}$$

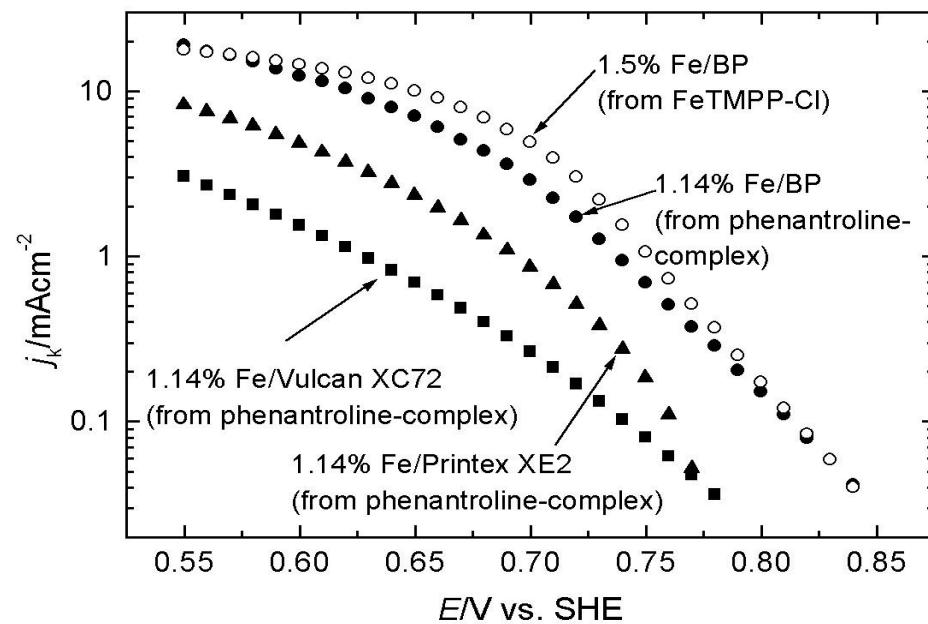


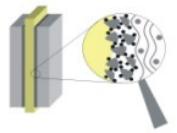
Koutecky-Levich-Plot



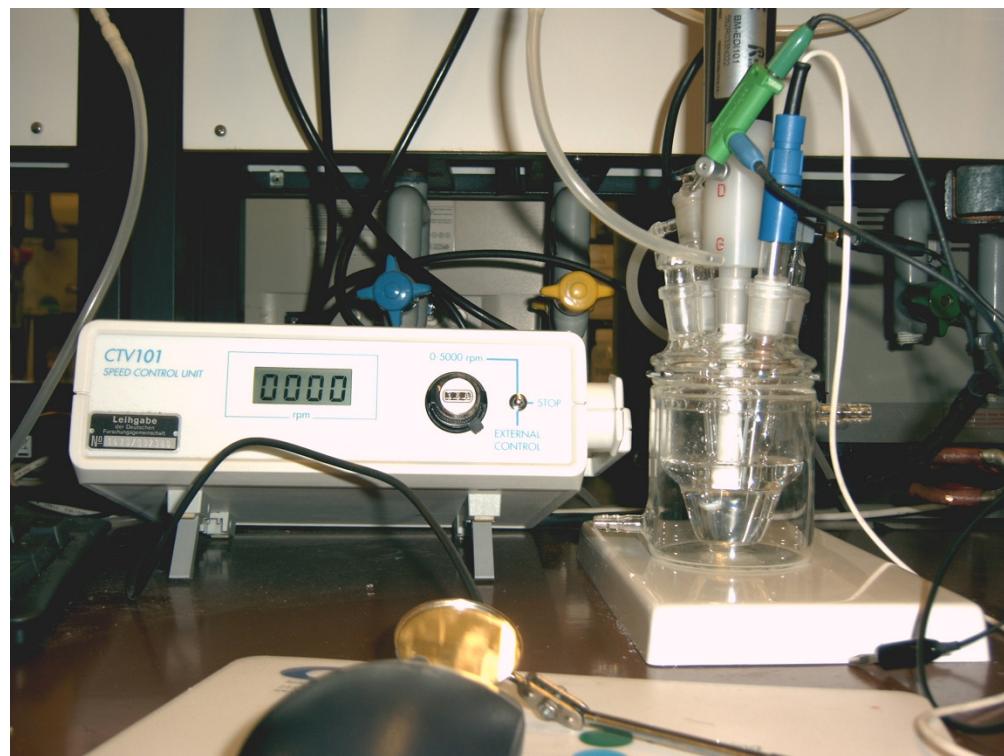
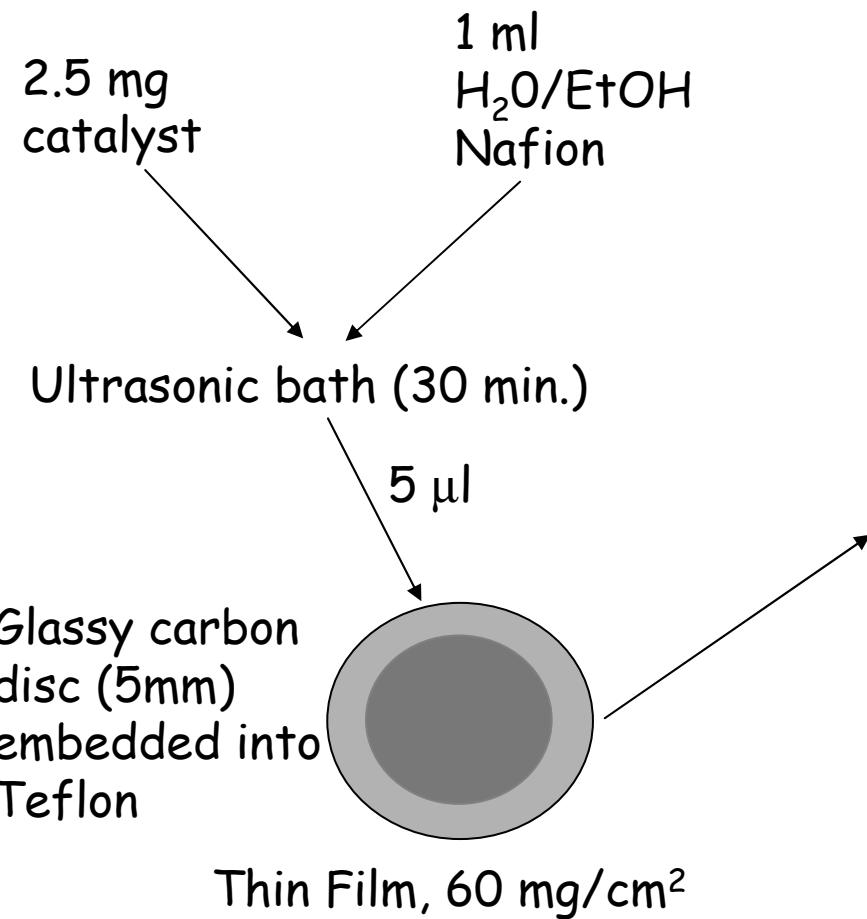
$$1/i = 1/i_k + 1/(Bc_0\omega^{1/2})$$

Tafel-Plot



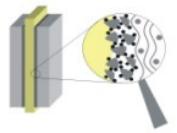


Electrode preparation for powder catalysts

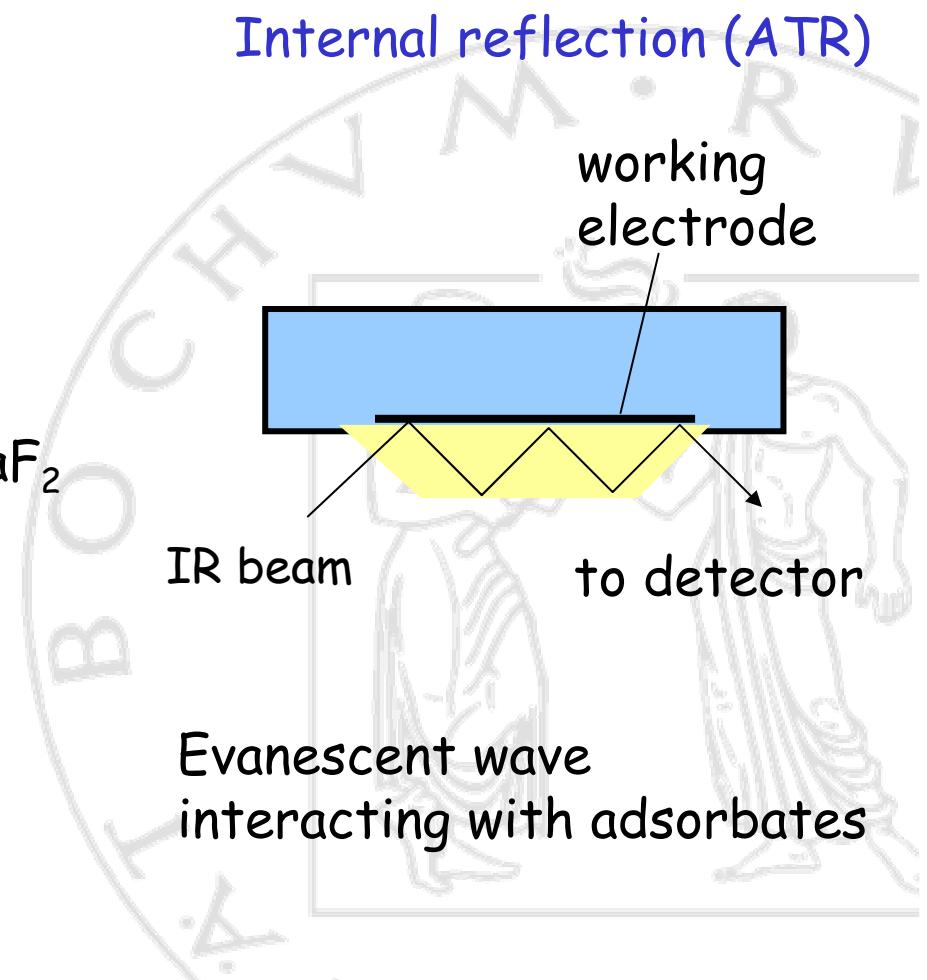
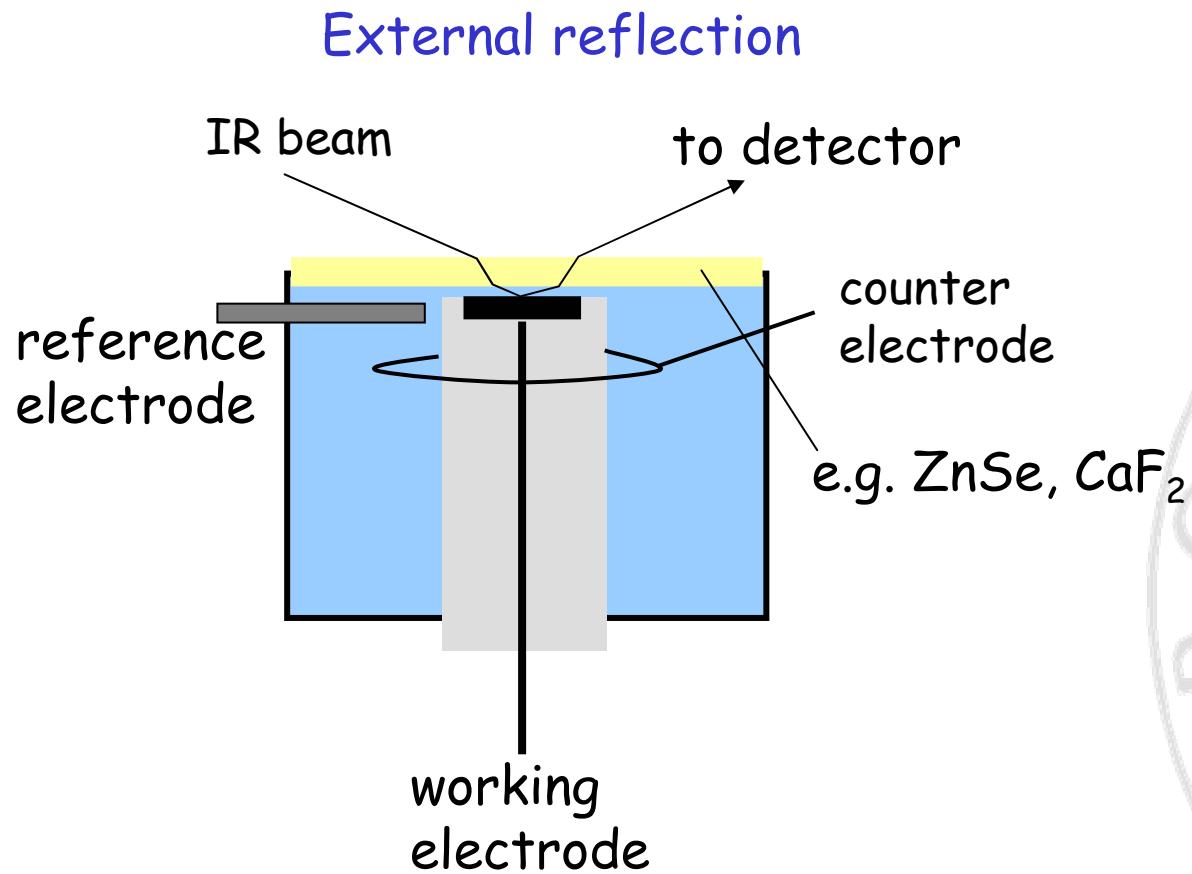


CV, RDE, Impedance

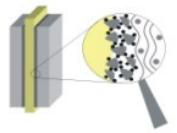
T.J. Schmidt et. al., J. Electrochem. Soc. 145 (1998) 2354.
M. Bron et al., J. Electroanal. Chem. 517 (2001) 85.



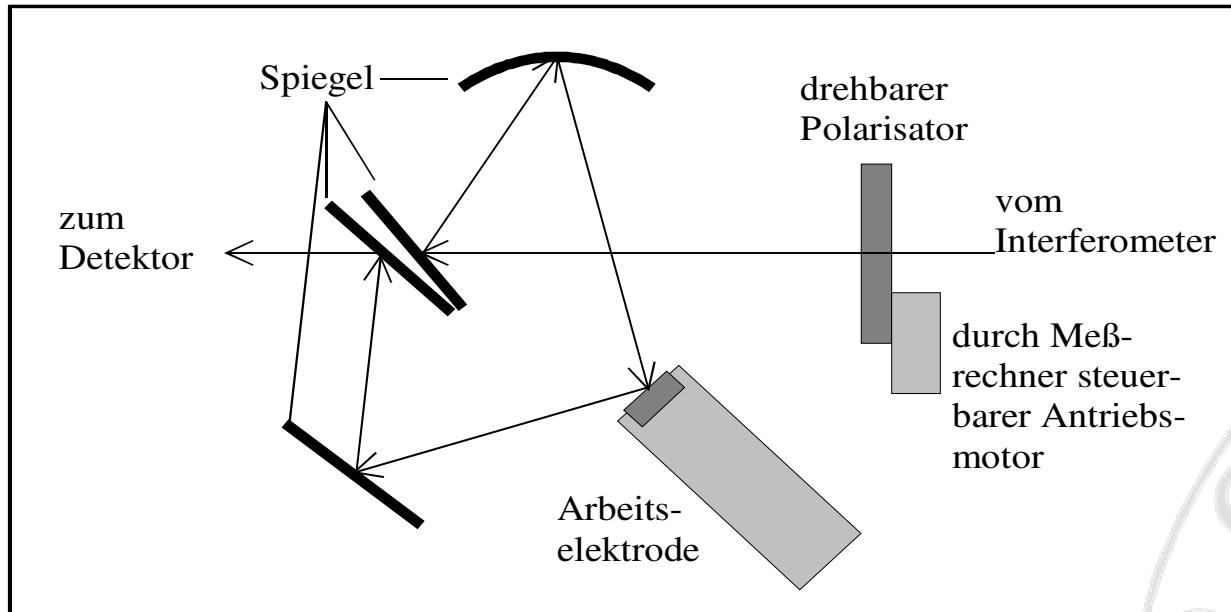
Electrochemical Infrared spectroscopy ("spectroelectrochemistry")



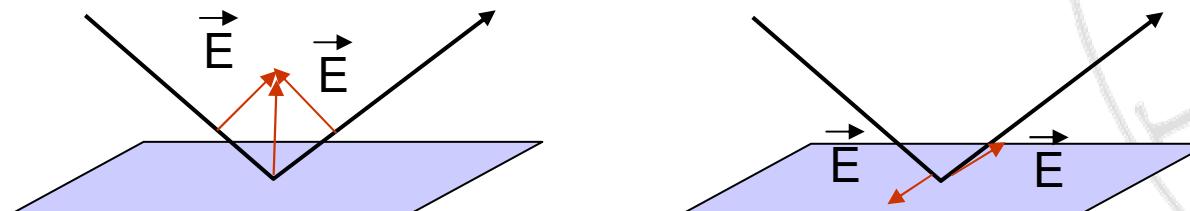
Gap electrode - window: < 10 µm



Setup for in situ-IR-spectroscopic experiments



Polarisation modulation

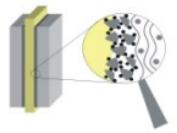


Potential modulation

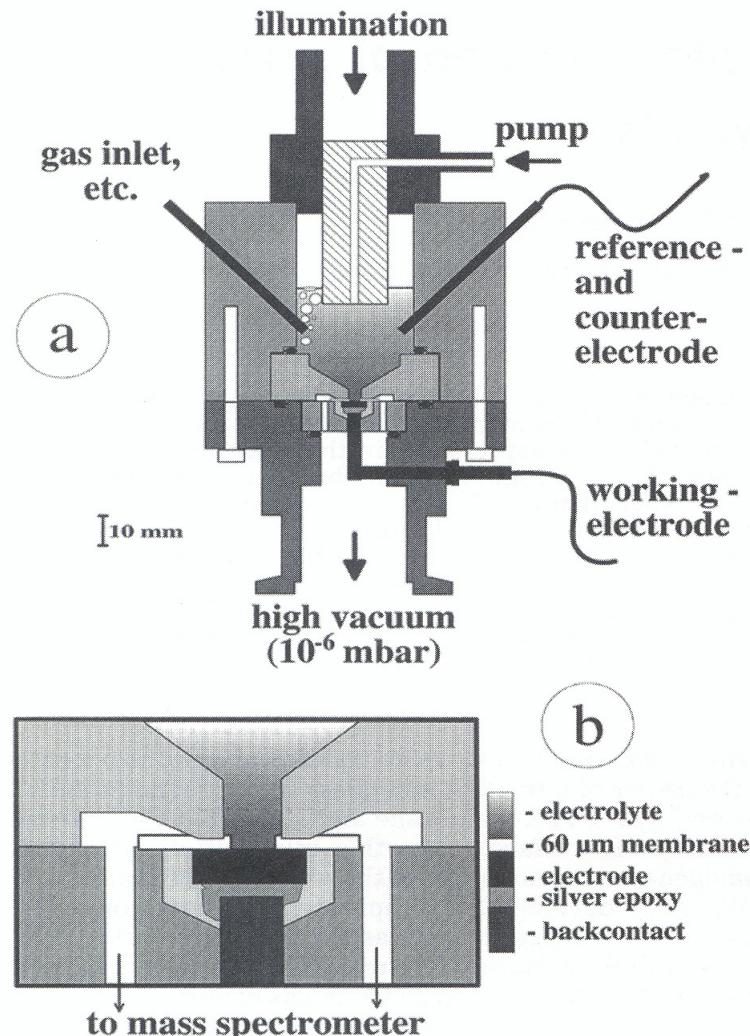


Adsorption strength depends on electrode potential

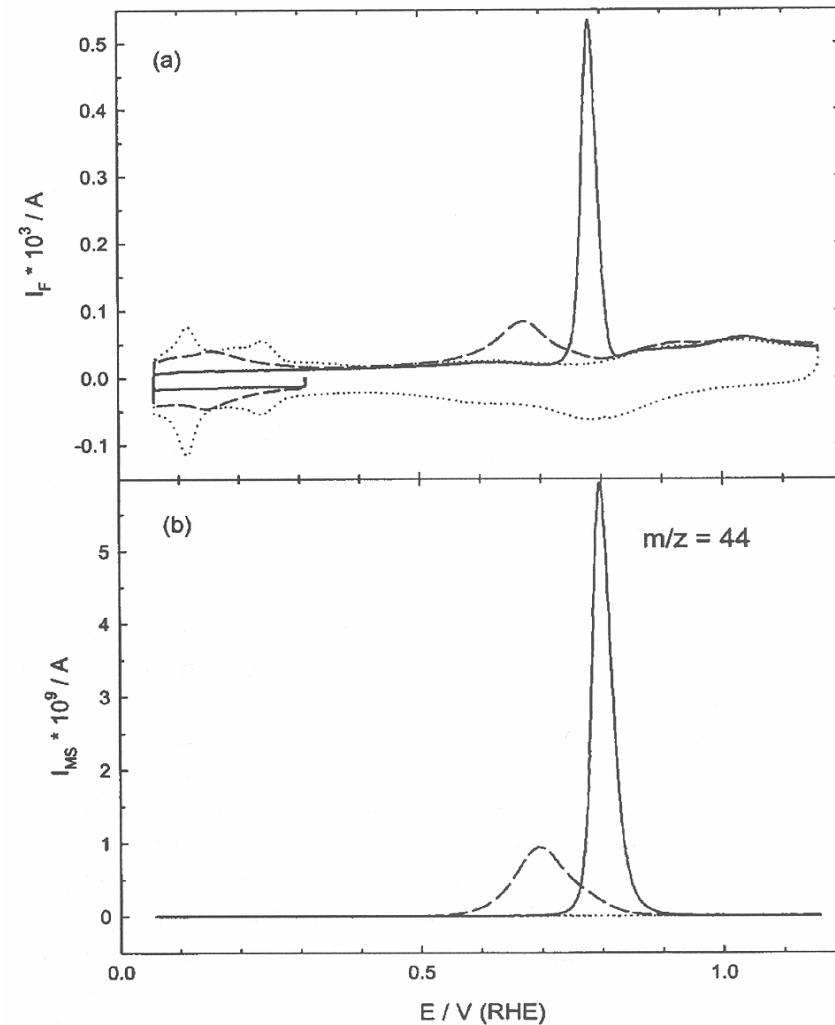
Adsorbate orientations:
Surface selection rule



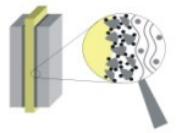
Differential electrochemical mass spectrometry DEMS



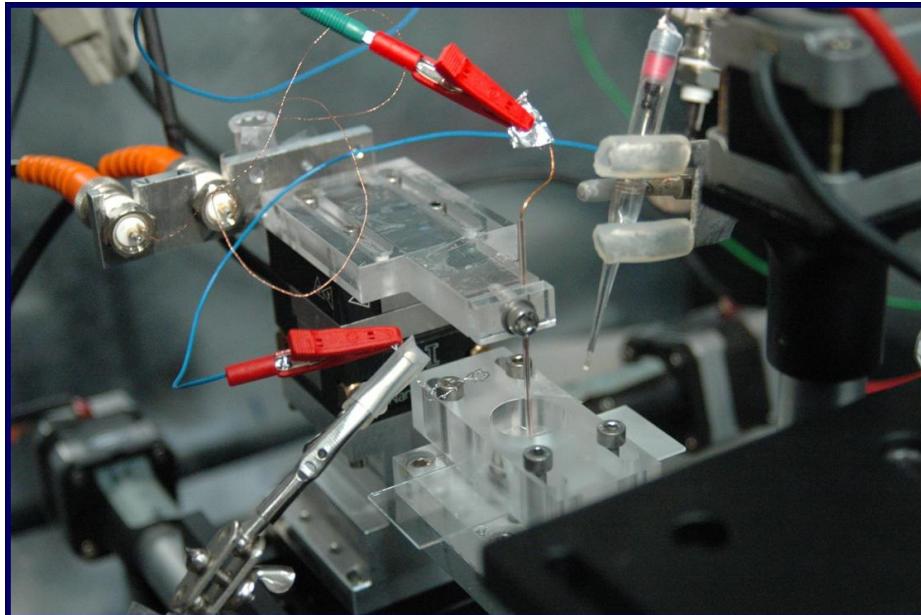
From: Bogdanoff et al., J. Electrochem. Soc. 145 (1998) 576.



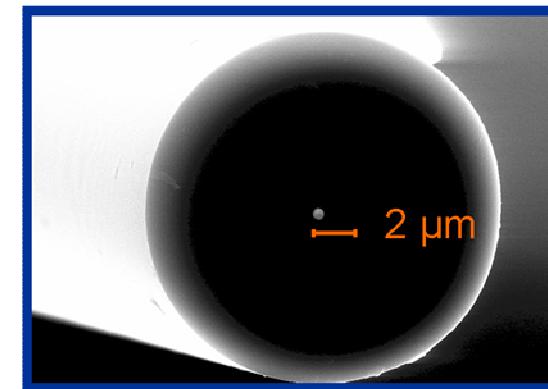
From: Jusys and Behm, J. Phys. Chem. B 105 (2001) 1874.



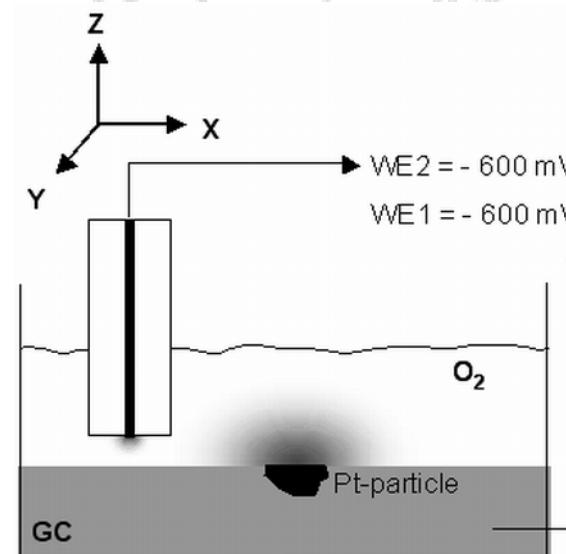
Scanning electrochemical microscope: monitoring catalytically active surfaces



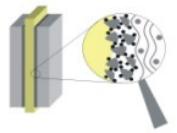
SECM setup



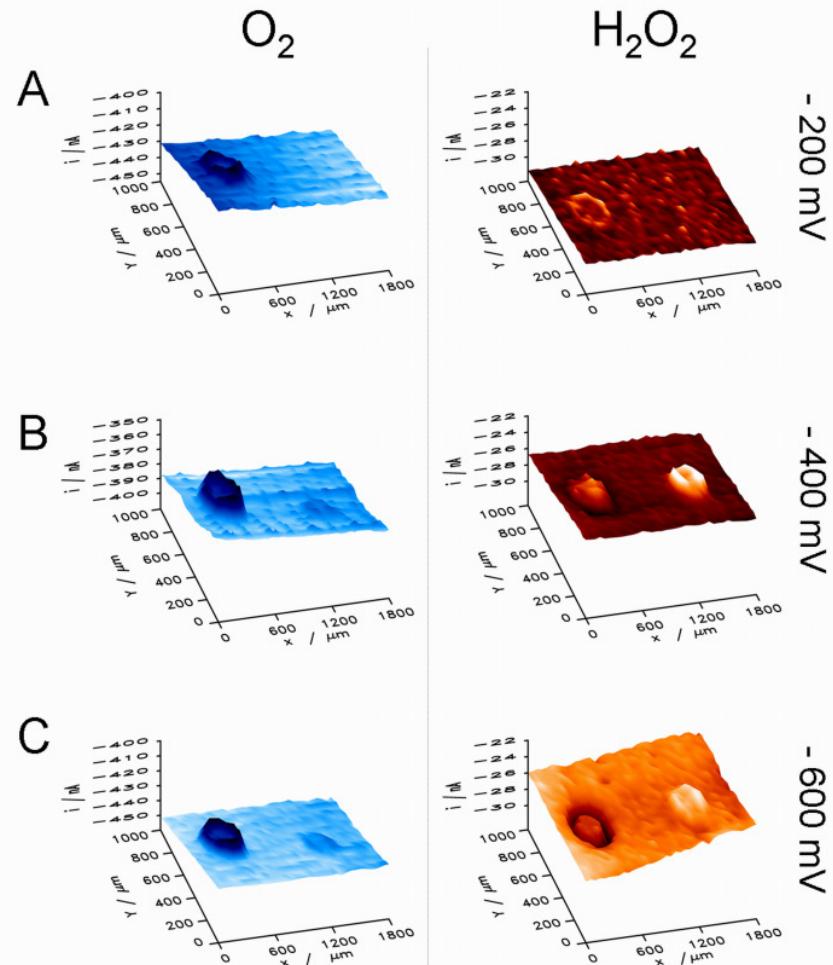
SECM tip



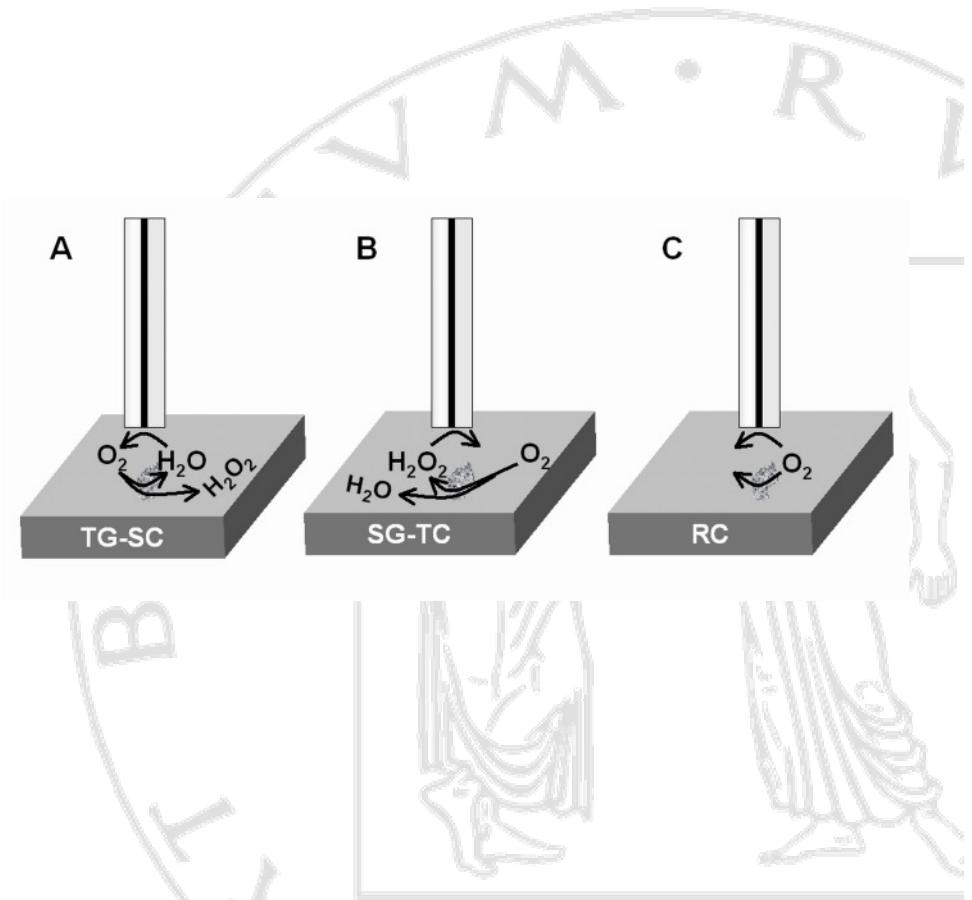
Thanks to K. Eckhard, Bochum



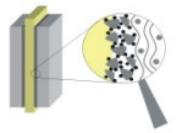
Redox-competition SECM



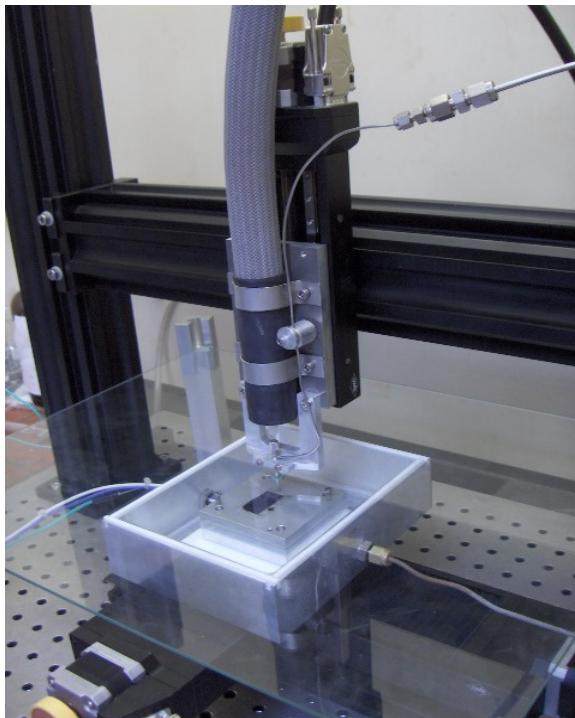
Visualising the activity of a Pt (left)
and an Au (right) catalyst



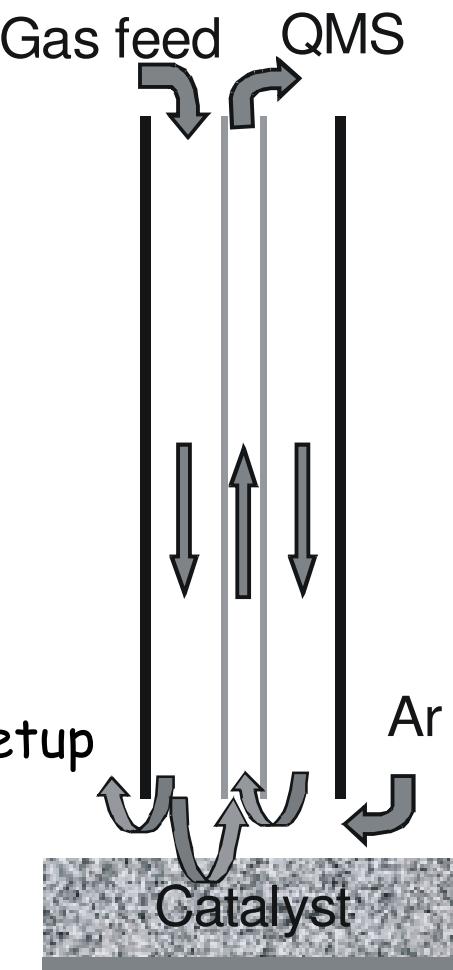
K. Eckhard, Dissertation, Bochum 2007



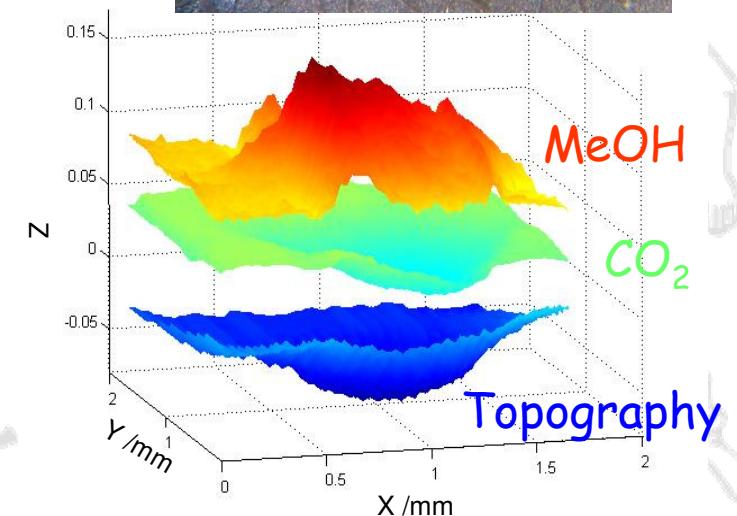
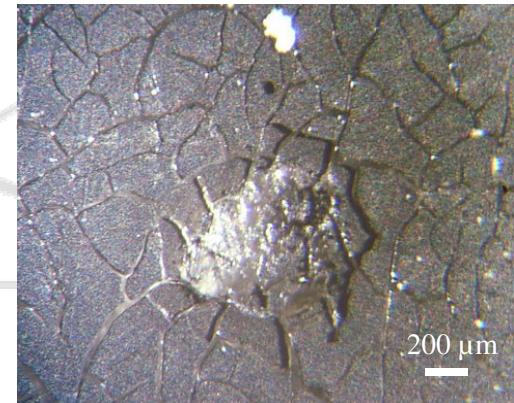
Scanning mass spectrometry



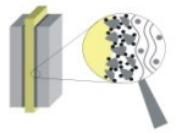
The scanning MS setup



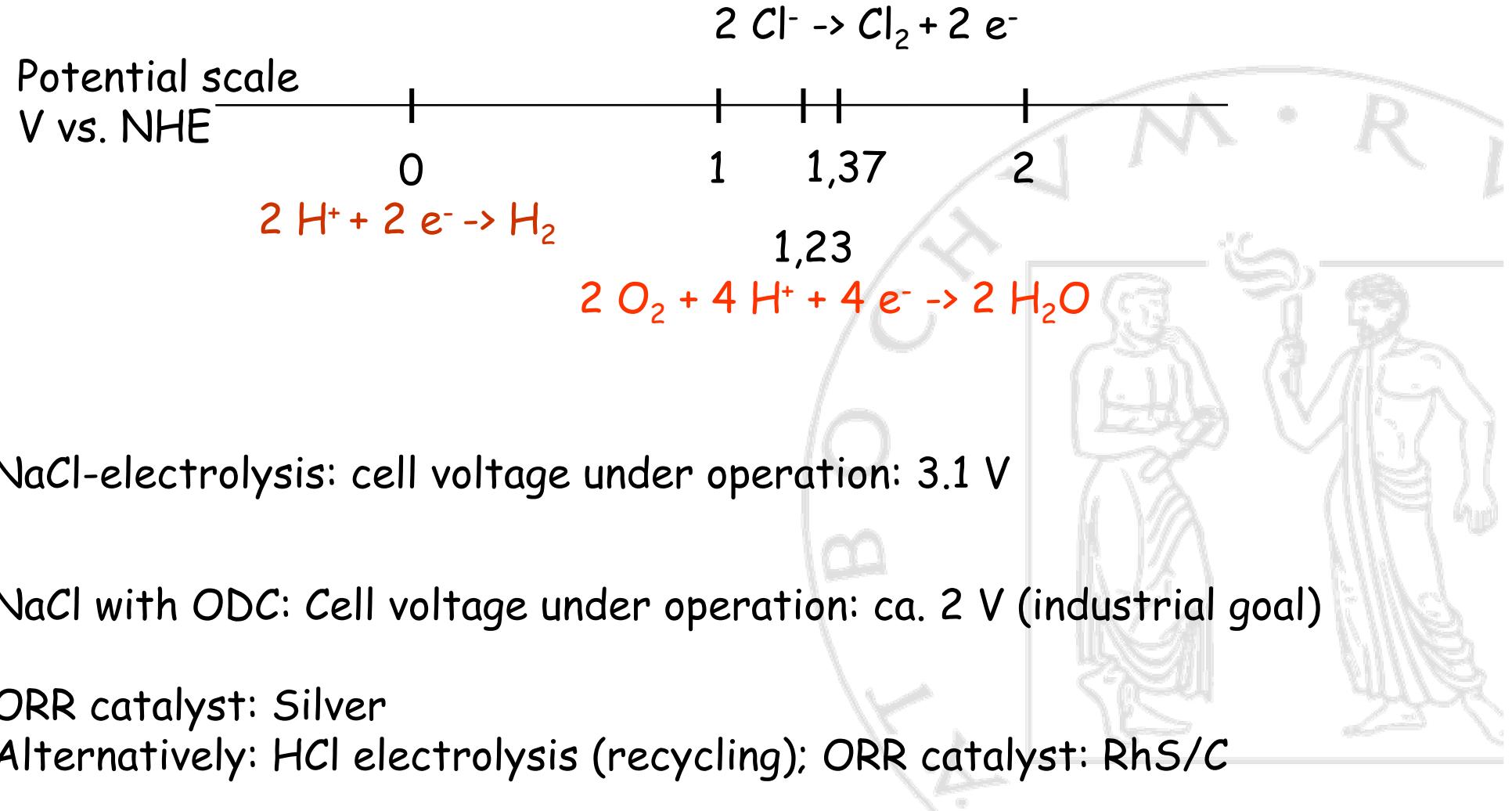
MeOH oxidation over
a damaged GDE

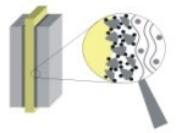


Nan Li, Dissertation, Bochum 2008



A „new trend“ in electrocatalysis: chlorine production





Literature

Electrochemical textbooks

Hamann, Carl H.; Vielstich, Wolf: Elektrochemie 3., überarb. u. erw. Aufl., Wiley-VCH (available also in english)

Bard, Allen J., Faulkner, Larry R.: Electrochemical Methods - Fundamentals and Applications, John Wiley & Sons, Januar 2001

D. Pletcher, R. Greff, R. Peat, L.M. Peter, J. Robinson:
Instrumental Methods in Electrochemistry, Albion/Horwood Publishing House September, 2002

Electrocatalysis:

J. Lipkowski, P.N. Ross, Eds.; Electrocatalysis, Wiley VCH, New York 1998.